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TECHNICAL REPORT ARBRL-TR-02302

TRANSPORT ALGORITHMS FOR PREMIXED,
LAMINAR STEADY STATE FLAMES

T. P. Coffee
J. M. Heimerl

March 1981



US ARMY ARMAMENT RESEARCH AND DEVELOPMENT COMMAND
BALLISTIC RESEARCH LABORATORY
ABERDEEN PROVING GROUND, MARYLAND

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20. ABSTRACT (Continue on reverse side if necessary and identify by block number) (clt) The effects of different methods of approximating multispecies transport phenomena in models of premixed, laminar, steady-state flames have been studied. Five approximation methods that span a wide range of computational complexity are developed. Identical data for individual species properties have been used for each method. Each approximation method is employed in the numerical solution of a set of five H ₂ -O ₂ -N ₂ flames. For each flame the computed species and temperature profiles, as well as the computed flame speeds are found to be very (continued on following page)		

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20. ABSTRACT (Cont'd)

nearly independent of the approximation method used. This does not indicate that transport phenomena are unimportant, but rather that the selection of the input values for the individual species transport properties is more important than the selection of the method used to approximate the multispecies transport.

Based on these results we have developed a sixth approximation method that is computationally efficient and which provides results extremely close to the most sophisticated and precise method used.

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I. INTRODUCTION

To determine validated sets of elementary chemical reactions for use in predictive combustion models, we have chosen to simulate the one dimensional, premixed, laminar flame. This approach has the advantage that the predicted temperature and species profiles can in principal be compared with suitable burner experiments of the same flame. The corresponding equations are derived by Bird, Stewart and Lightfoot,¹ and by Williams,² and are given in Appendix A.

Such a simulation requires as input not only the kinetics information (of our immediate interest), but also thermodynamic and transport data. Fortunately the thermodynamics input is by and large well defined.^{3,4} In addition, while some transport coefficients are only well defined through low temperature (< 1000 K) measurements,⁵ the theory is sufficiently developed to allow reasonable estimates to be made at higher temperatures.⁶ A theory has been developed for multicomponent

¹R. B. Bird, W. S. Stewart and E. N. Lightfoot, Transport Phenomena, John Wiley and Sons, NY, (1960).

²F. A. Williams, Combustion Theory, Addison-Wesley, Reading, MA, (1965).

³D. R. Stull and H. Prophet, JANAF Thermochemical Tables, 2nd Edition, NSRDS-NBS-37, June 1971.

⁴S. Gordon and B. J. McBride, "Computer Program for Calculation of Complex Chemical Equilibrium Compositions, Rocket Performance, Incident and Reflected Shocks and Chapman-Jouguet Detonations", NASA-SP-273, (1971), (1976 program version).

⁵Y. S. Touloukian, P. E. Liley, and S. C. Saxena, Thermophysical Properties of Matter, Vol. 3, Thermal Conductivity (Nonmetallic Liquids and Gases), IFI/Plenum, NY-Washington, (1970).

⁶J. O. Hirshfelder, C. F. Curtiss and R. B. Bird, Molecular Theory of Gases and Liquids, 2nd printing, corrected, with notes, John Wiley and Sons, NY, (1964).

mixtures,⁶⁻¹⁰ but it is computationally cumbersome. To circumvent this, previous workers have generally employed some level of simplification.¹¹⁻²¹

- ⁷C. S. Wang Chang, G. E. Uhlenbeck and J. deBoer, Studies in Statistical Mechanics, Vol. 2, John Wiley and Sons, NY, (1964).
- ⁸L. Monchick, K. S. Yun and E. A. Mason, "Formal Kinetic Theory of Transport Phenomena in Polyatomic Gas Mixtures", *J. Chem. Phys.*, 39, 654-699 (1963).
- ⁹L. Monchick, A. N. G. Pereira and E. A. Mason, "Heat Conductivity in Polyatomic and Polar Gases and Gas Mixtures", *J. Chem. Phys.*, 42, 3241-3256 (1965).
- ¹⁰L. Monchick, R. J. Munn and E. A. Mason, "Thermal Diffusion in Polyatomic Gases: A Generalized Stefan-Maxwell Diffusion Equation", *J. Chem. Phys.*, 45, 3051-3058 (1966).
- ¹¹G. Dixon-Lewis, et al., "Flame Structure and Flame Reaction Kinetics", *Proc. R. Soc., London A* 317, 235-263 (1970); *A* 330, 199-218 (1972); *A* 331, 571-584 (1973); and *A* 346, 261-278 (1975).
- ¹²G. Dixon-Lewis, "Kinetic Mechanism, Structure and Properties of Premixed Flames in Hydrogen-Oxygen-Nitrogen Mixtures", *Phil. Trans. R. Soc., London*, 292, 45-99 (1979).
- ¹³G. Tsatsaronis, "Prediction of Propagating Laminar Flames in Methane, Oxygen, Nitrogen Mixtures", *Combust. and Flame*, 33, 217-239 (1978).
- ¹⁴J. Warnatz, "Calculation of the Structure of Laminar Flat Flames 1; Flame Velocity of Freely Propagating Ozone Decomposition Flames", *Ber. Bunsenges Phys. Chem.*, 82, 193-200 (1978).
- ¹⁵D. B. Spalding and P. L. Stephenson, "Laminar Flame Propagation in Hydrogen + Bromine Mixtures", *Proc. R. Soc. London A*, 324, 315-337 (1971).
- ¹⁶P. L. Stephenson and R. G. Taylor, "Laminar Flame Propagation in Hydrogen, Oxygen, Nitrogen Mixtures", *Combust. and Flame* 20, 231-244 (1973).
- ¹⁷L. D. Smoot, W. C. Hecker, and G. A. Williams, "Prediction of Propagating Methane-Air Flames", *Combust. and Flame* 26, 323-342 (1976).
- ¹⁸J. Warnatz, "Calculation of the Structure of Laminar Flat Flames II; Flame Velocity and Structure of Freely Propagating Hydrogen-Oxygen and Hydrogen-Air Flames", *Ber. Bunsenges Phys. Chem.*, 82, 643-649 (1978).
- ¹⁹D. B. Spalding, P. L. Stephenson, and R. G. Taylor, "A Calculation Procedure for the Prediction of Laminar Flame Speeds", *Combust. and Flame* 17, 55-64 (1971).
- ²⁰L. Bledjian, "Computation of Time-Dependent Laminar Flame Structure", *Combust. and Flame*, 20, 5-17 (1973).
- ²¹E. Cramarossa and G. Dixon-Lewis, "Ozone Decomposition in Relation to the Problem of the Existence of Steady-State Flames", *Combust. and Flame* 16, 243-251 (1971).

This paper addresses the question: which of the mathematical approximations to the multicomponent transport properties provides a desirable trade-off between precision and computational effort. Another way of phrasing this question is to ask what loss in precision of predicted flame speeds and profiles occurs as the mathematical approximations to the multicomponent, polyatomic transport expressions are made cruder.

We approach this problem by actually computing the flame properties for a given flame with a fixed set of input conditions. The transport algorithms are varied and the resulting flame speeds and profiles compared. The numerical method is discussed in references 22 and 23. We have selected the H_2 - O_2 - N_2 system as the candidate flame because it has a well characterized set of input parameters. (See Appendix B).

This paper is divided into the following sections. Section II outlines a sequence of five methods for approximating the transport coefficients. Section III shows the numerical results of these approximation methods relative to the most accurate method, and Section IV discusses their relative precision for a set of five flames. Based on these results, we outline in Section V an algorithm which provides a reasonable balance between computational effort and theoretical rigor and includes a crude approximation for the effects of thermal diffusion. There are several appendices that contain sufficient detail to reproduce our computations.

II. APPROXIMATION METHODS

In this section we outline five approximations to the multicomponent, polyatomic formalism, based on the theory of Wang Chang and Uhlenbeck.⁶⁻¹⁰ We start with the most accurate and progressively consider cruder approximations. Method I is the three term Sonine approximation to the formalism. Dixon-Lewis (DL)²⁴ gives a discussion of this approximation, and we will generally follow his approach. Method II involves a level of approximation using smaller matrices. Methods III and IV use

²²T. P. Coffee and J. M. Heimerl, "A Method for Computing the Flame Speed for a Laminar, Premixed, One Dimensional Flame", BRL Technical Report, ARBRL-TR-02212, Jan 80.

²³T. P. Coffee, "A Computer Code for the Solution of the Equations Governing a Laminar, Premixed, One Dimensional Flame", BRL Memorandum Report, to be published.

²⁴G. Dixon-Lewis, "Flame Structure and Flame Reaction Kinetics II. Transport Phenomena in Multicomponent Systems", Proc. Roy. Soc. A 307, 111-135 (1968).

non-matrix techniques. Method V discusses the case of constant transport parameters. In each case we need to determine the diffusion velocities V_i , $i = 1, 2, \dots, N$, and the heat flux q .

A. Method I

Following (DL), we can write

$$q = \sum_{i=1}^N \rho Y_i V_i h_i - \lambda_0 \frac{\partial T}{\partial x} - \sum_{i=1}^N \frac{RT D_i^T}{M_i Y_i} \frac{\partial X_i}{\partial x} \quad (1)$$

and

$$V_i = \frac{1}{X_i} \sum_{j=1}^N \frac{Y_j}{X_j} D_{ij} \frac{\partial X_j}{\partial x} - \frac{D_i^T}{\rho Y_i} \frac{\partial}{\partial x} (\ln T), \quad (2a)$$

or

$$V_i = V_i + w_i, \quad (2b)$$

a notation we will later find convenient. The diffusion coefficients can be written in terms of the Sonine expansion coefficients,

$$D_{ij} = X_i \frac{16T}{25p} \frac{\sum_{k=1}^N M_k X_k}{M_j} c_{i00}^{1ji} \quad (3)$$

and

$$D_i^T = \frac{8}{5} \frac{M_i X_i}{R_a} a_{i00}^1. \quad (4)$$

Substituting equations (3) and (4) into equation (2) we find

$$V_i = \frac{16T}{25p} \sum_{j=1}^N (c_{i00}^{1ji} \frac{\partial X_j}{\partial x}) - \frac{8T}{5p} a_{i00}^1 \frac{\partial}{\partial x} (\ln T). \quad (5)$$

Similarly, we can write

$$\lambda_o = \lambda_{o,tr} + \lambda_{o,int} = -4 \sum_{i=1}^N X_i a_{i10}^1 - 4 \sum_{i=1}^N X_i a_{i01}^1 \quad (6)$$

The diffusion velocities and the heat flux are now defined in terms of the a_{i00}^1 , a_{i10}^1 , a_{i01}^1 , and c_{i00}^{1ji} . If we use three terms in the polynomial expansion, these are defined implicitly by the equations

$$\begin{aligned} (L) & (a_{100}^1 \dots a_{N00}^1, a_{110}^1 \dots a_{N10}^1, a_{101}^1 \dots a_{N01}^1)^T \\ & = (0 \dots 0, X_1 \dots X_N, X_1 \dots X_N)^T \end{aligned} \quad (7)$$

and

$$\begin{aligned} (L) & (c_{100}^{1hk} \dots c_{N00}^{1hk}, c_{110}^{1hk} \dots c_{N10}^{1hk}, c_{101}^{1hk} \dots c_{N01}^{1hk})^T \\ & = (\delta_{1h} - \delta_{1k} \dots \delta_{Nh} - \delta_{Nk}, 0 \dots 0, 0 \dots 0) \quad h, k = 1 \dots N. \end{aligned} \quad (8)$$

The elements of the $3N$ by $3N$ matrix (L) are given in Appendix C. The procedures we have used for computing these elements are discussed in Appendix D.

From equation (8), it appears that we must solve N^2 sets of equations to obtain the c_{i00}^{1ji} . In fact, it has been recommended^{6,8,24} that only the a terms be computed using this level of approximation, and that the c terms be computed using a one term expansion (see Method II).

However, this is not necessary if we observe that we are only interested in the V_i 's, and not directly in the c terms. We can convert the c -vector in equation (8) to a vector whose elements are in fact the V_i by multiplying each equation of (8) by $\frac{16T}{25p} \frac{\partial X_h}{\partial x}$ and then summing over h . After some algebra we find

$$(L) (V_1 \dots V_N, \dots)^T = \left(\frac{16T}{25p} \frac{\partial X_1}{\partial x} \dots \frac{16T}{25p} \frac{\partial X_N}{\partial x}, 0 \dots 0, 0 \dots 0 \right)^T. \quad (9)$$

Equation (9) shows that we can solve directly for the required V_i and that the right hand side is not a function of either h or k .

In solving for the transport in our code, we decompose (L) as the product of an upper matrix multiplying a lower matrix. Equations (7) and (9) can then be solved efficiently by back substitution. It is computationally efficient to do this rather than generate another, smaller matrix for the V_i using a one term approximation and solving this new system. To solve these systems of algebraic equations we have used an assembly language algorithm²⁵ which has been found to execute on the BRL CDC 7600 about five times faster than the equivalent FORTRAN coding.

B. Method II

The above formalism is quite complicated to work with, and so further simplifications are almost invariably made.

For diffusion, we can simplify by taking only one term in the Sonine polynomial expansions. This results in

$$(L^{00,00}) (c_{100}^{1hk} \dots c_{N00}^{1hk})^T = (\delta_{1h} - \delta_{1k}, \dots, \delta_{Nh} - \delta_{Nk})^T \quad h, k = 1 \dots N, \quad (10)$$

where the elements of $(L^{00,00})$ are defined in Appendix C. This can be rearranged⁶ to give the Stefan-Maxwell equations, namely,

$$\frac{\partial X_i}{\partial x} = \sum_{j=1}^N \frac{X_j X_i}{D_{ij}} (V_j - V_i), \quad i=1 \dots N. \quad (11)$$

This set of equations is not independent, and the constraint

$$\sum_{i=1}^N Y_i V_i = 0 \quad (12)$$

must be used in place of one of the equations in (11). Then the diffusion velocities can be found by solving a set of N equations in N unknowns. This approach gives zero for the thermal diffusion velocity, W_i .

²⁵ A. C. Hindmarsh, L. J. Sloan, K. W. Fong, and G. H. Rodrigue, "DEC/SOL: Solution of Dense Systems of Linear Algebraic Equations", Lawrence Livermore Laboratory, UCID-30137, 1976.

Thermal conductivity cannot be simplified this easily. However, ignoring internal energy, we can obtain the matrix form

$$L^{10,10} (a_{110}^1 \dots a_{N10}^1)^T = (X_1, \dots X_N)^T, \quad (13)$$

where $\lambda_o = \lambda_{o, \text{tr}} = -4 \sum_{i=1}^N X_i a_{i10}^1$.²⁶ This form will be valid for a mixture of monatomic gases.

To define the heat conductivity for a mixture of polyatomic gases, we adopt Hirshfelder's* Eucken-type relation,^{27,5}

$$\lambda_{\text{mix}}^{\text{poly}} = \lambda_{\text{mix}}^{\text{mon}} + \sum_{i=1}^N \frac{\lambda_i - \lambda_i^{\text{mon}}}{1 + \sum_{j \neq i} \frac{D_{ij}}{D_{ii}} \frac{X_j}{X_i}}. \quad (14)$$

The quantity λ_o in method I is not exactly identical to the usual thermal conductivity $\lambda_{\text{mix}}^{\text{poly}}$, but can be interpreted as the thermal conductivity of a mixture in which the diffusion forces vanish.

If the thermal diffusion coefficients are zero, as they are at this level of approximation, then $\lambda_o = \lambda_{\text{mix}}^{\text{poly}}$.

C. Method III

By making additional assumptions, the Stefan-Maxwell equations (11) can be further simplified. A common assumption is that all but the i th species move with the same velocity V . Then we find that

*The detailed analysis of Monchick, et al.,⁹ shows that the D_{ij} should be $D_{i, \text{int}, j}$. From a practical point of view we have taken $D_{i, \text{int}, j} = D_{ij}$.

²⁶C. Muckenfuss and C. F. Curtiss, "Thermal Conductivity of Multicomponent Gas Mixtures", *J. Chem. Phys.* 29, 1273-1277 (1958).

²⁷J. O. Hirshfelder, "Heat Conductivity in Polyatomic, Electronically Excited, or Chemical Reacting Mixtures. III", *Sixth International Combustion Symposium*, Reinhold Publishing Corporation, NY, 351-366 (1957).

$$\frac{\partial X_i}{\partial x} = X_i (V - V_i) \sum_{j \neq i} \frac{X_j}{D_{ij}}. \quad (15)$$

Employing (12) we find

$$V = - \frac{Y_i V_i}{1 - Y_i} \quad (16)$$

which when substituted into (15) yields the formula recommended by Hirshfelder and Curtiss²⁸

$$V_i = - \frac{(1 - Y_i)}{X_i \sum_{j \neq i} \frac{X_j}{D_{ij}}} \frac{\partial X_i}{\partial x}. \quad (17)$$

Unfortunately, the expression in (17) does not in general satisfy equation (12). One technique to satisfy this constraint is due to Boris and Oran.²⁹ They note that if a set of diffusion velocities V_i satisfy the Stefan-Maxwell equations (11), then so does the set $(V_i + V_c)$, where V_c is some constant. The value of V_c is chosen such that the constraint (12) is satisfied.*

The heat conductivity formula employed at this level of approximation is taken from Mason and Saxena's^{30,5} simplification of (14), specifically

²⁸J. O. Hirshfelder and C. F. Curtiss, "Theory of Propagation of Flames Part I: General Equations", Third International Combustion Symposium, Williams and Wilkins Co., Baltimore, 121-127 (1949).

²⁹E. S. Oran and J. P. Boris, "Detailed Modeling of Combustion Systems", to appear in Progress in Energy and Combustion Science.

* Boris and Oran also discuss higher order approximations to the Stefan-Maxwell equations that will not be discussed here.

³⁰E. A. Mason and S. C. Saxena, "Approximate Formula for the Thermal Conductivity of Gas Mixtures", Phys. Fluids, 1, 361-369 (1958).

$$\lambda_o = \frac{\sum_{i=1}^N \lambda_i}{1 + \sum_{j \neq i} \phi_{ij} (X_j/X_i)} \quad (18)$$

where

$$\phi_{ij} = \frac{1.065}{8^{1/2}} \left(1 + \frac{M_i}{M_j}\right)^{-1/2} \left[1 + \left(\frac{\eta_i M_j}{\eta_j M_i}\right)^{1/2} \left(\frac{M_i}{M_j}\right)^{1/4}\right]^2. \quad (19)$$

D. Method IV

Equation (17) or some analogous form has often been used to compute diffusion. However, the usual procedure has been to use (17) only to compute V_1, \dots, V_{N-1} . Then V_N is computed from (12). This is less accurate than the Boris and Oran procedure, especially for V_N .

Also, an empirical formula for the thermal conductivity,

$$\lambda_o = 0.5 \left[\sum_{i=1}^N X_i \lambda_i + \left\{ \sum_{i=1}^N X_i / \lambda_i \right\}^{-1} \right], \quad (20)$$

is often used.^{31,5}

Method IV is comprised of these common approximations.

E. Method V

In the case of a binary mixture the Stefan-Maxwell equations (11) reduce to Fick's law. Specifically we have,

$$Y_1 V_1 = -D_{12} \frac{\partial Y_1}{\partial x}. \quad (21)$$

³¹J. H. Burgoyne and F. Weinber, "A Method of Analysis of a Plane Combustion Wave", *Fourth Symposium on Combustion*, Williams and Wilkins Co., Baltimore, 294-302 (1953).

A generalization of (21) can be made,¹ and yields

$$Y_i V_i = -D_{im} \frac{\partial Y_i}{\partial x}, \quad (22)$$

where

$$D_{im} = \frac{1 - X_i}{\sum_{j \neq i} \frac{X_j}{D_{ij}}}. \quad (23)$$

In the Lennard-Jones formalism $D_{ij} \propto T^{1.5}/\Omega^{(1,1)*}$, where $\Omega^{(1,1)*}$ is approximately proportional to $T^{-0.17}$.³² Since $\rho \propto T^{-1}$ it is not unreasonable to assume that $\rho^2 D_{ij}$ is approximately independent of temperature. Generalizing, it is often assumed that $(\rho^2 D_{im})$ is constant. Likewise for a monatomic gas $\lambda \propto T^{0.5}/\Omega^{(2,2)*}$, where $\Omega^{(2,2)*} \propto T^{-0.16}$,³² and it is not unreasonable to assume that $(\rho\lambda)$ is approximately independent of temperature. We now outline a procedure that permits an *a priori* selection of these quantities.

For a given flame we know T_u and Y_{iu} , the temperature and the mass fractions of the unburned mixture. We also have a chemical kinetics scheme and a method of computing the specific heats c_{pi} and specific enthalpies h_i . Since enthalpy is conserved, i.e.,

$$\left(\sum_{i=1}^N Y_i h_i \right)_B = \left(\sum_{i=1}^N Y_i h_i \right)_u, \quad (24)$$

we can compute the adiabatic flame temperature T_B . The numerical procedure is to guess a trial burned temperature T_t and, using an ODE package, find the corresponding equilibrium mass fractions Y_{it} . We then compute the enthalpy of the burned mixture and compare with the unburned mixture enthalpy. T_t is iteratively adjusted until the burned and unburned mixture enthalpies agree to within a pre-determined error tolerance. We then accept these values of T_t and Y_{it} as T_B and Y_{iB} .

³²A. A. Westenberg, "Present Status of Information on Transport Properties Applicable to Combustion Research", *Combustion and Flame*, 1, 346-358 (1957).

At this level of approximation we would like to use an appropriate constant (or "global") c_p . So we will assume that $c_{pi} = c_p = \text{constant}$, $i = 1 \dots N$. Then the relation $h_i = h_i^\circ + \int_{T_o}^T c_{pi} dT$ becomes $h_i = h_i^\circ + c_p (T - T_o)$ and the mixture enthalpy is given by

$$\sum_{i=1}^N Y_i h_i = \sum_{i=1}^N Y_i h_i^\circ + c_p (T - T_o) . \quad (25)$$

Substituting (25) into (24) we find

$$c_p = \frac{\sum_{i=1}^N h_i^\circ (Y_{iu} - Y_{iB})}{T_B - T_u} . \quad (26)$$

As a heuristic rule, we select $T = 0.5 (T_B + T_u)$ and $Y_i = 0.5 (Y_{iB} + Y_{iu})$ and then evaluate D_{im} and $\rho\lambda$ by using equations (23) and (20), respectively. Then $\rho^2 D_{im}$, $i = 1, 2, \dots, N-1$, and $\rho\lambda$ are evaluated. The diffusion velocity V_N is found from equation (12).

Others¹⁹⁻²¹ have employed the concept of constant $\rho^2 D_{im}$, $\rho\lambda$ and c_p , but the method of evaluation varies from author to author.

III. NUMERICAL RESULTS

Table 1 shows a summary of the five methods of computing the transport properties used in this paper. Five H_2 - O_2 - N_2 flames were selected and their initial conditions listed in Table 2. The total pressure is fixed at one atmosphere for all flames. The computed flame speed for each flame as a function of transport method is tabulated in Table 3. (The flame speeds for flame A are not corrected to 291 K, as has been done.¹¹ If this were done, the value AI for example would be 12.2 cm/s instead of 14.1 cm/s.) The values of the flame speeds span a large range and for a given flame are essentially independent of the transport method. The largest difference between Method I, the most complete formulation of the transport, and any other method is 16%. (Compare Methods I and III, flame D). Note that even Method V gives results that are quite close to the much more complex Method I.

TABLE 1. SUMMARY OF TRANSPORT METHODS

<u>Method</u>	<u>Remarks</u>
I	3 terms of Sonine polynomial expansion (3 N by 3 N matrix); only method that has non-zero thermal diffusion.
II	For diffusion, 1 term of Sonine polynomial expansion (N by N matrix), Eq. (11) and (12). For thermal conductivity, Hirshfelder-Eucken method (N by N matrix), Eq. (13) and (14).
III	Diffusion velocities computed from simplified Stefan-Maxwell relation, Eq. (17). Each v_i is adjusted by a common factor, V_c , so as to satisfy $\sum_{i=1}^N Y_i V_i = 0$. Thermal conductivity from Mason and Saxena, Eq. (18) and (19).
IV	Diffusion velocities computed from the simplified Stefan-Maxwell relation, Eq. (17), for N-1 species. V_N is computed from Eq. (12). Empirical thermal conductivity formula, Eq. (20).
V	$\rho^2 D_{im} = \text{constant}$; $\rho\lambda = \text{constant}$; $c_p = \text{constant}$; constants are determined <i>a priori</i> .

TABLE 2. INITIAL TEMPERATURE AND MOLE FRACTIONS FOR THE FIVE FLAMES STUDIED

<u>Flame</u>	<u>X_{H2}</u>	<u>X_{O2}</u>	<u>X_{N2}</u>	<u>T_u</u>
A	.1883	.0460	.7657	336
B	.2000	.1680	.6320	298
C	.5000	.1050	.3950	298
D	.9000	.1000	0	298
E	.6000	.4000	0	298

TABLE 3. FLAME SPEEDS CALCULATED USING
THE FIVE TRANSPORT MODELS

<u>Flame</u>	<u>I</u>	<u>II</u>	<u>III</u>	<u>IV</u>	<u>V</u>
A	14.1	14.6	14.9	14.9	16.0
B	98	101	102	103	96
C	292	300	310	308	291
D	378	379	438	402	348
E	892	922	971	969	847

Reproduction of flame speeds is a necessary but not sufficient condition to judge the relative effectiveness of the transport methods. We must also examine the species and temperature profiles of these flames. As examples we consider two sets of profiles that exhibit differences among the five methods that are as large as any observed. Figures 1 and 2 show the OH profiles for flame D. Figures 3 and 4 show the H₂ profiles for flame C. As can be seen these profiles are very similar. Almost all the other species profiles and all temperature profiles show a greater degree of similarity among the five profiles than the examples given.

In general, our results agree with those reported by Warnatz.¹⁸ The exception is flame A, for which Warnatz reported a flame speed of 10.4 cm/sec, referenced to 291K. Our computed flame speed is about twenty percent higher. Based on our results, we infer that Warnatz's use of a transport method slightly different from any of those reported here should not make that large a difference. We do not know the cause of the discrepancy.

As a check of our code, we computed the flame speed for flame A, using the kinetics and transport parameters of Dixon-Lewis¹² and Method I. The resulting flame speed was 9.2 cm/sec, referenced to 291K. This agrees with the computed result reported by Dixon-Lewis and we conclude that our code is functioning properly.

We are comparing the model results produced as we vary the transport algorithm and not comparing the model result with experiment. Thus, the fact that the use of Warnatz' parameters produces a slightly inaccurate flame speed for flame A is of no concern.

IV. DISCUSSION

The numerical results shown in Table 3 demonstrate that reliable results can be obtained for the H₂-O₂-N₂ system even for the case of our *a priori* determined constant transport method. Note that we cannot infer that transport is unimportant! The computed profiles and flame speeds can be sensitive to the choice of transport parameters selected. For the relative tests of the transport methods here, we have employed the same set of species viscosities, thermal conductivities and binary diffusion coefficients in all cases. We have demonstrated that the method used to generate the multicomponent, polyatomic transport coefficients is not critical for the H₂-O₂-N₂ flame. And since this flame is reasonably complex we infer that this result has a high probability of being valid for other flames.

Indeed, we conclude that gross errors detected in comparing the results of different models are more likely to be traceable to differences in input data rather than to the method of approximating multicomponent polyatomic transport properties.

We cannot completely explain the surprising agreement among the

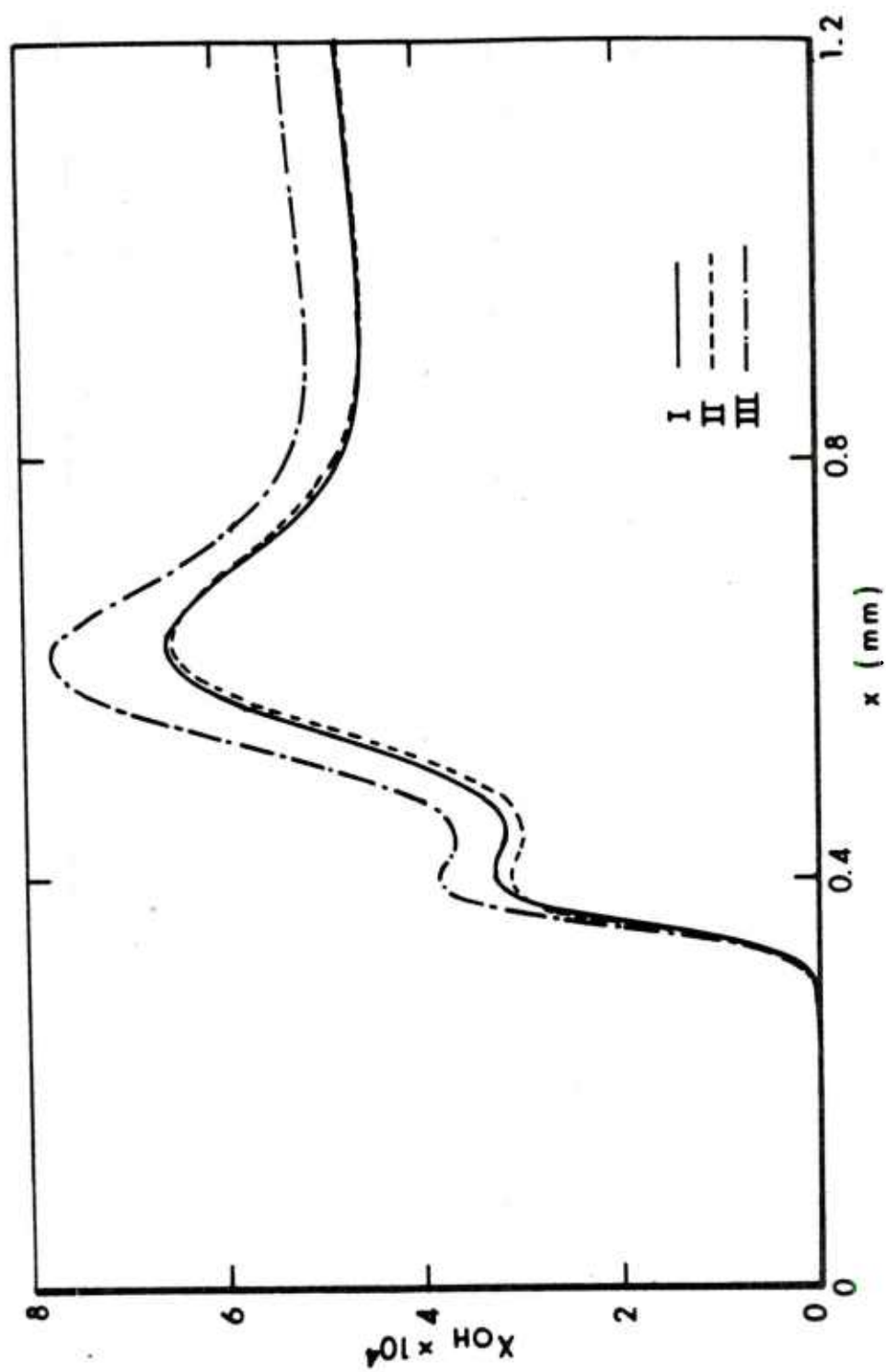


Figure 1. The OH Profile for Flame D.

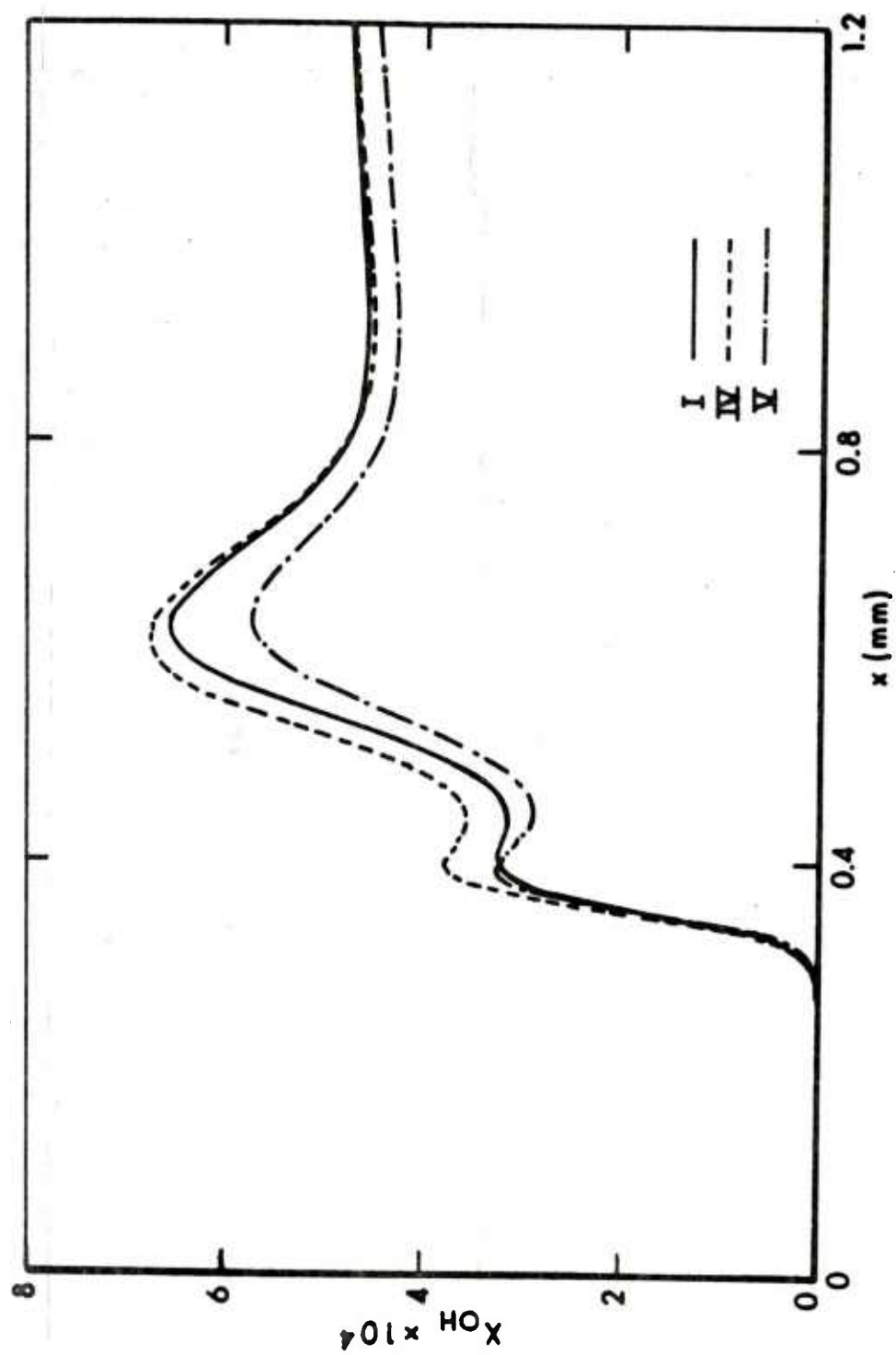


Figure 2. The OH Profile for Flame D.

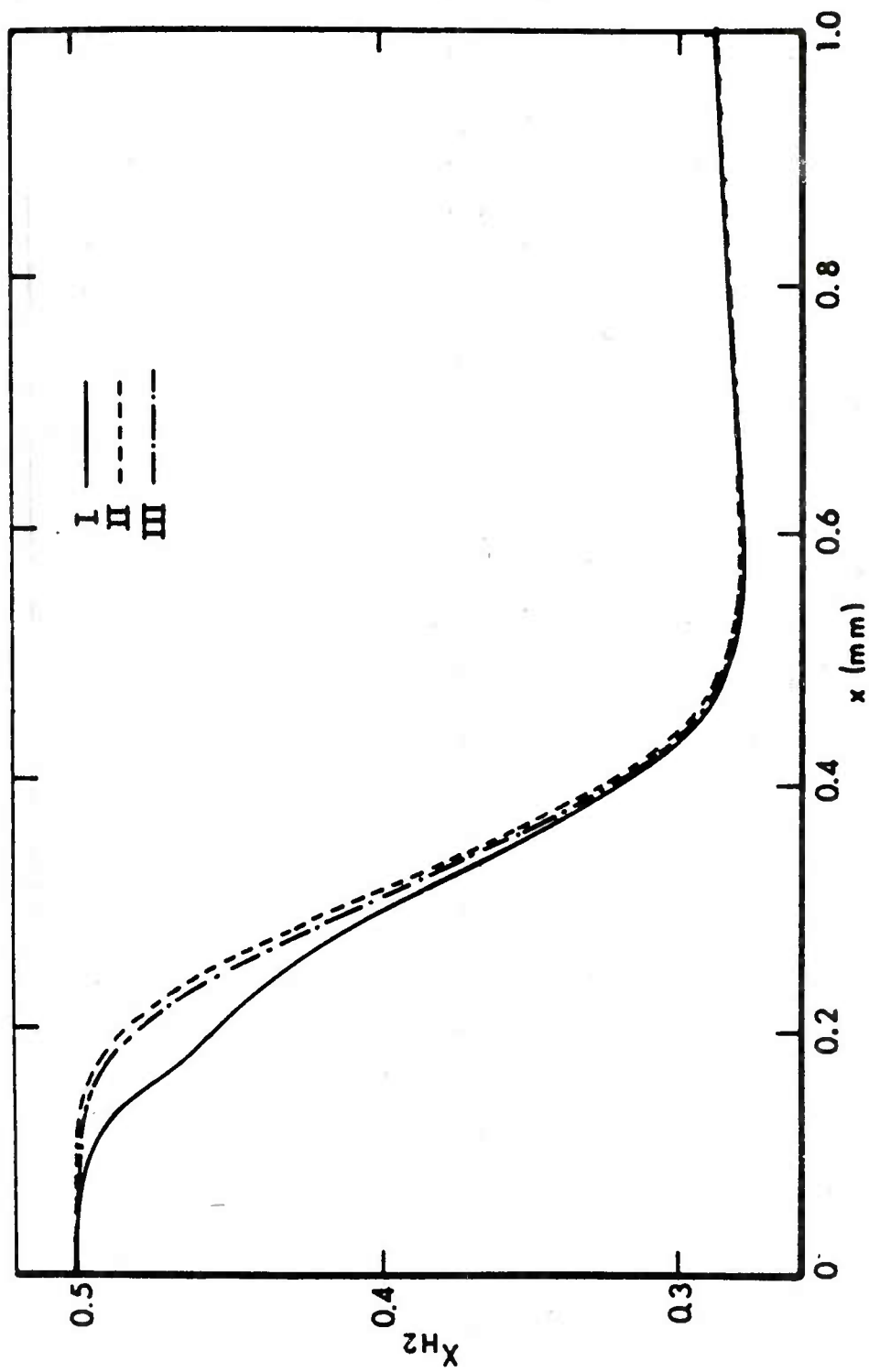


Figure 3. The H_2 Profile for Flame C.

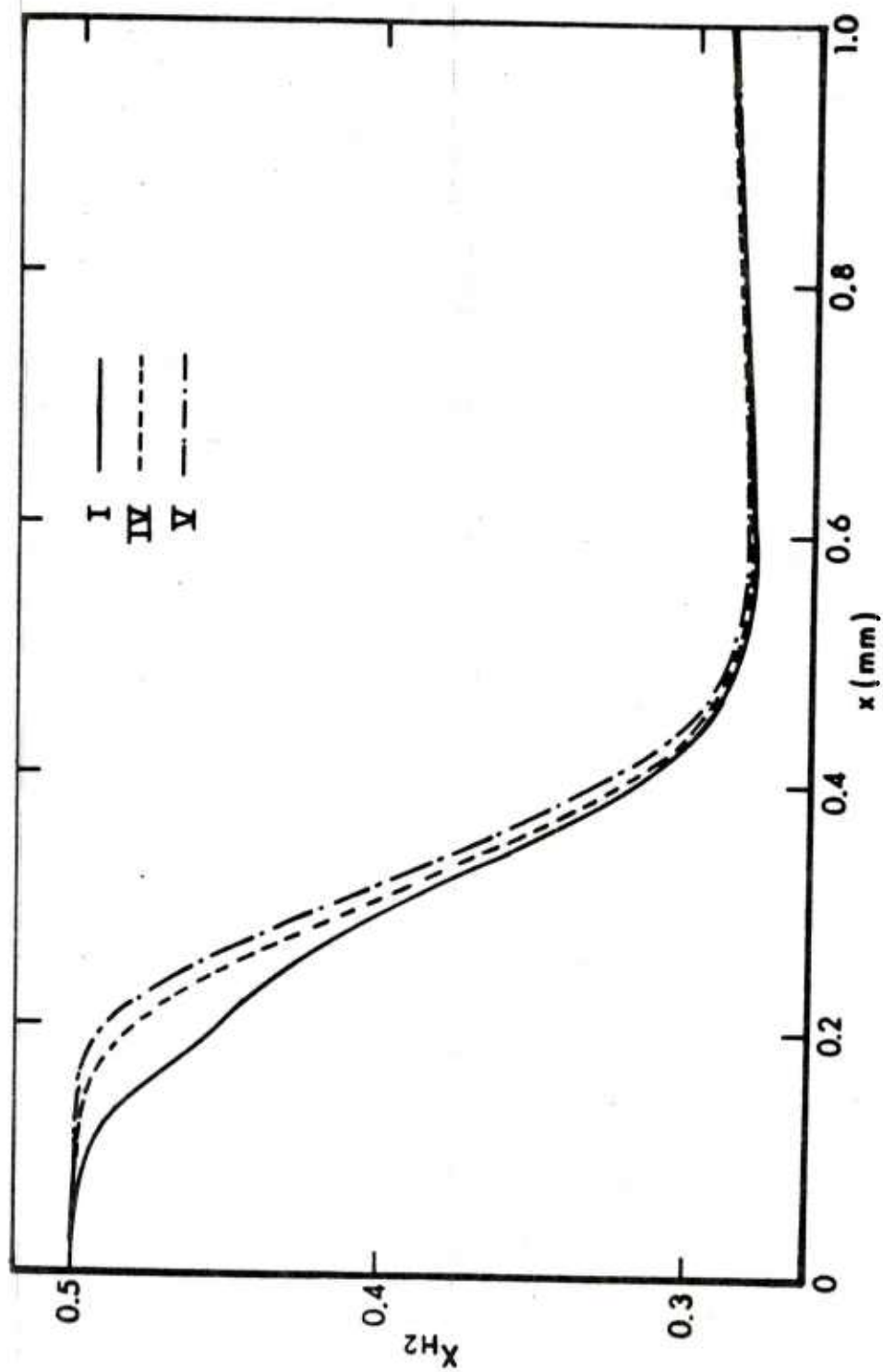


Figure 4. The H_2 Profile for Flame C

various methods. In this section we will show that our results are consistent with the few previous studies of transport algorithms. We will also discuss some additional numerical results that give some indication of the processes involved.

Warnatz¹⁴ essentially compared Methods II and III for an ozone flame and found the differences negligible. However, it was not clear that his observations could be generalized to more complex flames.

In another paper¹⁸ Warnatz included thermal diffusion in a simulation of an H_2 - O_2 - N_2 flame. He used essentially Method IV together with a simple binary formula for thermal diffusion valid only for heavy isotopes.⁶ He found that the effect of thermal diffusion so defined was to lower the flame speed in a rich flame by about 5%. Species and temperature profiles were only slightly changed. He did not discuss the accuracy of this approximation for a mixture.

As noted earlier, Dixon-Lewis²⁴ considered the effect of thermal diffusion. However, he assumed a particular mass flow and simplified chemistry. He found that the thermal diffusion flux of H_2 was quite large and inferred that effects due to thermal diffusion would be important when considering hydrogen atom diffusion in flame systems. This inference is contrary to our findings. Our results also show that, for H and H_2 , the thermal diffusion velocity W_i can be quite large compared to the species diffusion velocity V_i . However, we find that these differences cause only small changes in both the flame speeds and the profiles. This finding supports that of Dixon-Lewis¹² who in a recent paper reported that the inclusion of thermal diffusion for near stoichiometric H_2 -air flames lowers the burning velocity by 5 to 6%.

In an attempt to gain additional insight, we have written an auxiliary code to directly compare the transport properties. The input required for this code are the values of the temperature, the species concentrations, and the temperature and species gradients. Then the thermal conductivity λ_0 and the diffusion velocities V_i are computed using the subroutines written for Methods I through IV, and comparisons among the values for λ_0 and V_i are made. By doing this we avoid the complicated interplay between transport and chemistry that occurs in flames.

The auxiliary code was executed using several hundred sets of input values that were typical of those observed in the flames reported above. These input values were divided into four groups for analysis. Group 1 consisted of small species and temperature gradients, Group 2 of large species and temperature gradients, Group 3 of large species gradients and a zero temperature gradient, and Group 4 of small species gradients and large temperature gradients. By a large gradient we mean a value typical of a flame front.

The values of thermal conductivity computed with the auxiliary code showed little variation, regardless of the input group or approximation

method used. Specifically, the differences between Methods I and II, I and III, and I and IV averaged 2, 3 and 5%, respectively. In general, the thermal conductivities of the individual species are not this well known either theoretically or experimentally. So despite the widely different levels of complexity, the four methods produced equivalent values for λ_0 .

The results of the comparisons for diffusion velocities are more difficult to summarize. Differences varied from less than 1% up to several hundred percent, depending on the particular input values and the particular species considered. Differences of 30 to 40% were common and in general were larger for the major species than for the minor species.

We could not establish why there was a high degree of similarity in the flame speeds and profiles even though these were large differences in the V_i in the auxiliary code. We speculate that part of the reason for this is due to the constraint $\sum_{i=1}^N Y_i V_i = 0$, which is satisfied by all of our methods. Another constraint on the diffusion velocities in the flame code is the fixed chemistry employed. How the non-linear feedback between the chemistry and the transport affects the similarity in the flame speeds and profiles is unknown.

Nevertheless, some interesting conclusions can be drawn from these comparisons. For instance, it is often assumed that thermal diffusion is negligible. This assumption corresponds to that made in Group 3. (If the temperature gradient is zero, the thermal diffusion velocities w_i will also be zero).

For this group, we find that the values of the diffusion velocities computed by Methods I and II agree to about 1%. In contrast, the values of the diffusion velocities computed by Methods III and IV differ from those computed by Method I by much more (typical differences are around 40%). This comparison implies that Method II (i.e., the Stefan-Maxwell equations) is much more accurate in determining the values for the diffusion velocities than the non-matrix methods. Note that this conclusion is valid only for the case of zero temperature gradient.

For the other three groups of input to our auxiliary code, we find that the diffusion velocities computed by Method III are usually in better agreement with those computed by Method I than those computed by Method II! This situation can occur because in Method III the errors in ignoring thermal diffusion and in approximating the molecular diffusion velocities are generally of opposite sign. We conclude that it is a waste of effort to use a matrix method (such as the Stefan-Maxwell equations) to compute diffusion velocities unless thermal diffusion is also considered.

Method III is generally more accurate than Method IV. Method IV can be extremely inaccurate in computing the diffusion velocity for the

Nth species. In the cases considered we have found that the values computed by Method IV for N_2 differ, on the average, more than 100% from the values found by Method I. This is due to the procedure used to obtain the diffusion velocity for the Nth species. This procedure tends to associate cumulative errors caused by neglect of the constraint, Eq. (12), with the Nth species, here N_2 . We have found that Method III (the Boris and Oran procedure) is at least as accurate and in some cases substantially more accurate than the traditional Method IV for computing the V_i . Furthermore the Boris and Oran procedure involves very little additional computational effort.

V. A NEW TRANSPORT METHOD

For flames more complicated than $H_2-O_2-N_2$ we require a transport algorithm that is computationally efficient and relatively precise. The most exact procedure considered, Method I, can become prohibitively expensive for a large number of species. Method V is computationally efficient, but we feel caution is necessary in using such a simplified model. There does not seem to be a great deal to choose from among Methods II, III, and IV and so we have assembled a new method, Method VI.

As with Methods II-V we require expressions for λ_0 and for the $V_i (= V_i + W_i)$. For the thermal conductivity we use the simplest formula (20), since the exact choice does not appear to be important. For the molecular diffusion velocities V_i we use the expression in equation (17).

For problems with light species and steep temperature gradients, the neglect of thermal diffusion is often as important as the differences between the computational methods. So below we generate a technique that approximates the thermal diffusion contribution to the diffusion velocity, W_i . We shall first derive an expression for W_i of a binary mixture and then generalize the results.

For a binary mixture equation (2a) can be written

$$V_1 = - \frac{(1-Y_1)}{X_1 X_2} D_{12} \frac{\partial X_1}{\partial x} - \frac{D_1^T}{\rho Y_1} \frac{\partial \ln T}{\partial x} \quad (27)$$

from which we identify

$$W_1 = - \frac{D_1^T}{\rho Y_1} \frac{\partial \ln T}{\partial x} \quad (28)$$

Since, from Eq. (17),

$$v_1 = - \frac{(1-Y_1)}{X_1 X_2} D_{12} \frac{\partial X_1}{\partial x} \quad (29)$$

and since the thermal diffusion ratio is defined by reference 6

$$k_{12} = \frac{X_1 X_2}{\rho Y_1 Y_2} \frac{D_1^T}{D_{12}} \quad (30)$$

we can write, after some algebra,

$$w_1 = k_{12} v_1 \frac{\partial}{\partial x} (\ln T) / \frac{\partial X_1}{\partial x} \quad (31)$$

Theoretical expressions for k_{12} have been derived and even in the first approximation the expressions are quite complicated.⁶ For the special case of heavy isotopes, however, the first approximation simplifies to⁶

$$k_{12} = \frac{15(2A^* + 5)(6C^* - 5)(M_1 - M_2)}{2A^*(16A^* - 12B^* + 55)(M_1 + M_2)} X_1 X_2 \quad (32)$$

Fortunately Eq. (32) reproduces H₂-N₂ thermal diffusion ratios to within 30%, and so we use it as a simple but reasonable approximation for k_{12} . Equation (31) can now be evaluated (in the code).

Generalizing Eq. (31) we define

$$w_i = k_{im} v_i \frac{\partial}{\partial x} (\ln T) / \frac{\partial X_i}{\partial x} \quad (33)$$

If an expression for k_{im} can be obtained, then w_i of Eq. (33) can be evaluated. Chapman and Cowling³³ have derived an approximation for k_{im} ,

³³S. Chapman and T.G. Cowling, The Mathematical Theory of Non-Uniform Gases, Third Edition, Cambridge University Press (1970).

specifically

$$k_{im} = \sum_{\substack{j=1 \\ i \neq j}}^N k_{ij} \quad (34)$$

where k_{ij} is given by an expression analogous to Eq. (32).

From Eq. (32) we can see that the influence of ω_i will be the greater the larger the mass differences. Normally the thermal diffusion ratio does not exceed 0.1 and for the H_2 - O_2 - N_2 system, we have computed ω_i only for the species H and H_2 . The resulting diffusion velocities $V_i = V_i + \omega_i$ do not satisfy the constraint $\sum_{i=1}^N Y_i V_i = 0$. We use the Boris and Oran procedure discussed in Section II to obtain this condition.

Computationally, the quantity $15(2A^* + 5)/(2A^*(16A^* - 12B^* + 55))$ can be fitted very accurately by a function of the form: $a \exp(c/T^*)$. The quantity $(6C^* - 5)$ varies over the range zero to one and could not be fitted accurately by a simple expression. The fit for C^* given in Appendix D is used instead.

This new method for approximating multispecies transport has been exercised in our test flames. Table 4 compares the flame speeds for Methods I and VI. The results are so close that we infer that some of the errors made in the approximations involved in Method VI are cancelling.

Figure 5 compares the OH profiles for flame D and figure 6 compares the H_2 profiles for flame C. In general, for the minor species, the accuracy of Method VI is comparable to Methods II or III. However, in almost every profile involving a major species, the accuracy was improved.

VI. ADDENDUM

A few additional comparisons have recently been made. In the spirit of approximation exemplified in the discussion of Method V, the further assumption is sometimes made that all the Lewis numbers ($Le_i = \lambda/c_p \rho D_{im}$) are equal to unity. Given values for $\rho\lambda$ and c_p , this assumption defines the diffusion coefficients and removes the requirement of supplying independent information for them. We tested how well this additional level of simplification fared by applying it in the code using flame C. The computed flame speed was about 40% lower than for Method I. While the major species profiles were still reasonably close to those of Method I, they were noticeably less accurate than Method V. The minor species profiles showed large differences: the peak concentrations of O, HO_2 , and H_2O_2 were lower than those of Method I by about a factor of two.

In an effort to substantiate our earlier inference concerning the transfer of these results to other (hydrocarbon) flames we performed some checks on the stoichiometric methane-air flame. For this flame we used the input parameters listed by Tsatsaronis,¹³ the kinetics scheme was used as listed, and we made no attempt to critically evaluate it. The flame speeds computed for Methods I, V, and VI are in the ratio 1.00 to 0.88 to 0.94, respectively. The profiles for Method VI are more accurate than those produced by Method V. These results follow the same trend as in the $H_2-O_2-N_2$ flames reported above.

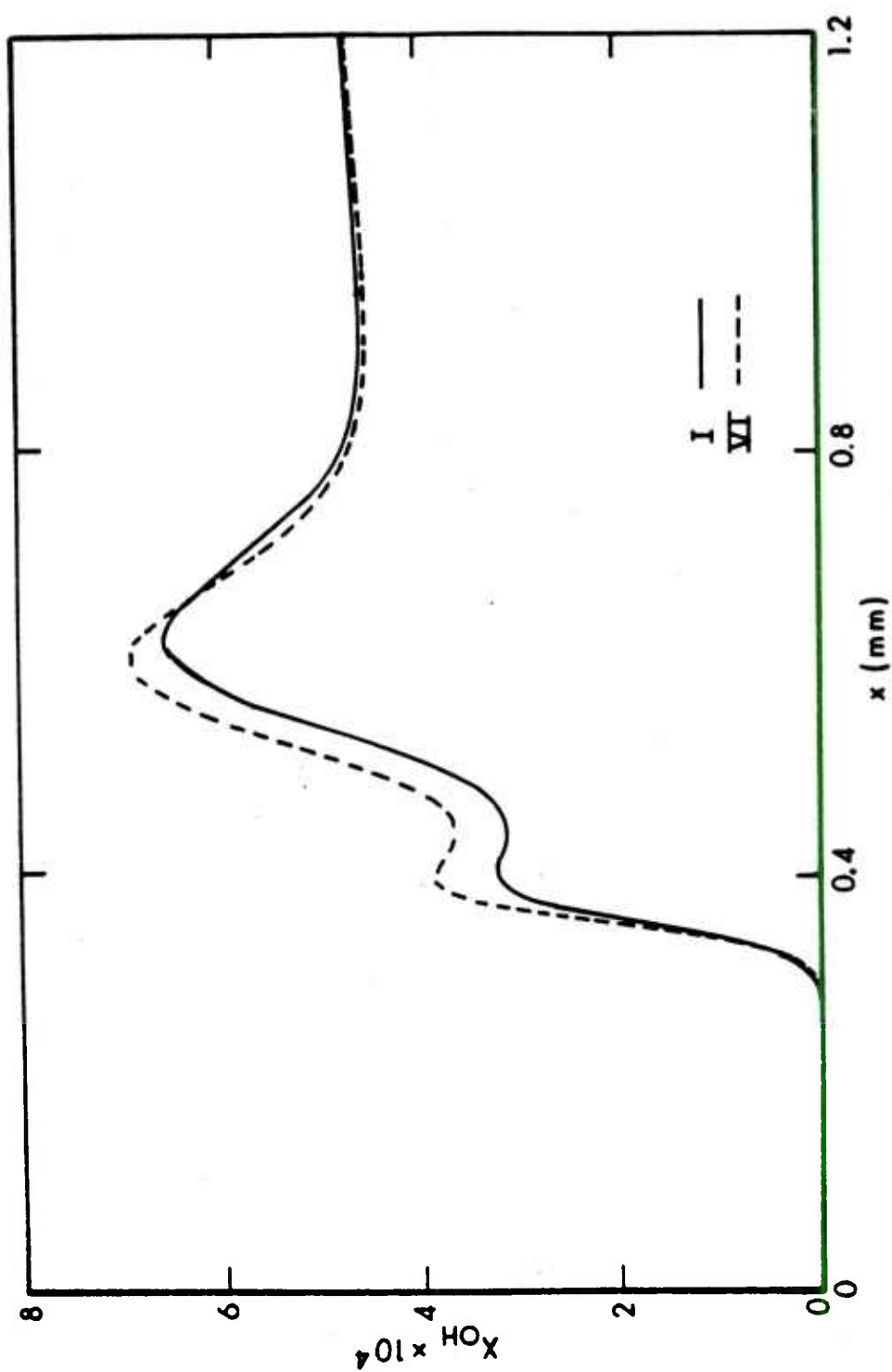


Figure 5. The OH Profile for Flame D.

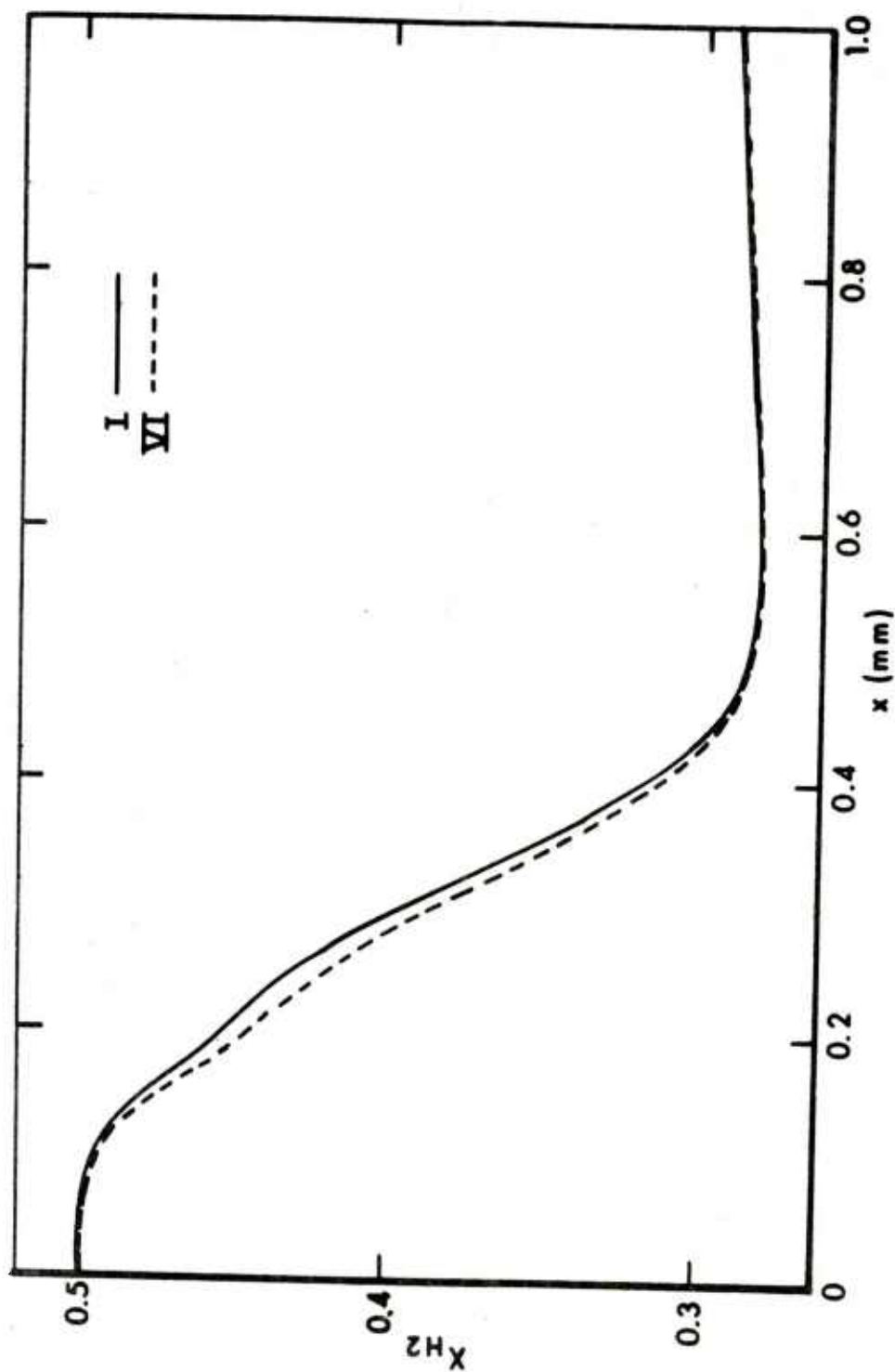


Figure 6. The H_2 Profile for Flame C.

TABLE 4. FLAME SPEEDS CALCULATED USING TWO TRANSPORT MODELS

<u>Flame</u>	<u>I</u>	<u>VI</u>
A	14.1	14.0
B	98	97
C	292	292
D	378	402
E	892	894

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APPENDIX A. THE FLAME EQUATIONS

We are interested in the equations that describe a one-dimensional, laminar, premixed flame that propagates in an unbounded ideal gas. The effects of radiation, viscosity, and body forces are ignored. Since the burning velocity is small compared with the local speed of sound, the pressure is taken to be constant. The resulting equations (see for example reference 2 of text) are:

Overall Continuity:

$$\rho \frac{\partial \rho}{\partial t} + \frac{\partial (\rho u)}{\partial x} = 0 \quad . \quad (A-1)$$

Continuity of Species:

$$\rho \frac{\partial Y_i}{\partial t} + \rho u \frac{\partial Y_i}{\partial x} = - \frac{\partial}{\partial x} (\rho Y_i V_i) + R_i M_i, \quad i = 1, \dots, N \quad . \quad (A-2)$$

and Conservation of Energy:

$$\rho c_p \frac{\partial T}{\partial t} + \rho u c_p \frac{\partial T}{\partial x} = - \frac{\partial q}{\partial x} + \sum_{i=1}^N h_i \left[\frac{\partial (\rho Y_i V_i)}{\partial x} - R_i M_i \right] \quad . \quad (A-3)$$

The boundary conditions are the following ($t \geq 0$). For $x = -\infty$;

$$T = T_u \quad \text{and} \quad Y_i = Y_{iu} \quad (i=1, \dots, N) \quad , \quad (A-4)$$

and for $x = \infty$;

$$\frac{\partial T}{\partial x} = \frac{\partial Y_i}{\partial x} = 0 \quad (i=1, \dots, N) \quad . \quad (A-5)$$

The transport properties that we are interested in are the diffusion velocities V_i and the heat flux q .

APPENDIX B. $\text{H}_2\text{-O}_2\text{-N}_2$ INPUT PARAMETERS

The required input data for the $\text{H}_2\text{-O}_2\text{-N}_2$ flames are for the most part taken from Warnatz (see reference 18 of text).

The kinetic scheme consists of thirty reactions and has been taken in toto from Warnatz' Table 3, which for the most part was taken from the Leeds review.¹ Our interest here is a study of the effects of using different transport algorithms, and not a critical evaluation of the kinetics. So we have uncritically used Warnatz' mechanism. This mechanism is in reasonable agreement with experimental data.

The enthalpies and heat capacities are evaluated using the sixth order polynomial fits of Gordon and McBride (see reference 4 of text). These reproduce the JANNAF (see reference 3 of text) values to within a few parts per thousand over the temperature range 300K-3000K.

The transport parameters are given in Table B-2. These are from Warnatz except for ξ_{ii}^∞ for OH, which is from Dixon-Lewis (see reference 12 of text). The values for σ and ϵ/k are obtained from viscosity measurements.

The manipulation of these parameters is discussed in Appendix D.

^{B1}D. L. Baulch, D. D. Drysdale, D. G. Horne, and A. C. Lloyd, Evaluated Kinetic Data for High Temperature Reactions, Vol. 1, Butterworths, London 1972.

TABLE B-1. REACTIONS IN THE $\text{H}_2\text{-O}_2\text{-N}_2$ SYSTEM

NO	REACTION	A*	B	C
1	$\text{OH} + \text{H}_2 \rightarrow \text{H}_2\text{O} + \text{H}$	$2.2\text{E}13^{**}$	0	- 2590
2	$\text{H} + \text{H}_2\text{O} \rightarrow \text{OH} + \text{H}_2$	$9.3\text{E}13$	0	-10250
3	$\text{H} + \text{O}_2 \rightarrow \text{OH} + \text{O}$	$2.2\text{E}14$	0	- 8450
4	$\text{O} + \text{OH} \rightarrow \text{H} + \text{O}_2$	$1.0\text{E}13$	0	0
5	$\text{O} + \text{H}_2 \rightarrow \text{OH} + \text{H}$	$1.8\text{E}10$	1	- 4480
6	$\text{H} + \text{OH} \rightarrow \text{O} + \text{H}_2$	$8.3\text{E}09$	1	- 3500
7	$\text{OH} + \text{OH} \rightarrow \text{H}_2\text{O} + \text{O}$	$6.3\text{E}12$	0	- 550
8	$\text{O} + \text{H}_2\text{O} \rightarrow \text{OH} + \text{OH}$	$6.8\text{E}13$	0	- 9240
9	$\text{H} + \text{H} + \text{M}' \rightarrow \text{H}_2 + \text{M}'$	$9.0\text{E}17$	-1	0
10	$\text{H} + \text{OH} + \text{M}' \rightarrow \text{H}_2\text{O} + \text{M}'$	$2.2\text{E}22$	-2	0
11	$\text{H} + \text{O}_2 + \text{M}' \rightarrow \text{HO}_2 + \text{M}'$	$5.0\text{E}15$	0	500
12	$\text{H} + \text{HO}_2 \rightarrow \text{OH} + \text{OH}$	$2.5\text{E}14$	0	- 950
13	$\text{H} + \text{HO}_2 \rightarrow \text{H}_2 + \text{O}_2$	$2.5\text{E}13$	0	- 350
14	$\text{H} + \text{HO}_2 \rightarrow \text{H}_2\text{O} + \text{O}$	$1.5\text{E}13$	0	- 500
15	$\text{OH} + \text{HO}_2 \rightarrow \text{H}_2\text{O} + \text{O}_2$	$5.0\text{E}13$	0	- 500
16	$\text{O} + \text{HO}_2 \rightarrow \text{OH} + \text{O}_2$	$5.0\text{E}12$	0	- 500
17	$\text{OH} + \text{OH} + \text{M} \rightarrow \text{H}_2\text{O}_2 + \text{M}$	$9.1\text{E}14$	0	2550
18	$\text{H} + \text{H}_2\text{O}_2 \rightarrow \text{H}_2\text{O} + \text{OH}$	$3.2\text{E}14$	0	- 4500
19	$\text{HO}_2 + \text{HO}_2 \rightarrow \text{H}_2\text{O}_2 + \text{O}_2$	$8.5\text{E}12$	0	- 500
20	$\text{H}_2 + \text{M}' \rightarrow \text{H} + \text{H} + \text{M}'$	$8.8\text{E}14$	0	-48300
21	$\text{O} + \text{O} + \text{M} \rightarrow \text{O}_2 + \text{M}$	$7.0\text{E}13$	0	900
22	$\text{HO}_2 + \text{M}' \rightarrow \text{H} + \text{O}_2 + \text{M}'$	$7.0\text{E}15$	0	-23000
23	$\text{OH} + \text{OH} \rightarrow \text{HO}_2 + \text{H}$	$1.2\text{E}13$	0	-20200

TABLE B-1. REACTIONS IN THE $H_2-O_2-N_2$ SYSTEM (Cont'd)

<u>NO</u>	<u>REACTION</u>	<u>A*</u>	<u>B</u>	<u>C</u>
24	$HO_2 + H_2 \rightarrow H_2O_2 + H$	7.3E11	0	- 9400
25	$H + H_2O_2 \rightarrow H_2 + HO_2$	1.7E12	0	- 1900
26	$H_2O_2 + M \rightarrow OH + OH + M$	1.2E17	0	-22900
27	$O + H_2O_2 \rightarrow OH + HO_2$	2.8E13	0	- 3200
28	$O + H_2O_2 \rightarrow H_2O + O_2$	2.8E13	0	- 3200
29	$OH + H_2O_2 \rightarrow H_2O + HO_2$	1.0E13	0	- 910
30	$HO_2 + H_2O \rightarrow H_2O_2 + OH$	2.8E13	0	-16500

[M] = total concentration

[M'] = 6.0 [H₂O] + 1.0 [H₂] + 0.4 [O₂] + 0.4 [N₂]

* A is in units of $cm^3/mole\text{-}sec$ or $cm^6/mole^2\text{-}sec$, $k = AT^B \exp (C/T)$.

** $2.2E13 = 2.2 \times 10^{13}$.

TABLE B-2. MOLECULAR PARAMETERS USED FOR
THE DETERMINATION OF TRANSPORT PROPERTIES

<u>Species</u>	$\sigma [\text{\AA}]$	$\frac{\epsilon}{k} [\text{K}]$	$\mu [\text{Debye}]$	$\alpha [\text{\AA}^3]$	ξ_{ii}^∞
O	2.75	80	0	0	
O ₂	3.46	107	0	1.60	14.4
H	2.05	145	0	0	
H ₂	2.92	38	0	0.79	280
OH	2.75	80	0	0	4.5
H ₂ O	2.60	572	1.844	0	4.0
N ₂	3.62	97.5	0	0	15.7

HO₂, H₂O₂ like O₂

APPENDIX C. DEFINITION OF THE MATRIX L

The matrix L can be partitioned into nine N by N matrices

$$L = \begin{pmatrix} L^{00,00} & L^{00,10} & L^{00,01} \\ L^{10,00} & L^{10,10} & L^{10,01} \\ L^{01,00} & L^{01,10} & L^{01,01} \end{pmatrix} \quad (C-1)$$

where

$$L_{ii}^{00,00} = 0, \quad (C-2)$$

$$L_{ij}^{00,00} = \frac{16}{25} \frac{T}{P} \left[\frac{X_i X_j}{D_{ij}} + \sum_{k \neq i} \frac{M_j}{M_i} \frac{X_k X_j}{D_{ik}} \right], \quad i \neq j, \quad (C-3)$$

$$L_{ij}^{00,10} = - \frac{8T}{5P} \frac{M_j (1.2 C_{ij}^* - 1) X_i X_j}{(M_i + M_j) D_{ij}}, \quad i \neq j, \quad (C-4)$$

$$L_{ii}^{00,10} = - \sum_{j \neq i} L_{ji}^{00,10}, \quad (C-5)$$

$$L_{ij}^{10,00} = L_{ji}^{00,10}, \quad (C-6)$$

$$L_{ij}^{01,00} = L_{ij}^{00,01} = 0 \quad (C-7)$$

$$L_{ii}^{10,10} = - \frac{16}{15} \frac{M_i}{R} \frac{X_i^2}{\eta_i} \left(1 + \frac{10}{3\pi} \frac{C_{i, \text{rot}}}{R \xi_{ii}} \right) - \frac{16T}{25P} \sum_{k \neq i} \left\{ \frac{X_i X_k}{(M_i + M_k)^2 D_{ik}} \times \right. \\ \left. \left[\frac{15}{2} M_i^2 + \frac{25}{4} M_k^2 - 3 M_k^2 B_{ik}^* + 4 M_i M_k A_{ik}^* \left(1 + \frac{5}{3\pi} \right. \right. \right. \\ \left. \left. \left. \left\{ \frac{C_{i, \text{rot}}}{R \xi_{ik}} + \frac{C_{k, \text{rot}}}{R \xi_{ik}} \right\} \right) \right] \right\}, \quad (C-8)$$

$$L_{ij}^{10,10} = \frac{16T}{25P} \frac{M_i M_j X_i X_j}{(M_i + M_j)^2 D_{ij}}$$

$$\left\{ \frac{55}{4} - 3 B_{ij}^* - 4 A_{ij}^* \left[1 + \frac{5}{3\pi} \left(\frac{C_{i, \text{rot}}}{R \xi_{ij}} + \frac{C_{j, \text{rot}}}{R \xi_{ji}} \right) \right] \right\}, \quad i \neq j \quad (C-9)$$

$$L_{ii}^{10,01} = \frac{16M_i X_i^2 C_{i, \text{rot}}}{3\pi R \eta_i C_{i, \text{int}} \xi_{ii}}$$

$$+ \frac{32 T}{5\pi p C_{i, \text{int}}} \sum_{k=i} \frac{M_i A_{ik}^* X_i X_k C_{i, \text{rot}}}{(M_i + M_k) D_{ik} \xi_{ik}}, \quad (C-10)$$

$$L_{ij}^{10,01} = \frac{32 T M_j A_{ij}^* X_i X_j C_{j, \text{rot}}}{5 p \pi C_{j, \text{int}} (M_i + M_j) D_{ji} \xi_{ji}} \quad (C-11)$$

$$L_{ij}^{01,10} = L_{ji}^{10,01}, \quad (C-12)$$

$$L_{ij}^{01,10} = 0, \quad i \neq j \quad (C-13)$$

and

$$L_{ii}^{01,01} = - \frac{8M_i X_i^2 C_{i, \text{rot}}}{\pi \eta_i \xi_{ii} C_{i, \text{int}}^2}$$

$$- \frac{4RT}{p C_{i, \text{int}}} \left\{ \sum_k \frac{X_i X_k}{D_{i, \text{int}, k}} \right.$$

$$\left. + \sum_{k \neq i} \frac{12 M_i A_{ik}^* X_i X_k C_{i, \text{rot}}}{5\pi M_k D_{ik} C_{i, \text{int}} \xi_{ik}} \right\}. \quad (C-14)$$

When solving equations (7) and (6) for the thermal conductivity, λ_0 will turn out to have the units $\text{cm}^2\text{-atm-s}^{-1}\text{-K}^{-1}$. To convert to the more usual units of $\text{cal-cm}^{-1}\text{-s}^{-1}\text{-K}^{-1}$, we multiply by $R/R_a = 1.9872/82.05$.

APPENDIX D. MANIPULATION OF TRANSPORT DATA

The quantities required to compute the elements of the matrix L used in Method I can be calculated from the transport parameters (Table B-2) and the heat capacities (see reference 4 of text). We shall discuss the procedures in this appendix.

The viscosity η_i and the binary diffusion coefficients D_{ij} can be obtained from Lennard-Jones (non-polar) or Stockmayer (polar) parameters σ_k and ϵ_k/k . For polar molecules (here only H_2O) we also need the dipole moment μ_i . For the binary diffusion coefficient of a polar and a non-polar species, we also need the polarizability α_i of the non-polar species. Then η_i and D_{ij} are calculated using tabulated values of the collision integrals^{1,2} (see also reference 6 of text).

The quantities A^*_{ij} , B^*_{ij} , and C^*_{ij} do not have exactly their standard meanings (see reference 9 of text). However, they can be closely approximated by the usual quotients of collision integrals. For Lennard-Jones parameters, these are tabulated in reference 6 of text. For simplicity, we will assume that at most one of the species is polar (in our case H_2O). Since a polar molecule interacting with a non-polar molecule can be represented by a Lennard-Jones potential, all the quantities A^*_{ij} , B^*_{ij} , and C^*_{ij} can be cast into the Lennard-Jones formalism. They are functions only of $T^*_{ij} = T/(\epsilon_{ij}/k)$, where ϵ_{ij} is obtained from ϵ_i and ϵ_j by standard combining rules¹ (see also reference 6 of text).

The collision numbers ξ_{ij} for rotational relaxation of species i on colliding with species j are difficult to obtain, particularly if $i \neq j$. Fortunately, these values are not critical. For simplicity, we will assume that $\xi_{ij} = \xi_{ii}$. Parker³ has calculated values for ξ_{ii} for homonuclear diatomic molecules, as well as the temperature relation

$$\xi_{ii} = \xi_{ii}^{\infty} \left[1 + \frac{\pi^{3/2}}{2(T_i^*)^{1/2}} + \left(\frac{\pi^2}{4} + \pi \right) \frac{1}{T_i^*} \right]^{-1} \quad (D-1)$$

We use his values for O_2 and N_2 . For other types of molecules, we must look for experimental values. In this paper, we take these other ξ_{ii} 's to be constant. The values for ξ_{ii} are taken from Warnatz (see reference 14 of text) except the value of ξ_{ii} for OH (see reference 12 of text).

^{D1} R. C. Reid and T. K. Sherwood, *The Properties of Gases and Liquids*, 2nd Edition, McGraw-Hill, NY, (1966).

^{D2} L. Monchick and E. A. Mason, "Transport Properties of Polar Gases", *J. Chem. Phys.*, 33, 1676-1697 (1961).

The quantities $\mathcal{D}_{i,int,j}$ refer to the diffusion of internal energy, which is approximated by \mathcal{D}_{ij} . More accurate values are very difficult to calculate, and there is no known way of determining them experimentally (see reference 9 of text).

To obtain the $C_{i,rot}$ and $C_{i,int}$, we need to properly partition $C_{i,v}$, the heat capacity at constant volume. $C_{i,v}$ can be calculated from the Gordon and McBride polynomial fits (see reference 4 of text). It can be partitioned as

$$C_{i,v} = C_{i,tr} + C_{i,int}, \quad (D-2)$$

where $C_{i,tr} = 1.5 R$. The internal energy can be further partitioned into rotational and vibrational energy. $C_{i,rot} = 0$ for a monatomic molecule, $C_{i,rot} = R$ for a linear molecule, and $C_{i,rot} = 1.5 R$ for a polyatomic molecule.

For Method I, we do not need to directly compute the separate species thermal conductivities λ_i . These values are required for the other methods, so we will discuss them here.

For monatomic gases,

$$\lambda_i^{mon} = \frac{15}{4} \frac{R}{M_i} \eta_i, \quad (D-3)$$

where a hard sphere model has been assumed¹ (see also reference 6 of text).

For polyatomic gases, there are many procedures. We will follow the analysis of Mason and Monchick,^{1,4} and write

$$\frac{\lambda_i M_i}{\eta_i} = f_{tr} C_{i,tr} + f_{int} C_{i,int} \quad (D-4)$$

where

^{D3} J. G. Parker, "Rotational and Vibrational Relaxation in Diatomic Gases", *Phys. Fluids*, 2, 449-462 (1959).

^{D4} E. A. Mason and L. Monchick, "Heat Conductivity of Polyatomic and Polar Gases", *J. Chem. Phys.*, 36, 1622-1639 (1962).

$$f_{tr} = \frac{5}{2} \left[1 - \frac{10}{3\pi} \left(1 - \frac{2}{5} \frac{M_i \rho \mathcal{D}_{i,int,i}}{\eta_i} \right) \left(\frac{C_{i,rot}}{R \xi_{ii}(rot)} + \frac{C_{i,vib}}{R \xi_{ii}(vib)} \right) \right] , \quad (D-5)$$

$$f_{int} = \frac{M_i \rho \mathcal{D}_{i,int,i}}{\eta_i} \left[1 + \frac{5}{\pi} \left(1 - \frac{2}{5} \frac{M_i \rho \mathcal{D}_{i,int,i}}{\eta_i} \right) \left(\frac{C_{i,rot}}{C_{i,int} \xi_{ii}(rot)} + \frac{C_{i,vib}}{C_{i,int} \xi_{ii}(vib)} \right) \right] . \quad (D-6)$$

Normally, $\xi_{ii}(vib) \gg \xi_{ii}(rot)$, so we will ignore the vibrational term. We then refer to $\xi_{ii}(rot)$ just as ξ_{ii} . As usual, we approximate $\mathcal{D}_{i,int,i}$ by the self diffusion coefficient \mathcal{D}_{ii} .

Using either Lennard-Jones or Stockmayer collision integrals,

$$\frac{M_i \rho \mathcal{D}_{ii}}{\eta_i} = 1.1999 A^* \approx 1.32. \quad (D-7)$$

Equation (D-4) then simplifies to

$$\frac{\lambda_i M_i}{\eta_i} = 1.32 C_{i,v} + 1.77R - .886 \frac{C_{i,rot}}{\xi_{ii}} . \quad (D-8)$$

As before, the exact value of ξ_{ii} is not critical in the computation.

For actual use in the code, a fit to the η_i , λ_i , and \mathcal{D}_{ij} is made of the form aT^b over an appropriate temperature range, using the logarithmic method with proper transformation of weights.⁵ The resulting fits are accurate within two percent.

^{D5} R. J. Cvetanovic and D. L. Singleton, *Internat. J. Chem. Kinet.*, 9, 481-488, 1977; R. J. Cvetanovic and D. L. Singleton, *Internat. J. Chem. Kinet.*, 1007-1009, 1977.

The quantities A^* , B^* , and C^* are fit over a range $1.0 \leq T^* \leq 400$. This covers the range likely to occur in a flame. If the fit is extended to values of $T^* < 1$, the accuracy suffers. A^* can be fit very accurately by a function of the form: $a(T^*)^b$. To fit B^* and C^* accurately, we need to use the functional form: $a \exp(c/T^*)$ (see Table D-1).

Given the above information, we have developed software to write the actual transport subroutine used in the code.

TABLE D-1. FITS TO THE FUNCTIONS A^* , B^* , C^*
($a(T^*)^b$ or $a \exp(c/T^*)$)

Function	a	b	c
A^*	1.0885	$9.0557E-3$	0
B^*	1.0786	0	$8.5001E-2$
C^*	.95426	0	- .14357

APPENDIX E. PROGRAM LISTINGS

We have included here the FORTRAN programs for writing the transport subroutines, as well as examples of the subroutines themselves. Some of these routines are very long for the H_2 - O_2 - N_2 system (over 3500 lines for Method I). So as an example we have considered a binary mixture of H_2 and N_2 . This shows the main features of the programs while conserving space.

A copy of the actual flame code used is given in reference 23 of the text. Method V (constant transport) is included in this code as the default. The appropriate constant transport values for a given flame must be read in, but the subroutine itself is not rewritten.

For our other transport methods, the subroutine is written specifically for a given set of chemical species. The procedure is straightforward. We attach to TAPE15 the coefficients for computing the thermodynamic quantities. We attach to TAPE9 the least squares fits for the viscosities, thermal conductivities, and binary diffusion coefficients. There are computed in another program using the methods discussed in this article. The program also requires the appropriate Lennard-Jones (Stockmayer) parameters, the pressure, and for some methods the least squares fits for A^* , B^* , and C^* . The flame code actually works with non-dimensional forms of the flame equations, so appropriate normalization terms for the space coordinate, time coordinate, and temperature must also be supplied.

The transport statements are written onto TAPE3. This tape is read and attached to a standard set of initial statements. The corresponding FORTRAN subroutine F can then be attached to the flame code.

Given the mass fractions, the non-dimensional temperature, and their first and second space derivatives, F computes the corresponding time derivatives. The needed chemistry terms are found by calling the subroutine RT. This subroutine is also written by a FORTRAN program (see reference 22 of text).

For details on the actual form of the equations used and the connections between F and the rest of the flame code, see reference 23 of the text.

The listing that follows gives the FORTRAN program (MAIN) and the corresponding transport subroutines for a binary mixture of H_2 and N_2 (F) for Methods I, II, III, IV and VI.

```

1  PROGRAM LOADF(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,
    * TAPE3,TAPE9,TAPE15)
2  C  LOADF CREATES THE SUBROUTINE F IN PDECOL-FLCT.
3  DIMENSION II(72)
4  DIMENSION LH(25),W(25),AU(7,25),AL(7,25)
5  DIMENSION ALD(25),BLD(25),ABD(25,25),HBD(25,25)
6  DIMENSION LBPR(25)
7  DIMENSION III(44)
8  DIMENSION LBROT(25),SGA(25),ESK(25),UM(25),ALP(25),ZROT(25),DF(25)
9  DIMENSION LD(25),LDV(25)
10 DIMENSION AV(25),BV(25)
11 DIMENSION E(25,25)
12 WRITE(3,1000)
13 I000 FORMAT(1HC,2X,34HWE WANT TO AVOID DIVISION BY ZERO. )
14 WRITE(3,1012)
15 I012 FORMAT(6X,14HDO 5 K=1,NPDEM)
16 WRITE(3,1014)
17 I014 FORMAT(6X,32HIF(ABS(U(K)),LT.SMALL)U(K)=SMALL )
18 WRITE(3,1016)
19 I016 FORMAT(1X,1H5,4X,36HIF(ABS(UPH(K)),LT.SMALL)UPH(K)=SMALL )
20 READ(5,12)NLINE
21 I2 FORMAT(1014)
22 C  NLINE IS THE NUMBER OF COMMENT LINES TO BE READ AND PRINTED.
23 DO 20 K=1,NLINE
24 READ(5,22)I1
25 WRITE(3,22)I1
26 CONTINUE
27 I20 CONTINUE
28 I22 FORMAT(72A1)
29 I24 FORMAT(1X,72A1/)
30 READ(5,12)NSPC
31 NM=NSPC-1
32 LBM=IH-
33 LBU=2HU(
34 LBP=IH)
35 WRITE(3,1020)((LHM,LBU,K,LBP),K=1,NM)
36 I020 FORMAT(6X,6HYN=1.0,8(A1,42,12,A1),A1,2(/5X,1H*,1X,
    * 8(A2,12,A1,A1)) )
37 WRITE(3,1025)
38 I025 FORMAT(6X,33HCALL RT(U,YN,R,NPDE,KPDE,IC,KSKR) )
39 WRITE(3,18)NSPC
40 I18 FORMAT(6X,4HIST=12,7H*(IC-I) )
41 C  ASSUME AT MOST ONE POLAR SPECIES. (DIPOLE MOMENT NON-ZERO).
42 C  THEN A* AND B* CAN BE APPROXIMATED BY LENNAK-D-JONES COLLISION
43 C  INTEGRALS, EVEN IF THE INPUT PARAMETERS ARE STUCKMAYER.
44 DO 30 K=1,NSPC
45 HEAD(5,32) LR(K),W(K),DF(K),SGA(K),ESK(K),UM(K),ALP(K),ZROT(K),
    * LBROT(K)
46 WRITE(6,34)K,LR(K),W(K),DF(K),SGA(K),ESK(K),UM(K),ALP(K),ZROT(K),
    * LBROT(K)
47 HEAD(15,36)(AU(L,K),L=1,5),(III(L),L=1,5)
48 WRITE(6,36)(AU(L,K),L=1,5),(III(L),L=1,5)
49 READ(15,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(III(L),L=1,5)
50 WRITE(6,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(III(L),L=1,5)
51 HEAD(15,37)(AL(L,K),L=4,7),(III(L),L=1,20)
52 WRITE(6,37)(AL(L,K),L=4,7),(III(L),L=1,20)
53 CONTINUE
54 I30 HEAD(5,232)1PN,PHN,TMN
55

```

```

232 FORMAT(IP3E12.4)
C THE ROWS AND COLUMNS CORRESPONDING TO INTERNAL EFFECTS FOR MONATOMICS
C ARE SKIPPED. LD KEEPS TRACK OF WHICH ROW OR COLUMN IS BEING
C WORKED ON.
LD(I)=1
IF (DF(1).EQ.0.0)LD(1)=0
DO 38 L=2,NSPC
LM=L-1
LD(L)=LD(LM)+1
IF (DF(L).EQ.0.0)LD(L)=LD(L)-1
CONTINUE
38
32 FORMAT(A5,7F7.0,A5)
34 FORMAT(/2X,14,4X,A5,4X,7F8.2,4X,A5/)
36 FORMAT(5E15.8,5A1)
37 FORMAT(4E15.8,20A1)
WRITE(3,1100)IPN
FORMAT(6X,13HDT=UPH(NPDE)*,IPE14.6)
WRITE(3,27)
FORMAT(6X,22HIF(KSK1.GT.1)GO TO 100)
WRITE(3,28)
FORMAT(6X,22HIF(KSKR.GT.1)GO TO 125 )
READ(5,12)NLINE
DO 40 K=1,NLINE
READ(5,22)11
WRITE(3,22)11
40 CONTINUE
C *****
C ENTHALPIES AND HEAT CAPACITIES.
C *****
WRITE(3,42)
FORMAT(6X,24HIF(T.GT.1000.)GO TO 2000)
DO 50 K=1,NSPC
WRITE(3,52)K,AL(1,K),AL(2,K)
WRITE(3,54)(AL(L,K),L=3,5)
A=AL(2,K)
B=AL(3,K)*2.0
C=AL(4,K)*3.0
D=AL(5,K)*4.0
WRITE(3,1112)K,A,B,C,D
1112 * 2(4H+T*(,1PE16.8,7H)))*DT )
FORMAT(6X,24HDC,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8,5X,1H*,1X,
* 2(4H+T*(,1PE16.8,7H)))*DT )
WRITE(3,62)K,AL(6,K),AL(1,K)
WRITE(3,64)AL(2,K),AL(3,K)
WRITE(3,66)AL(4,K),AL(5,K)
CONTINUE
50
52 FORMAT(6X,1HC,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
54 FORMAT(5X,1H*,1X,3(4H+T*(,1PE16.8,5H))))
WRITE(3,56)
FORMAT(6X,10HG TO 3000)
WRITE(3,58)
FORMAT(4H2000,2X,8HCONTINUE)
58
DO 60 K=1,NSPC
WRITE(3,52)K,AU(1,K),AU(2,K)
WRITE(3,54)(AU(L,K),L=3,5)
A=AU(2,K)
B=AU(3,K)*2.0
C=AU(4,K)*3.0

```

```

115      D=AU(5,K)*4.0
        WHITE(3,1112)K,A+B,C,D
        WHITE(3,62)K,AU(6,K),AU(1,K)
        WHITE(3,64)AU(2,K),AU(3,K)
        WHITE(3,66)AU(4,K),AU(5,K)
120      CONTINUE
        60      FORMAT(6X,1HH,I2,9H=1.9872*(,IPEI6.8,4H+T*(,IPEI6.8)
        62      FORMAT(5X,1H*,1X,4H+1*(,IPEI6.8,4H/2.0,4H+1*(,IPEI6.8,4H/3.0)
        64      FORMAT(5X,1H*,1X,4H+1*(,IPEI6.8,4H/4.0,4H+1*(,IPEI6.8,
        66      * 4H/5.0,4H))))))
125      WHITE(3,68)
        FORMAT(4H3000,2X,8HCONTINUE)
        68      WHITE(3,134)
        FORMAT(1HC,2X,39HSPECIFIC HEATS AND SPECIFIC ENTHALPIES. )
130      DO 140 K=1,NSPC
        134      WRITE(3,142)K,K,W(K)
        1116     FORMAT(6X,7HDC(1ST+,I2,4H)=DC,I2,1H,F6.2)
        140      WRITE(3,144)K,K,W(K)
        142      CONTINUE
        144      FORMAT(6X,6HC(1ST+,I2,3H)=C,I2,1H,F6.2)
        146      FORMAT(6X,6HH(1ST+,I2,3H)=H,I2,1H,F6.2)
        148      WRITE(3,146)
        146      FORMAT(1X,3H125,2X,8HCONTINUE)
        C *****
        C THERMAL CONDUCTIVITIES AND BINARY DIFFUSION COEFFICIENTS.
        C READ IN VISCOSITY, THERMAL CONDUCTIVITY, AND BINARY DIFFUSION
        C COEFFICIENTS FROM A FILE CREATED BY VALUES, CY=5.
        C *****
        145      READ(5,12)NLINE
        DO 72 K=1,NLINE
        147      READ(5,22)I1
        148      WRITE(3,22)I1
        149      CONTINUE
        150      FORMAT(1HC,5X,1HV,I2,1H=,IPEI4.6,5H*(I**,IPEI4.6,1H) )
        152      READ(5,12)NLINE
        DO 70 K=1,NLINE
        153      READ(5,22)I1
        154      WRITE(3,22)I1
        155      CONTINUE
        DO 80 K=1,NSPC
        156      READ(9,82)AV(K),BV(K),I11
        157      WRITE(6,84)K,LB(K),AV(K),BV(K),I11
        158      READ(9,82)ALD(K),BLD(K),I11
        159      WRITE(6,84)K,LB(K),ALD(K),BLD(K),I11
        160      CONTINUE
        80      FORMAT(1P2EI4.6,44A1)
        82      FORMAT(1/2X,I4,4X,A4,4X,IP2EI4.6,44A1/)
        84      DO 76 K=1,NSPC
        165      WRITE(3,78)K,AV(K),BV(K)
        76      DO 90 K=1,NSPC
        166      WRITE(3,92)K,ALD(K),BLD(K)
        90      CONTINUE
        92      FORMAT(1HC,5X,2HVL,I2,1H=,IPEI4.6,5H*(I**,IPEI4.6,1H) )
        READ(5,12)NLINE
        DO 100 K=1,NLINE
        170      READ(5,22)I1

```

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PROGRAM LOADF 76/76 OPT=1 ROUND=**/ TRACE FTN 4.8+498

```

175      100      WRITE(3,22)111
              CONTINUE
              NM=NSPC-1
              DO 110 I=1,NSPC
                DO 110 J=1,NSPC
                  READ(9,82)ABD(1,J),HBD(1,J),111
                  WRITE(6,112)1,J,LB(1),LB(J),ABD(1,J),HBD(1,J),111
                CONTINUE
              110 FORMAT(/2X,14,4X,14,4X,A4,4X,A4,4X,1P2E14.6,44A1/)
              112 HEAD(S,114)PRESS
              114 FORMAT(F6.0)
              WRITE(3,116)PRESS
              116 FORMAT(1HC,2X,7HPRESS =,F6.2)
              DO 120 I=1,NSPC
                DO 120 J=1,NSPC
                  ABD(1,J)=ABD(1,J)/PRESS
                  WRITE(3,122)1,J,ABD(1,J),HBD(1,J)
                CONTINUE
              120 FORMAT(1HC,5X,1HD,212,1H=,1PE14.6,5SH*(T**,1PE14.6,1H) )
              122 C *****
              C SPACE DERIVATIVES.
              C *****
              195      LHPL=1H+
              WRITE(3,148)
              148 FORMAT(1HC,2X,42HDEFINE USEFUL COMBINATIONS AND DERIVATIVES )
              NS=NSPC+1
              WRITE(3,149)NS
              149 FORMAT(6X,4HYS=Y,12)
              DO 150 K=1,NSPC
                WRITE(3,152)K,K
              150 CONTINUE
              152 FORMAT(6X,1HX,12,2H=Y,12,3H/Y5)
              DO 160 K=1,NM
                WRITE(3,162)K,K
                WRITE(3,164)K,K
                WRITE(3,166)K,K
              160 CONTINUE
              162 FORMAT(6X,1HU,12,3H=U(,12,1H) )
              164 FORMAT(6X,2HOU,12,5H=UPH(,12,1H) )
              166 FORMAT(6X,3HODU,12,6H=UPH2(,12,1H) )
              LBU=1HU
              172 WRITE(3,172)NSPC,((LBM,LBU,K),K=1,NM)
              215      172 FORMAT(6X,1HU,12,4H=1.0,8(A1,A1,12),A1,2(/5X,1H*,1X,
                * 8(A1,12,A1) )
              LBDU=2HOU
              174 WRITE(3,174)NSPC,((LBM,LBDU,K),K=1,NM)
              220      174 FORMAT(6X,2HOU,12,1H=,8(A1,A2,12),A1,2(/5X,1H*,1X,
                * 8(A2,12,A1) )
              LHODU=3HODU
              176 WRITE(3,176)NSPC,((LBM,LHODU,K),K=1,NM)
              225      176 FORMAT(6X,3HODU,12,1H=,8(A1,A3,12),A1,2(/5X,1H*,1X,
                * 8(A3,12,A1) )
              DO 180 K=1,NSPC
                WRITE(3,182)K,K,w(K)
              180 CONTINUE
              182 FORMAT(6X,2HDY,12,3H=1HU,12,1H/Y,12,2)

```



```

230      LBDY=2HDY
      WRITE(3,186)((LPL,LBDY,K),K=1,NSPC)
      FORMAT(6X,4HDYS=,8(A1,A2,I2),A1,2(/5X,IH*,IX,8(A2,I2,A1)) )
      DO 190 K=1,NSPC
      WRITE(3,188)K,K,W(K)
      FORMAT(6X,3HDY,I2,4H=000,I2,1H/,F6.2)
      CONTINUE
      LBDY=3HDY
      WRITE(3,192)((LPL,LBDY,K),K=1,NSPC)
      FORMAT(6X,5HDYS=,5(A1,A3,I2),A1,2(/5X,IH*,IX,5(A3,I2,A1)) )
      PSK=PRESS/82.05
      WRITE(3,234)TPN,PHN,TMN
      WRITE(6,234)TPN,PHN,TMN
      * SHTMN =,IPEI2.4)
      WRITE(3,242)PSR
      FORMAT(6X,5SHDRH=,,IPE20.12,2IH*(UT/T+DYS/YS)/(T*YS) )
      WRITE(3,1202)
      FORMAT(6X,I6HDYS=DYS/(YS*YS) )
      WRITE(3,194)
      DO 1250 K=1,NSPC
      WRITE(3,1204)K,K,K
      FORMAT(6X,2HDX,I2,3H=DY,I2,5H/YS-Y,I2,5H*UDYSY )
      WRITE(3,196)K,K,K,K,K
      FORMAT(6X,3HDDX,I2,5H=(DDY,I2,7H-2.0*DY,I2,13H*UDYS/YS,2.0*Y,I2,
      * 9H*UDYSQ-Y,I2,12H*UDYS/YS)/YS )
      C ZROT HAS BEEN READ IN AT T = INFINITY.
      C IF LBROT = 5H CNST, THEN TREAT ZROT AS A CONSTANT.
      C IF LBROT = 5H VAR, THEN USE THE FORMULA OF PARKER FOR THE
      C TEMPERATURE DEPENDENCE.
      PI=2.0*ACOS(0.0)
      LBVR=5H VAR
      LBCN=5H CNST
      IF (DF(K).EQ.0.0)GO TO 1210
      B=SQRT(PI*PI*PI*ESK(K))/2.0
      C=(PI*PI/4.0*PI)*ESK(K)
      A=DF(K)/(2.0*ZROT(K))
      B=A*B
      C=A*C
      * WRITE CROT/ZROT
      IF (LBROT(K).EQ.LBVR)WRITE(3,1206)K,A,B,C
      1206      * 8HSQRT(T)+,IPE20.12,1H/,IPE20.12,1H/,5X,IH*,IX,
      IF (LBROT(K).EQ.LBCN)WRITE(3,1207)K,A
      1207      * 8HSQRT(T)+,IPE20.12,1H/,IPE20.12,
      B=B/2.0
      IF (LBROT(K).EQ.LBVR)WRITE(3,1120)K,B,C
      1120      * IPE19.12,RH/T)*DT/T )
      IF (LBROT(K).EQ.LBCN)WRITE(3,1121)K
      1121      * IPE19.12,RH/T)*DT/T )
      A=10.0/(3.0*PI)
      WRITE(3,1274)K,K,A,K
      * WRITE C INTERNAL.
      A=W(K)/1.9872
      231      MAIN
      232      MAIN
      233      MAIN
      234      MAIN
      235      MAIN
      236      MAIN
      237      MAIN
      238      MAIN
      239      MAIN
      240      MAIN
      241      MAIN
      242      MAIN
      243      MAIN
      244      MAIN
      245      MAIN
      246      MAIN
      247      MAIN
      248      MAIN
      249      MAIN
      250      MAIN
      251      MAIN
      252      MAIN
      253      MAIN
      254      MAIN
      255      MAIN
      256      MAIN
      257      MAIN
      258      MAIN
      259      MAIN
      260      MAIN
      261      MAIN
      262      MAIN
      263      MAIN
      264      MAIN
      265      MAIN
      266      MAIN
      267      MAIN
      268      MAIN
      269      MAIN
      270      MAIN
      271      MAIN
      272      MAIN
      273      MAIN
      274      MAIN
      275      MAIN
      276      MAIN
      277      MAIN
      278      MAIN
      279      MAIN
      280      MAIN
      281      MAIN
      282      MAIN
      283      MAIN
      284      MAIN
      285      MAIN
      286      MAIN

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FTN 4.8+49H

76/76 OPT=1 ROUND=-*/ TRACE

PROGRAM LOADF

```

1212 WRITE(3,I2I2)K,K,A
      FORMAT(6X,4HCINT,I2,7H=C(IST+,I2,2H)*,IPE20,I2,4H-2.5)
1124 WRITE(3,I124)K,K,A
      FORMAT(6X,5HDCINT,I2,8H=DC(IST+,I2,2H)*,IPE20,I2)
1216 WRITE(3,I216)K,K,K
      FORMAT(6X,3HCSC,I2,5H=CSZR,I2,5H/CINT,I2)
1128 WRITE(3,I128)K,K,K,K
      FORMAT(6X,4HOCSC,I2,7H=(DCSZR,I2,5H-CSZR,I2,6H*DCINT,I2,
      * 5H/CINT,I2,6H)/CINT,I2 )
      GO TO 1250
1210 CONTINUE
      WRITE(3,I272)K,K
      WRITE(3,I132)K,K
1250 CONTINUE
      DO 1300 I=1,NSPC
      DO 1300 J=1,NSPC
1254 WRITE(3,I254)I,J,I,J
      FORMAT(6X,IHX,2I2,2H=X,I2,2H*X,I2)
1256 WRITE(3,I256)I,J,I,J,I,J
      FORMAT(6X,2HDX,2I2,3H=DX,I2,2H*X,I2,2H*X,I2,3H*DX,I2)
      A=1.0/ABD(I,J)
      B=-BRO(I,J)
      C WRITE THE RECIPROCAL OF THE BINARY DIFFUSION COEFFICIENT.
      WRITE(3,I258)I,J,A,B
1258 FORMAT(6X,2HVD,2I2,IH=,IPE20,I2,6H*(I**,(IPE14,6,2H) )
      A=A*B
      B=B-I.0
1262 WRITE(3,I262)I,J,A,B
      FORMAT(6X,3HVD,2I2,IH=,IPE20,I2,6H*(I**,(IPE14,6,5H))*DT )
1266 WRITE(3,I266)I,J,I,J,I,J
      FORMAT(6X,3HXS,2I2,2H=X,I2,2H*X,I2,3H*VD,2I2)
1270 WRITE(3,I270)I,I,J,I,I,J,I,I,J
      FORMAT(6X,4HXS,2I2,3H=DX,2I2,3H=VD,2I2,2H*X,I2,2H*VD,2I2)
      IF (I.EQ.J) GO TO 1300
      A=5.0/(3.0*PI)
      IF (OF(I).EQ.0.0.AND.UF(J).EQ.0.0) WRITE(3,I272)I,J
      IF (OF(I).EQ.0.0.AND.UF(J).EQ.0.0) WRITE(3,I132)I,J
1132 FORMAT(6X,3HDCZ,2I2,4H=0.0)
1272 IF (OF(I).NE.0.0.AND.UF(J).EQ.0.0) WRITE(3,I274)I,J,A,I
      IF (OF(I).NE.0.0.AND.UF(J).EQ.0.0) WRITE(3,I134)I,J,A,I
1134 FORMAT(6X,3HOCZ,2I2,IH=,IPE20,I2,7H*(DCSZR,I2,IH) )
1274 IF (OF(I).EQ.0.0.AND.UF(J).NE.0.0) WRITE(3,I274)I,J,A,J
      FORMAT(6X,2HXCZ,2I2,5H=I.0,IPE20,I2,6H*(CSZR,I2,IH) )
      IF (OF(I).EQ.0.0.AND.UF(J).NE.0.0) WRITE(3,I134)I,J,A,J
      IF (OF(I).EQ.0.0.AND.UF(J).NE.0.0) WRITE(3,I276)I,J,A,I,J
      IF (OF(I).NE.0.0.AND.UF(J).NE.0.0) WRITE(3,I136)I,J,A,I,J
1136 FORMAT(6X,3HOCZ,2I2,IH=,IPE20,I2,7H*(DCSZR,I2,IH) )
1276 FORMAT(6X,2HXCZ,2I2,5H=I.0,IPE20,I2,6H*(CSZR,I2,5H+CSZR,I2,IH) )
1300 CONTINUE
      LHX=IHX
      LHVU=3H*VD
      K=1
1304 WRITE(3,I304)K,((L*PL*LBX,L*LBVU)*K,L),L=2,NSPC)
      FORMAT(6X,4HXS,2I2,IH=5(2A1,I,A3,2I2),A1,3(/5X,IH*,I*,
      * 5(A1,I2,A3,2I2,A1) )
      LHX=2HDX

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345      LBDVD=4H*DVD
      WRITE(3,1308)K,((LBPL,LBDX,L,LBVD,K,L,LBPL,LBX,L,LBDVD,K,L)
      *L=2,NSPC)
1308      * 9/(5X,1H*,1X,2(A2,12,A3,2I2,2A1,12,A4,2I2),A1,
      DO 1310 K=2,NM
      KM=K-1
      KP=K+1
      WRITE(3,1304)K,((LBPL,LBX,L,LBVD,L,K),L=1,KM),
      * ((LBPL,LBX,L,LBVD,K,L),L=KP,NSPC)
      WRITE(3,1308)K,((LBPL,LBDX,L,LBVD,L,K,LBPL,LBX,L,LBDVD,L,K),
      *L=1,KM),((LBPL,LBDX,L,LBVD,K,L,LBPL,LBX,L,LBDVD,K,L),L=KP,NSPC)
1310      CONTINUE
      K=NSPC
      WRITE(3,1304)K,((LBPL,LBX,L,LBVD,L,K),L=1,NM)
      WRITE(3,1308)K,((LBPL,LBDX,L,LBVD,L,K,LBPL,LBX,L,LBDVD,L,K),
      *L=1,NM)
      DO 1325 K=1,NSPC
      A=1.0/AV(K)
      B=-BV(K)-1.0
      C WRITE THE RECIPROCAL OF THE VISCOSITY TIMES THE TEMPERATURE.
      WRITE(3,1312)K,A,B
1312      FORMAT(6X,3HSTV,12,1H=,1PE20.12,6H*(T**,(1PE14.6,2H)) )
      A=A*B
      B=B-1.0
      WRITE(3,1314)K,A,B
1314      FORMAT(6X,4HSTV,12,1H=,1PE20.12,6H*(T**,(1PE14.6,5H))*DT)
      WRITE(3,1316)K,K,K,K
1316      FORMAT(6X,4HSTV,12,2H=X,2I2,4H*STV,12)
      WRITE(3,1320)K,K,K,K,K,K
1320      FORMAT(6X,5HSTV,12,3H=DX,2I2,4H*STV,12,2H=X,2I2,5H*STV,12)
1325      CONTINUE
      C *****
      C SPECIFIC HEAT OF THE MIXTURE.
      C *****
      WRITE(3,124)
124      FORMAT(1HC,2X,44HSPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA. )
      LBC=6HC(1ST+
      LBU=3H)*U
      WRITE(3,132)((LBPL,LBC,K,LBU,K),K=1,NSPC)
132      FORMAT(6X,7HCM(IC)=,4(A1,A6,12,A3,12),A1,
      * 4(/5X,1H*,1X,4(A6,12,A3,12,A1)) )
      C *****
      C THERMAL CONDUCTIVITY AND DIFFUSION.
      C *****
      C HOLTZMAN CONSTANT.
      RK=1.38054E-16
      C GAS CONSTANT.
      RG=1.9872
      WRITE(3,272)
      WRITE(3,274)
272      FORMAT(1HC,2X,24HDIFFUSION AND HEAT FLUX. )
274      FORMAT(1HC,2X,16HSEE DIXON-LEWIS. )
      WRITE(3,276)
276      FORMAT(1HC,2X,60H11. TRANSPORT PHENOMENA IN MULTICOMPONENT SYSTEM
      *S.
      READ(5,279)AAST,HAST,111

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14.17.09

04/15/80

FTN 4.8*498

PROGRAM LOAUF 76/76 OPT=1 MOUND=+*/* TRACE

```

400      279      FORMAT(IP2E14.6,44A1)
        WRITE(6,123)AAS,BAS1,111
123      FORMAT(1/2X,IP2E14.6,44A1)
        READ(5,279)ABST,CBST,111
        WRITE(6,123)ABST,CHST,111
        READ(5,279)ACST,CCST,111
        WRITE(6,123)ACST,CCST,111
C      LM 00.00
        WRITE(3,301)
301      FORMAT(1HC,2X,8HLM 00.00)
        DO 305 K=1,NSPC
        WRITE(3,302)K,K
305      CONTINUE
302      FORMAT(6X,2HZ(,12,1H,12,SH)=0.0 )
        DO 310 I=1,NSPC
        DO 310 J=1,NSPC
        IF(1.EQ.J)GO TO 310
        A =W(J)/W(I)
        IMIN=MIN0(1,J)
        IMAX=MAX0(1,J)
        WRITE(3,308)I,J,IMIN,IMAX,A,J,I
308      * 5H*XSXD*12)
        WRITE(3,312)I,J,IMIN,IMAX,A,J,I,J,I
312      * 5H*XSXD,12,2H*X,12,6H*DSXD,12,1H) )
        FORMAT(6X,2HZ(,12,1H,12,SH)=XSU,212,1H*,1PE20.12,2H*X,12,
        * 5H*XSXD*12)
        WRITE(3,312)I,J,IMIN,IMAX,A,J,I,J,I
310      CONTINUE
C      FIND THE SIGMA FOR EACH PAIR OF SPECIES.
C      ASSUME THAT ONLY ONE SPECIES IS POLAR.
        DO 320 I=1,NSPC
        DO 320 J=1,NSPC
        IF(1.EQ.J)GO TO 320
        E(I,J)=SQRT(ESK(I)*ESK(J))
        IF(UM(I).EQ.0.0.AND.UM(J).EQ.0.0)GO TO 320
C      COMBINING RULE. P. 528, REID AND SHERWOOD.
        IF(UM(I).NE.0.0)LP=1
        IF(UM(J).NE.0.0)LP=J
        IF(LP.EQ.I)LNP=J
        IF(LP.EQ.J)LNP=I
        UMP=UM(LP)*1.0E-1H
        SGC=SGA(LP)*1.0E-8
        TPSTAR=UMP*UMP/(ESK(LP)*RK*SGC*SGC*SQRT(H*0))
        FC=1.0+(1.0/SQRT(2.0))*(ALP(LNP)*TPSTAR/(SGA(LNP)**3))*
        * SQRT(ESK(LP)/ESK(LNP))
        WRITE(6,1234)I,J,LP,LNP,FC
1234      FORMAT(414,1PE12.4)
        E(I,J)=E(I,J)*FC*FC
320      CONTINUE
C      FIND T*, A*, R*, AND C*.
        WRITE(3,1350)
1350      FORMAT(1HC,2X,24HFIND T*, A*, R*, AND C*. )
        DO 1360 I=1,NM
        IP=I+1
        DO 1360 J=IP,NSPC
        WRITE(3,1354)E(I,J)
1354      FORMAT(6X,5HTS=T*,1PE14.6)
        WRITE(3,1364)E(I,J)

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```

1364  FURMAT(6X,7HDTSDT/,IPE14.6)
      WRITE(3,1356)I,J,AAST,ABST
1356  FURMAT(6X,3HAST,2I2,1H=,IPE14.6,7H*(TS**((,IPE14.6,2H)) )
      A=AAST*ABST
      B=ABST*1.0
      WRITE(3,1366)I,J,A,B
1366  FURMAT(6X,4HDAST,2I2,1H=,IPE20.12,11H*DTSDT*(TS**((,IPE14.6,2H)) )
      WRITE(3,1365)CBST
1365  FURMAT(6X,7HEX=EXP(,IPE14.6,4H/TS) )
      LBB=3HBT
      WRITE(3,1358)LBB,I,J,ABST
1358  FURMAT(6X,A3,2I2,1H=,IPE14.6,3H*EX)
      LHUB=4HBT
      A=-ABST*CBST
      WRITE(3,1368)LBUB,I,J,A
1368  FURMAT(6X,A4,2I2,1H=,IPE14.6,15H*DTSDT*EX/(TS*TS) )
      WRITE(3,1365)CCST
      LBC=3HCT
      WRITE(3,1358)LBC,I,J,ACST
      LBUC=4HCT
      A=-ACST*CCST
      WRITE(3,1368)LBDC,I,J,A
1360  CONTINUE
      C LM 00,10 AND LM 10,00
      WRITE(3,321)
321  FURMAT(1HC,2X,21HLM 00,10 AND LM 10,00 )
      DO 330 IS=1,NSPC
      DO 330 JS=1,NSPC
      IF(15.EQ.JS)GO TO 330
      I=IS
      J=JS*NSPC
      A=-2.5*W(1S)/(W(1S)+W(JS))
      IMIN=MIN0(1S,JS)
      IMAX=MAX0(1S,JS)
      WRITE(3,326)A,IMIN,IMAX
326  FURMAT(6X,3HCT=,IPE20.12,9H*(1.2*CT,2I2,5H-1.0) )
      A=A*1.2
      WRITE(3,1140)A,IMIN,IMAX
1140  FURMAT(6X,4HCT=,IPE20.12,5H*UCSI,2I2)
      IMIN=MIN0(1S,JS)
      IMAX=MAX0(1S,JS)
      WRITE(3,328)I,J,IMIN,IMAX
328  FURMAT(6X,2HZ(,12,1H=,12,8H)=CT*XS0,2I2)
      WRITE(3,1144)I,J,IMIN,IMAX,IMIN,IMAX
1144  FURMAT(6X,2HDZ,12,1H=,12,8H=CT*XS0,2I2,8H*DT*XS0,2I2)
330  CONTINUE
      I1=1
      I2=1+NSPC
      LBZ=2HZ(
      LBC=1H,
      LBP=1H,
      LHM=1H-
      WRITE(3,336)I1,I2,((LBM*LBZ,K,LHC,12,LHP),K=2,NSPC)
336  FURMAT(6X,2HZ(,12,1H=,12,2H)=,5(A1,A2,12,A1,12,A1),A1,
      * 3(,5X,1H*,1X,5(A2,12,A1,12,2A1)) )
      LBZ=2HDZ
      LBSP=1HS

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```

515      WRITE(3,338)I,I,I2,((LBM,LBZ,K,LHC,I2,LBP),K=1,IM),
516      FORMAT(6X,2HDZ,I2,IHS,I2,IH=4(A1,A2,I2,AI,I2),A1,
517      * 2(/5X,IH*,IX,7(A2,I2,A1,I2,A1)) )
518      DO 340 I=2,NM
519      IM=I-1
520      IP=I+1
521      I1=I
522      I2=I+NSPC
523      WRITE(3,336)I,I,I2,((LBM,LBZ,K,LHC,I2,LBP),K=1,IM),
524      * ((LBM,LBZ,K,LBP),K=IP,NSPC)
525      WRITE(3,338)I,I,I2,((LBM,LBZ,K,LHC,I2,LBP),K=1,IM),
526      * ((LBM,LBZ,K,LHC,I2,LBP),K=IP,NSPC)
527      CONTINUE
528      I1=NSPC
529      I2=NSPC+NSPC
530      WRITE(3,336)I,I,I2,((LBM,LBZ,K,LHC,I2,LBP),K=1,NM),
531      WRITE(3,338)I,I,I2,((LBM,LBZ,K,LBP),K=1,NM)
532      DO 350 IS=1,NSPC
533      DO 350 JS=1,NSPC
534      IN=IS+NSPC
535      JN=JS
536      WRITE(3,342)IN,JN,JN,IN
537      WRITE(3,346)IN,JN,JN,IN
538      FORMAT(6X,2HZ(I2,IH,I2,4H)=Z(I2,IH,I2,IH) )
539      FORMAT(6X,2HDZ,I2,IHS,I2,3H=OZ,I2,IHS,I2)
540      CONTINUE
541      C LM 01.00 AND LM 00.01
542      C ROWS OF LM 01.00 AND COLUMNS OF LM 00.01 CORRESPONDING TO
543      C MONATOMICS ARE DELETED.
544      WRITE(3,351)
545      FORMAT(1HC,2X,2IHLM 01.00 AND LM 00.01 )
546      DO 360 IS=1,NSPC
547      DO 360 JS=1,NSPC
548      IF (OF(IS).EQ.0.0)GO TO 360
549      I=LD(IS)+2*NSPC
550      J=JS
551      WRITE(3,362)I,J
552      FORMAT(6X,2HZ(I2,IH,I2,5H)=0.0)
553      CONTINUE
554      DO 363 IS=1,NSPC
555      DO 363 JS=1,NSPC
556      IF (OF(JS).EQ.0.0)GO TO 363
557      I=IS
558      J=LD(JS)+2*NSPC
559      WRITE(3,362)I,J
560      CONTINUE
561      C LM 10.10 SYMMETRIC.
562      WRITE(3,361)
563      FORMAT(1HC,2X,8HLM 10.10 )
564      DO 370 IS=1,NM
565      IP=IS+1
566      DO 370 JS=IP,NSPC
567      I=IS+NSPC
568      J=JS+NSPC
569      A=W(IS)*W(JS)/(W(IS)+W(JS))*2)
570      WRITE(3,372)A,IS,JS,IS,JS
571      FORMAT(6X,3HCT=,1PE20.12,15H*(13.75-3.0*AS I,212,

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575      * 8H-4.0*AST,2I2,3H*CZ,2I2,1H) )
      WRITE(3,1146)A,IS,JS,IS,JS,IS,JS,IS,JS,IS,JS,IS,JS,IS,JS
1146      FORMAT(6X,5HDCT=-,IPE20,12,10H*(3.0*DBST,2I2,9H*4.0*(AST,
      * 2I2,4H*DCZ,2I2,5X,1H*,1X,5H*DBST,2I2,3H*CZ,2I2,2H) ) )
      WRITE(3,376)I,J,IS,JS
376      FORMAT(6X,2HZ(,I2,1H,,I2,8H)=CT*XSD,2I2)
      WRITE(3,377)J,I,I,J
377      FORMAT(6X,2HZ(,I2,1H,,I2,4H)=Z(,I2,1H,,I2,1H) )
      WRITE(3,380)I,J,IS,JS,IS,JS
380      FORMAT(6X,2HDZ,I2,1HS,I2,8H=CT*UXSD,2I2,8H*DCI*XSD,2I2)
      WRITE(3,379)J,I,I,J
379      FORMAT(6X,2HDZ,I2,1HS,I2,3H=DZ,I2,1HS,I2)
370      CONTINUE
      DO 400 IS=1,NSPC
585      I=IS*NSPC
      RGA=82.05
      C USE THE GAS CONSTANT IN UNITS OF CM**3-ATM/MOLE-K SO ALL THE
      C ELEMENTS OF Z ARE IN THE SAME UNITS.
      A=-5.0*PRESS*W(IS)/(3.0*RGA)
      WRITE(3,382)A,IS,IS
590      FORMAT(6X,3HCT=,IPE20,12,3H*CZ,2I2)
      WRITE(3,383)A,IS,IS
383      FORMAT(6X,4HDCI=,IPE20,12,4H*DCZ,2I2)
      DO 390 KS=1,NSPC
595      IF (KS.EQ.15) GO TO 390
      IMIN=MIN0(15,KS)
      IMAX=MAX0(15,KS)
      A=7.5*W(IS)*W(IS)+6.25*W(KS)*W(KS)
      B=3.0*W(KS)*W(KS)
      C=4.0*W(IS)*W(KS)
      RMT=1.0/((W(IS)+W(KS))*2)
      A=A*RMT
      B=B*RMT
      C=C*RMT
      WRITE(3,386)KS,C,IMIN,IMAX,IMIN,IMAX
386      FORMAT(6X,2HCT,I2,1H=,IPE20,12,4H*AST,2I2,3H*CZ,2I2)
      WRITE(3,1150)KS,C,((IMIN,IMAX),L=1,4)
1150      FORMAT(6X,3HDCI,I2,1H=,IPE20,12,6H*(DAST,2I2,3H*CZ,2I2,
      * 4H*AST,2I2,4H*DCZ,2I2,1H) )
      WRITE(3,388)KS,A,B,IMIN,IMAX,KS
388      FORMAT(6X,2HCT,I2,1H=,IPE20,12,1H=,IPE20,12,4H*BST,2I2,3H*CT,I2)
      WRITE(3,1154)KS,B,IMIN,IMAX,KS
1154      FORMAT(6X,3HDCI,I2,2H=-,IPE20,12,5H*DBST,2I2,4H*DCI,I2)
390      CONTINUE
      LHXSD=3H*XS0
      LHDXS0=4H*XS0
      LBCT=3H*CT
      LHDCI=4H*DCI
      IF (IS.GT.1) GO TO 393
      WRITE(3,392)I,I,IS,((LBM,LBXSD,IS,KS,LHCT,KS),KS=2,NSPC)
392      FORMAT(6X,2HZ(,I2,1H,,I2,9H)=CT*XSTV,I2,
      * 2(AI,A3,2I2,A3,I2),AI,5(/5X,1H*,IX,4(A3,2I2,A3,I2,AI)) )
      WRITE(3,394)I,I,IS,IS,((LBM,LBXSD,IS,KS,LHCT,KS,LBM,LHXSD,IS,
      * KS,LHDCI,KS),KS=2,NSPC)
394      FORMAT(6X,2HDZ,I2,1HS,I2,9H=CT*UXSTV,I2,9H*DCI*XSTV,I2,AI,A4,
      * 2I2,A3,I2,AI,A3,2I2,A4,I2,AI,1(/5X,1H*,IX,2(A4,2I2,A3,I2,AI,A3,
      * 2I2,A4,I2,AI)) )

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620 GO TO 400
621 IF (IS.LT.NSPC) GO TO 396
622 WRITE(3,392) I, I, IS, ((LBM,LBXSD,KS,IS,LBCT,KS),KS=I,NM)
623 WRITE(3,394) I, I, IS, IS, ((LBM,LBUXSD,KS,IS,LBCT,KS,LBM,LBXSD,
624 * KS,IS,LBDCI,KS),KS=I,NM)
625 GO TO 400
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685 430 CONTINUE
      LHCT=2HCT
      LBUCT=3HUCT
      LBXSD=4H*XSD
      LBUXSD=5H*DXSD
      IF (IS.GT.1) GO TO 433
      WRITE(3,432)I,J,IS,((LBPL,LBCT,KS,LBXSD,IS,KS),KS=2,NSPC)
      FORMAT(6X,2H2I,12,1H,12,9H)=CT*XSTV,I2,3(A1,A2,I2,A4,2I2),A1,
      * 5(/5X,1H*,1X,4(A2,I2,A4,2I2,A1))
      WRITE(3,434)I,J,IS,IS,((LBPL,LBCT,KS,LBXSD,IS,KS,LBPL,LBUCT,
      * KS,LBXSD,IS,KS),KS=2,NSPC)
      FORMAT(6X,2H2I,12,1H,12,9H)=CT*UXSTV,I2,9H*UCT*XSTV,I2,
      * A1,A2,I2,A5,2I2,A1,A3,I2,A4,2I2,A1,10(/5X,1H*,1X,
      * 2(A2,I2,A5,2I2,A1,A3,I2,A4,2I2,A1))
      GO TO 440
700 433 IF (IS.LT.NSPC) GO TO 436
      WRITE(3,432)I,J,IS,((LBPL,LBCT,KS,LBXSD,KS,IS),KS=I,NM)
      WRITE(3,434)I,J,IS,IS,((LBPL,LBCT,KS,LBXSD,KS,IS,LBPL,LBUCT,
      * KS,LBXSD,KS,IS),KS=I,NM)
      GO TO 440
705 436 CONTINUE
      IM=IS-I
      IP=IS+I
      WRITE(3,432)I,J,IS,((LBPL,LBCT,KS,LBXSD,KS,IS),KS=I,IM),
      * ((LBPL,LBCT,KS,LBXSD,IS,KS),KS=IP,NSPC)
      WRITE(3,434)I,J,IS,IS,((LBPL,LBCT,KS,LBXSD,KS,IS,LBPL,LBUCT,
      * KS,LBXSD,KS,IS),KS=I,IM),((LBPL,LBCT,KS,LBXSD,IS,KS,LBPL,LBUCT,
      * KS,LBXSD,IS,KS),KS=IP,NSPC)
      CONTINUE
440 CONTINUE
450 DO 418 IS=I,NSPC
      DO 418 JS=I,NSPC
      IF (DF(IS).EQ.0.0) GO TO 418
      I=LD(IS)+2*NSPC
      J=JS+NSPC
      WRITE(3,412)I,J,J,I
      FORMAT(6X,2H2I,12,1H,12,4H)=Z(I,I2,1H,12,1H)
      WRITE(3,416)I,J,J,I
      FORMAT(6X,2H2I,12,1H,12,3H=DZ,I2,1H,12)
412 416 CONTINUE
      C LM 01,01
      C ROWS AND COLUMNS OF LM 01,01 CORRESPONDING TO MONATOMICS ARE DELETED.
451 WRITE(3,451)
      FORMAT(1HC,2X,BHLM 01,01)
      DO 460 IS=I,NSPC
      DO 460 JS=I,NSPC
      IF (IS.EQ.JS) GO TO 460
      IF (DF(IS).EQ.0.0) OR (J5).EQ.0.0) GO TO 460
      I=LD(IS)+2*NSPC
      J=LD(JS)+2*NSPC
      WRITE(3,362)I,J
      CONTINUE
      LHL=IH
      LHP=IH)
      DO 490 IS=I,NSPC
      DO 490 JS=I,NSPC
      IF (DF(IS).EQ.0.0) GO TO 490
      I=LD(IS)+2*NSPC

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462 WRITE(3,462) IS
    FORMAT(6X,I4HCTM=-6.25/CINT,I2)
    WRITE(3,1166) IS,IS
745
1166 FORMAT(6X,I5HCTM=6.25*DCINT,I2,6H/(CINT,I2,5H*CINT,I2,IH) )
    A=2.0*PRESS*W(1S)/(PI*GA)
    WRITE(3,466) A,IS
748
466 FORMAT(6X,3HCT=,IPE20,I2,4H*CSC,I2)
    WRITE(3,1170) A,IS
749
1170 FORMAT(6X,4HCT=,IPE20,I2,5H*DCSC,I2)
    DO 470 KS=1,NSPC
    IF (IS.EQ.KS) GO TO 470
    A=I2.0*W(1S)/(5.0*PI*W(KS))
    IMIN=MIN0(1S,KS)
    IMAX=MAX0(1S,KS)
755
    WRITE(3,472) KS,A,IMIN,IMAX,IS
    FORMAT(6X,2HCT,I2,5H=1.0,*,IPE20,I2,4H*AST,I2,4H*CSC,I2)
757
472 WRITE(3,1172) KS,A,IMIN,IMAX,IS,IMIN,IMAX,IS
    FORMAT(6X,3HCT,I2,IH=,IPE20,I2,6H*(DAST,I2,4H*CSC,I2,
759
1172 * 4H*AST,I2,5H*DCSC,I2,IH) )
760
470 CONTINUE
    IF (IS.GT.1) GO TO 475
    WRITE(3,1176) IS,IS,IS,((LBPL,LBCT,KS,LBXSD,IS,KS),KS=2,NSPC)
    FORMAT(6X,4HSUM=,7HCT*XSTV,I2,4H*XSD,I2,2(AI,A2,I2,A4,2I2),AI,
763
1176 * 5(/5X,IH*,IX,4(A2,I2,A4,2I2,AI)) )
    WRITE(3,1180) IS,IS,IS,((LBPL,LBCT,KS,LBXSD,IS,KS,LBPL,LBCT,
765
1180 * KS,LBXSD,IS,KS),KS=2,NSPC)
    FORMAT(6X,5HOSUM=,8HCT*XSTV,I2,9H*CT*DXSTV,I2,5H*DXSD,I2,
767
1180 * AI,A2,I2,A5,2I2,AI,A3,I2,A4,2I2,AI,I0(/5X,IH*,IX,
770
1180 * 2(A2,I2,A5,2I2,AI,A3,I2,A4,2I2,AI)) )
    WRITE(3,476) I,I
    FORMAT(6X,2HZ(I2,IH,*,I2,9H)=CTM*SUM)
773
476 WRITE(3,478) I,I
    FORMAT(6X,2HDZ,I2,IHS,I2,I8H=DCTM*SUM*CTM*DSUM )
775
478 GO TO 490
    IF (IS.LT.NSPC) GO TO 480
    WRITE(3,1176) IS,IS,IS,((LBPL,LBCT,KS,LBXSD,KS,IS),KS=1,NM)
777
475 WRITE(3,1180) IS,IS,IS,((LBPL,LBCT,KS,LBXSD,KS,IS,LBPL,LBCT,
779
1180 * KS,LBXSD,KS,IS),KS=1,NM)
    WRITE(3,476) I,I
780
1180 WRITE(3,478) I,I
    GO TO 490
    IM=IS-I
    IP=IS+I
783
480
    WRITE(3,1176) IS,IS,IS,((LBPL,LBCT,KS,LBXSD,KS,IS),KS=1,IM),
785
1176 * ((LBPL,LBCT,KS,LBXSD,IS,KS),KS=IP,NSPC)
    WRITE(3,1180) IS,IS,IS,((LBPL,LBCT,KS,LBXSD,KS,IS,LBPL,LBCT,
787
1180 * KS,LBXSD,KS,IS),KS=1,IM),((LBPL,LBCT,KS,LBXSD,KS,IS,LBPL,LBCT,
789
1180 * KS,LBXSD,IS,KS),KS=IP,NSPC)
    WRITE(3,476) I,I
790
1180 WRITE(3,478) I,I
    CONTINUE
    C SOLVE FOR DIFF VELOCITIES AND ENERGY FLUX.
793
490
    WRITE(3,498)
    FORMAT(1HC,2X,47HSOLVE FOR DIFFUSION VELOCITIES AND ENERGY FLUX. )
795
    NMT=L0(NSPC)+2*NSPC
    NDI=30
    WRITE(3,500) NMT,NDI

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800      500      FORMAT(6X,9HCALL DEC(,I2,1H,,I2,11H,Z,1PS,IER) )
      DO 495 K=1,NSPC
      WRITE(3,492)K,K,PHN
      492      FORMAT(6X,2HV(,I2,7H)=RH*DX,I2,1H/,IPEI4.6)
      WRITE(3,702)K,K,K,PHN
      702      FORMAT(6X,2HDV,I2,8H=(URH*DX,I2,7H+RH*DDX,I2,2H)/,IPEI4.6)
      805      CONTINUE
      DO 515 I=1,NSPC
      IP=I*NSPC
      512      WRITE(3,512)IP
      FORMAT(6X,2HV(,I2,5H)=0.0)
      810      WRITE(3,712)IP
      712      FDRMAT(6X,2HDV,I2,4H=0.0)
      515      CONTINUE
      DO 517 I=1,NSPC
      IF (DF(I).EQ.0.0)GO TO 517
      IP=LD(I)+2*NSPC
      815      WRITE(3,512)IP
      WRITE(3,712)IP
      CONTINUE
      517      WRITE(3,520)NMT,NDIM
      820      FORMAT(6X,9HCALL SOL(,I2,1H,,I2,14H,Z,V,IPS) )
      CALL UR(NSPC,NMT,NDIM)
      DO 525 I=1,NSPC
      WRITE(3,522)I,I
      522      FORMAT(6X,2HVX,I2,3H=V(,I2,1H) )
      825      WRITE(3,722)I,I
      722      FORMAT(6X,3HDVX,I2,4H=DV(,I2,1H) )
      525      CONTINUE
      DO 528 I=1,NSPC
      WRITE(3,512)I
      830      WRITE(3,712)I
      CONTINUE
      DO 530 I=1,NSPC
      IP=I*NSPC
      835      WRITE(3,532)IP,I
      WRITE(3,714)IP,I
      714      FORMAT(6X,2HDV,I2,3H=DX,I2)
      530      CONTINUE
      532      FORMAT(6X,2HV(,I2,3H)=X,I2)
      840      IF (DF(I).EQ.0.0)GO TO 535
      IP=LD(I)+2*NSPC
      WRITE(3,532)IP,I
      WRITE(3,714)IP,I
      535      CONTINUE
      845      WRITE(3,520)NMT,NDIM
      CALL DR(NSPC,NMT,NDIM)
      LHV=2HV(
      LHP=1H)
      DO 540 I=1,NSPC
      WRITE(3,538)I,I,PHN
      850      FORMAT(6X,2HVT,I2,14H=-2.5*RH*DT*V(,I2,5H)/(T*,IPEI4.6,1H) )
      540      CONTINUE
      726      WRITE(3,726)IPN
      855      FORMAT(6X,1SHDT=UPH2(NPUE)*,1P,14.6)
      DO 730 K=1,NSPC
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04/15/80 14.17.09

FTN 4.8+498

PROGRAM LOADF 76/76 OPT=I ROUND=***/ TRACE

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860      WRITE(3,728)K,K,K,K,K,PHN
861      FORMAT(6X,3HDVT,I2,I6H=-2.5*(URH*DT*V(,I2,
862      * IH)+RH*DDT*V(,I2,I6H)+RH*DT*UV(,I2,I6H)-RH*DT*V(,I2,2H)*,
863      * /5X,IH*,IX,9HD1/T)/(T*,IPEI4.6,IH) )
864      CONTINUE
865      DO 545 I=1,NSPC
866      WRITE(3,542)I,I,I,I
867      FORMAT(6X,2HUV,I2,2H=U,I2,4H*(VX,I2,3H+VT,I2,IH) )
868      CONTINUE
869      DO 745 I=1,NSPC
870      WRITE(3,742)I,I,I,I,I,I,I
871      FORMAT(6X,3HDUV,I2,3H=DU,I2,4H*(VX,I2,3H+VT,I2,IH) ,
872      * 2H+U,I2,5H*(DVX,I2,4H+DVT,I2,IH) )
873      CONTINUE
874      DO 550 I=1,NSPC
875      WRITE(3,548)I,I,I
876      FORMAT(6X,9HRHUV(I1T+,I2,7H)=RH*UV,I2)
877      CONTINUE
878      DO 750 I=1,NSPC
879      WRITE(3,748)I,I,I,I
880      FORMAT(6X,I0HRHUV(I1T+,I2,8H)=URH*UV,I2,7H+RH*DUV,I2)
881      CONTINUE
882      C CONVERT FROM CM**3-ATM/SEC-CM-K TO CAL/SEC-CM-K.
883      A=-25.0*PRESS*I.9872/(4.0*82.05)
884      LBX=IHX
885      LBV=3H*V(
886      LBTRS=5HRLTRS
887      WRITE(3,556)((LBPL*LBX,K,LBV,K*NSPC*LBP),K=I,NSPC)
888      FORMAT(6X,4HSUM=,5(2AI,I2,A3,I2,A1),AI,3(/5X,IH*,IX,
889      * 5(AI,I2,A3,I2,2AI)) )
890      LBDX=2HDX
891      LBDV=4H*DV(
892      WRITE(3,756)((LBPL*LBDX,K,LBV,K*NSPC*LBP,LBPL*LBX,K,LBDV,
893      * K*NSPC*LBP),K=1,NSPC)
894      FORMAT(6X,5HDSUM=,2(AI,A2,I2,A3,I2,A3,I2,3AI,I2,A4,I2,A1),AI,
895      * 6(/5X,IH*,3(A2,I2,A3,I2,3AI,I2,A4,I2,2AI)) )
896      WRITE(3,557)LBTRS,A
897      FORMAT(6X,A5,IH=,IPEI4.6,6H*SUM/T)
898      LBDRTRS=6HDLRLTRS
899      WRITE(3,757)LBDRTRS,A
900      FORMAT(6X,A6,IH=,IPEI4.6,I8H*(DSUM-SUM*DT/T)/T )
901      LBINT=5HPLINT
902      DO 553 I=1,NSPC
903      IF (DF(I).EQ.0.0)GO TO 553
904      J=LD(I)
905      LOV(J)=I
906      CONTINUE
907      NT=LD(NSPC)
908      IF (NT.EQ.0)GO TO 554
909      WRITE(3,556)((LBPL*LBX,LDV(K),LHV,K*2*NSPC*LBP),K=1,NT)
910      WRITE(3,756)((LBPL*LBDX,LDV(K),LHV,K*2*NSPC*LBP,LBPL*LBX,LDV(K) ,
911      * LBDV,K*2*NSPC*LBP),K=1,NT)
912      WRITE(3,557)LBINT,A
913      LBDRINT=6HDLRLINT
914      WRITE(3,757)LBDRINT,A
915      CONTINUE
916      WRITE(3,562)

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562  FORMAT(6X,15HRLM=RLTKS+RLINT )
      WRITE(3,762)
915  FORMAT(6X,18HDLRLM=DRLTRS+DRLINT)
      WRITE(3,766)
566  FORMAT(6X,15HRLM(IC)=RH*RLM)
      WRITE(3,766)
920  FORMAT(6X,25HDLRLM(IC)=DRH*RLM+RH*DLRLM )
      LBDX=2HDX
      WRITE(3,570)((LHPL,LBDX,L,LBV,L,LBP),L=1,NSPC)
570  FORMAT(6X,4HSUM=,5(A1,A2,I2,A3,I2,A1),A1,3(/5X,IH*,IX,
      * 5(A2,I2,A3,I2,2A1)) )
      LBDX=3HDX
      WRITE(3,770)((LHPL,LBDX,L,LBV,L,LBP,LHPL,LBDX,L,LBP),
      * L=1,NSPC)
925  FORMAT(6X,5HDSUM=,2(A1,A3,I2,A3,I2,2A1,A2,I2,A4,I2,A1),A1,
      * 9(/5X,IH*,IX,2(A3,I2,A3,I2,2A1,A2,I2,A4,I2,2A1)) )
930  A=-2.5*I.9872*PRESS/(82.05*PHN)
      WRITE(3,572)A
572  FORMAT(6X,3HDX=,IPE20,I2,7H*RH*SUM)
      WRITE(3,772)A
935  C *****
772  FDRMAT(6X,RHDX(IC)=,IPE20,I2,IH*(DRH*SUM+RH*DSUM))
      C *****
      C FIND THE TIME DERIVATIVES.
      C *****
      WRITE(3,612)
612  FORMAT(1HC,2X,26HFIND THE TIME DERIVATIVES.)
      WRITE(3,622)
622  FORMAT(6X,15HSP=ASP+BSPTIME)
      TMSPH2=TMN/(PHN*PHN)
      WRITE(3,628)
628  FORMAT(1X,3HI00,2X,8HCONTINUE)
      WRITE(3,632)
632  FDRMAT(6X,25HIF(KPDE.EQ.NPDE)GO TO I50)
      WRITE(3,636)TMN
636  FORMAT(6X,3HRY=,IPE20,I0,8H*(KPDE) )
      TMSPH=TMN/PHN
      WRITE(3,638)TMSPH
638  FORMAT(6X,4HXY=,IPE20,I0,I6H*DRHUV(IST+KPDE) )
      WRITE(3,642)
642  FDRMAT(6X,23HFVAL=SP*UPH(KPDE)*(IY+RY)
      WRITE(3,646)
646  FORMAT(6X,6HRETURN)
      WRITE(3,648)
648  FORMAT(1X,3HI50,2X,8HCONTINUE)
      WRITE(3,662)TMSPH2
662  FORMAT(6X,3HTL=,IPE20,I0,IH*)
      WRITE(3,664)
664  FORMAT(5X,IH*,IX,4IH(DRHLM(IC)*UPH(NPDE)+RHLM(IC)*UPH2(NPDE)) )
      LBL=IH
      LHC=6HC(IST+
      LHRHUV=10H)*RHUV(IST
      WRITE(3,668)TMSPH,((LHBL,LHPL,LHLC,K,LHRRHUV,LHPL,K,LRP),K=1,NSPC)
      * ,LRP
945  FDRMAT(6X,4HTI=,IPE20,I0,I2H*UPH(NPDE)*(I2A1,A6,I2,A10,A1,I2,3A1,
      * 10(/5X,IH*,IX,2(A6,I2,A10,A1,I2,3A1)) )
      TMSPT=TMN/TPN
      LHR=2HR(

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04/15/80 14.17.09

FTN 4.8+498

PROGRAM LOADF 76/76 OPT=1 ROUND=-**/ IHACE

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970      LBH=8H)*H(IST+
        WRITE(3,672)TMSTP,((LB8L,LBPL,LHM,K,LBH,K,LBP),K=1,NSPC),LBP
672      * 9(/5X,IH*,IX,2(A2,I2,A8,I2,3A1))
        A=-TMN/(TPN*PHN)
        WRITE(3,674)A
975      * 674      FORMAT(6X,3HTX=,IPE20,I2,8H*DUX(IC) )
        * 676      WRITE(3,676)
        * 676      FORMAT(6X,38HF VAL=SP*UPH(NPOE)+ (IL+TR+TD+TX)/CM(IC) )
        STOP
        END
980
971      MAIN
972      MAIN
973      MAIN
974      MAIN
975      MAIN
976      MAIN
977      MAIN
978      MAIN
979      MAIN
980      MAIN
981      MAIN

```

```

1      SUBROUTINE DR(NSPC,NMT,NDIM)
C      FIND THE DERIVATIVES OF THE SOLUTIONS V.
      LHDZ=2HDZ
      LKSP=IHS
      LHM=IH-
      LHV=3H*V(
      LBP=IH)
      I=1
      NTOP=2*NSPC
      WRITE(3,10)1,1,((LHM,LBDZ,1,LBSP,J,LBV,J,LBP),J=2,NTOP)
10      FORMAT(6X,3HDV(,12,4H)=DV,12,3(A1,A2,12,A1,12,A3,12,A1),A1,
      * 7(/5X,1H*,1X,4(A2,12,A1,12,A3,12,2A1)) )
      NM=NSPC-1
      DO 15 I=2,NM
15      IM=I-1
      IP=I+1
      NST=NSPC+1
      WRITE(3,10)1,1,((LBM,LBDZ,1,LBSP,J,LBV,J,LBP),J=1,IM),
      * ((LBM,LBDZ,1,LBSP,J,LBV,J,LBP),J=IP,NSPC),
      * ((LBM,LBDZ,1,LBSP,J,LBV,J,LBP),J=NST,NTOP)
20      CONTINUE
15      I=NSPC
      WRITE(3,10)1,1,((LHM,LBDZ,1,LBSP,J,LBV,J,LBP),J=1,NM),
      * ((LBM,LBDZ,1,LBSP,J,LBV,J,LBP),J=NST,NTOP)
      DO 25 I=1,NSPC
      IP=I+NSPC
      WRITE(3,10)IP,IP,((LBM,LBDZ,IP,LBSP,J,LBV,J,LBP),J=1,NMT)
25      CONTINUE
      ITOP=NMT-2.0*NSPC
      DO 30 I=1,ITOP
      IP=1.2*NSPC
      WRITE(3,10)IP,IP,((LHM,LBDZ,IP,LBSP,J,LBV,J,LBP),J=NST,NTOP),
      * LHM,LBDZ,IP,LBSP,IP,LBV,IP,LBP
30      CONTINUE
      WRITE(3,32)NMT,NDIM
32      FORMAT(6X,9HCALL SOL(,12,1H,,12,10H,Z,DV,1PS) )
      RETURN
      END

```

PROGRAM WILL BE ENTERED AT LOADF (241)

BLOCK	ADDRESS	LENGTH	FILE
LOADF	110	17367	LGO
DR	17477	401	LGO
/STP.END/	20100	1	SL-FTNL18
/FCL.C./	20101	30	SL-FTNL18
/QB.10./	20131	144	SL-FTNL18
Q2NTRY=	20275	4	SL-FTNL18
COMIO=	20301	10	SL-FTNL18
FECMSK=	20311	41	SL-FTNL18
FEIFST=	20352	3	SL-FTNL18
FLTN=	20355	156	SL-FTNL18
FLTOUT=	20533	315	SL-FTNL18
FMTP=	21050	377	SL-FTNL18
FORSYS=	21447	300	SL-FTNL18
FORUTL=	21747	45	SL-FTNL18
GETFIT=	22014	54	SL-FTNL18
INCOM=	22070	144	SL-FTNL18
INPC=	22234	173	SL-FTNL18
KODER=	22427	476	SL-FTNL18
KRAKER=	23125	454	SL-FTNL18
OUTC=	23601	155	SL-FTNL18
OUTCOM=	23756	204	SL-FTNL18
SPA=	24162	11	SL-FTNL18
ERRCAP=	24173	317	SL-FTNL18
FERCAP=	24512	171	SL-FTNL18
ACUS	24703	6	SL-FTNL18
ACOSIN.	24711	63	SL-FTNL18
EXP.MSG	24774	16	SL-FTNL18
SQRT	25012	6	SL-FTNL18
SQRT.	25020	32	SL-FTNL18
SYSRID=	25052	1	SL-FTNL18
SYS=1ST	25053	65	SL-FTNL18

1	H2	2.00	2.00	2.92	38.00	0.00	.79	280.00	CNST
.31001901E+01	.51119464E-03	.52644210E-07	-.34909973E-10	.36945345E-14	H2				
-.87738042E+03	-.19629421E+01	.30574451E+01	.26765200E-02	-.58099162E-05	H2				
.55210391E-08	-.18122739E-11	-.98890474E+03	-.22997056E+01		H2				
2	N2	28.00	2.00	3.62	97.50	0.00	0.00	15.70	VAR
.28963194E+01	.15154866E-02	-.57235277E-06	.99807393E-10	-.65223555E-14	N2				
-.90586184E+03	.61615148E+01	.36748261E+01	-.12081500E-02	.23240102E-05	N2				
-.63217559E-09	-.22577253E-12	-.10611588E+04	.23580424E+01		N2				

1 H2 2.188700E-06 6.502900E-01 H2 VISCOSITY.

1 H2 6.357900E-06 7.383300E-01 H2 THERMAL CONDUCTIVITY.

2 N2 4.266700E-06 6.613600E-01 N2 VISCOSITY.

2 N2 6.407700E-07 7.999600E-01 N2 THERMAL CONDUCTIVITY.

1	1	H2	H2	1.119300E-04	1.661400E+00	H2	H2	BINARY DIFFUSION.
1	2	H2	N2	5.951700E-05	1.663800E+00	H2	N2	BINARY DIFFUSION.
2	2	N2	N2	1.537400E-05	1.672900E+00	N2	N2	BINARY DIFFUSION.

PRESS = 1.00

TPN = 1.0000E+03

PHN = 5.0000E-05 TMN = 1.0000E-03

1.088500E+00 9.055700E-03 A* HCB FIT A*TS**8

1.078600E+00 8.500100E-02 B* HCB FIT A*EXP(C/T)

9.542600E-01 -1.435700E-01 C* HCB FIT A*EXP(C/T)

```

1  SUBROUTINE F(TIME,PH,U,UPH,UPH2,FVAL,NPDE,KPDE,IC,KSKT,KSKR)
   DIMENSION Z(30,30),IPS(30)
   DIMENSION V(30),DV(30)
   DIMENSION U(NPDE),UPH(NPDE),UPH2(NPDE)
   COMMON/TABAB/ASP,ASP,TPN,PHN,TM,SPH,TMSPH2,TMSTP,TPENT
   COMMON/TABP/PRESS,PSK,NPOEM
   COMMON/TABSM/SMALL
   COMMON/TABAM/YAB,WAB
10  DIMENSION R(20)
   DIMENSION C(1000),H(1000),RHL M(100),ORHLM(100),CM(100)
   DIMENSION OC(1000)
   DIMENSION DQX(100)
   COMMON/TABCT/RL,CPMX,H0(20),R2D(20),R2DM(20)
   COMMON/TABMF/RHUV(IU00),ORHUV(IU00)
15  COMMON/TABRY/T,RH,Y1,Y2,Y3,Y4,Y5,Y6,Y7,Y8,Y9,Y10
   C AT EACH CALL THE TIME RATE OF CHANGE FOR ONE PDE IS RETURNED IN FVAL.
   C WE WANT TO AVOID DIVISION BY ZERO.
   DO 5 K=1,NPDEM
     IF(ABS(U(K)).LT.SMALL)U(K)=SMALL
20   IF(ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL
   C TEST CASE. BINARY MIX OF H2 AND N2. TRANSPORT WARNATZ PAR.
   C U = MASS FRACTIONS. Y = MASS FRACTIONS / MOLECULAR WEIGHTS.
     YN=1.0-U( 1)
     CALL RT(U,YN,R,NPDE,KPDE,IC,KSKR)
     IST= 2*(IC-1)
     OT=UPH(NPDE)* 1.000000E+03
     IF(KSKT.GT.1)GO TO 100
     IF(KSKR.GT.1)GO TO 125
   C NTIS ENTHALPIES AND HEAT CAPACITIES.
     IF(T.GT.1000.)GO TO 2000
30     C 1=1.9872*( 3.05744S10E+00+I*( 2.67652000E-03
       *+I*( -S.80991620E-06+I*( S.52103910E-09+I*( -1.81227390E-12))))))
       OC 1=1.9872*( 2.67652000E-03+I*( -1.16198324E-05
       *+I*( 1.65631173E-08+I*( -7.24909560E-12)))))*OT
       H 1=1.9872*( -9.88904740E+02+I*( 3.05744S10E+00
       *+I*( 2.67652000E-03/2.0+I*( -5.80991620E-06/3.0
       *+I*( S.52103910E-09/4.0+I*( -1.81227390E-12/5.0))))))
       C 2=1.9872*( 3.67482610E+00+I*( -1.20815000E-03
       *+I*( 2.32401020E-06+I*( -6.32175590E-10+I*( -2.25772530E-13))))))
       UC 2=1.9872*( -1.20815000E-03+I*( 4.64802040E-06
       *+I*( -1.89652677E-09+I*( -9.03090120E-13)))))*OT
       H 2=1.9872*( -1.06115880E+03+I*( 3.67482610E+00
       *+I*( -1.20815000E-03/2.0+I*( 2.32401020E-06/3.0
       *+I*( -6.32175590E-10/4.0+I*( -2.25772530E-13/5.0))))))
       GO TO 3000
40     CONTINUE
       C 1=1.9872*( 3.10019010E+00+I*( S.11194640E-04
       *+I*( S.26442100E-08+I*( -3.4909730E-11+I*( 3.694534S0E-15))))))
       OC 1=1.9872*( 5.11194640E-04+I*( 1.05288420E-07
       *+I*( -1.04729919E-10+I*( 1.4771380E-14)))))*OT
       H 1=1.9872*( -8.77380420E+02+I*( 3.10019010E+00
       *+I*( S.11194640E-04/2.0+I*( 5.26442100E-08/3.0
       *+I*( -3.4909730E-11/4.0+I*( 3.694534S0E-15/5.0))))))
       C 2=1.9872*( 2.89631940E+00+I*( 1.51548660E-03
       *+I*( -S.72352770E-07+I*( 9.98113930E-11+I*( -6.52233550E-15))))))
       OC 2=1.9872*( 1.51548660E-03+I*( -1.14470554E-06
       *+I*( 2.99422179E-10+I*( -2.50444220E-14)))))*OT

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      H 2=1.9872*(-9.05861840E+02+T*( 2.89631940E+00
      * +T*( 1.51548660E-03/2.0+T*( -5.72352770E-07/3.0
      * +T*( 9.98073930E-11/4.0+T*( -6.52235550E-15/5.0))))))
      3000 CONTINUE
      C SPECIFIC HEATS AND SPECIFIC ENTHALPIES.
      C(1ST+1)=C 1/ 2.00
      DC(1ST+1)=DC 1/ 2.00
      H(1ST+1)=H 1/ 2.00
      C(1ST+2)=C 2/ 28.00
      DC(1ST+2)=DC 2/ 28.00
      H(1ST+2)=H 2/ 28.00
      125 CONTINUE
      C VISCOSITY FROM WARNATZ ST PAR.
      C LEAST SQUARES FIT, T=300,2000.
      C THERMAL CONDUCTIVITIES FROM WARNATZ ST PAR.
      C LEAST SQUARES FIT, T=300,2000.
      C V 1= 2.188700E-06*(T** 6.502900E-01)
      C V 2= 4.266700E-06*(T** 6.613600E-01)
      C RL 1= 6.357900E-06*(T** 7.383300E-01)
      C RL 2= 6.407700E-07*(T** 7.999600E-01)
      C BINARY DIFFUSION COEFFICIENTS FROM WARNATZ ST PAR.
      C LEAST SQUARES FIT, T=300,2000.
      C PRESS = 1.00
      C D 1 1= 1.119300E-04*(T** 1.661400E+00)
      C D 1 2= 5.951700E-05*(T** 1.663800E+00)
      C D 2 2= 1.537400E-05*(T** 1.672900E+00)
      C DEFINE USEFUL COMBINATIONS AND DERIVATIVES
      YS=Y 3
      X 1=Y 1/Y
      X 2=Y 2/Y
      U 1=U( 1)
      DU 1=UPH( 1)
      DUU 1=UPH2( 1)
      U 2=1.0-U 1
      DU 2=-DU 1
      DUU 2=-DUU 1
      DY 1=DU 1/ 2.00
      DY 2=DU 2/ 28.00
      DYS=+DY 1+DY 2
      DDY 1=DUU 1/ 2.00
      DDY 2=DUU 2/ 28.00
      DDYS=+DDY 1+DDY 2
      C TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03
      DRH=- 1.218769043266E-02*(DT/T+DYS/YS)/(T*YS)
      DYS=DYS/(YS*YS)
      DYSYSO=(DYS/YS)**2
      DX 1=DY 1/Y-YS 1*DY
      DX 2=(DDY 1-2.0*DY 1*DYS/YS+2.0*Y 1*DDYS/YS)/YS
      CSZR 1= 3.571428571429E-03
      UCSZR 1=0.0
      CZ 1 1=1.0+ 1.061032953946E+00*(CSZR 1)
      DCZ 1 1= 1.061032953946E+00*(UCSZR 1)
      CINT 1=C(1ST+1)* 1.006441223833E+00-2.5
      DCINT 1=DC(1ST+1)* 1.006441223833E+00
      CSC 1=CSZR 1/CINT 1
      DCSC 1=(DCSZR 1-CSZR 1*DCINT 1)/CINT 1
      DX 2=DY 2/Y-YS 2*DY

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04/15/80 14.18.15

FTN 4.8*498

76/76 OPT=1 ROUNDED=+*/* TRACE

SUBROUTINE F

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115 DUX 2=10DY 2-2.0*UY 2*UDYS/YS+2.0*Y 2*UDYSQ-Y 2*UDYS/YS)/YS
    CSZR 2= 6.369426751592E-02+ 1.751045651893E+00/
    * SURT(T)+ 3.483292299373E+01/T
    DCZR 2=- ( 8.755228259466E-01/SURT(T)+ 3.483292299373E+01/T)*DT/T
    CZ 2 2=1.0+ 1.061032953946E+00*(CSZR 2)
    DCZ 2 2= 1.061032953946E+00*(DCZR 2)
    CINT 2=C(IST+ 2)* 1.409017713366E+01-2.5
    UCINT 2=DC(IST+ 2)* 1.409017713366E+01
    CSC 2=CSZR 2/CINT 2
    DCSC 2=(DCZR 2-CSZR 2*DCINT 2/CINT 2)/CINT 2
    X 1 1=X 1*X 1
    UX 1 1=DX 1*X 1*X 1*UX 1
    VU 1 1= 8.934155275619E+03*(T**(-1.661400E+00))
    DVU 1 1= -1.484320557491E+04*(T**(-2.661400E+00))*DT
    XSD 1 1=X 1 1*VD 1 1
    UXSD 1 1=DX 1 1*VD 1 1*X 1 1*VDV 1 1
    X 1 2=X 1*X 2
    UX 1 2=DX 1*X 2*X 1*UX 2
    VD 1 2= 1.680192213989E+04*(T**(-1.663800E+00))
    VVD 1 2= -2.795503805635E+04*(T**(-2.663800E+00))*DT
    XSD 1 2=X 1 2*VD 1 2
    UXSD 1 2=DX 1 2*VD 1 2*X 1 2*VDV 1 2
    CZ 1 2=1.0+ 5.305164769730E-01*(CSZR 1+CSZR 2)
    UCZ 1 2= 5.305164769730E-01*(DCSZR 1+DCSZR 2)
    X 2 2=X 2*X 2
    UX 2 2=DX 2*X 2*X 2*UX 2
    VD 2 2= 6.504488096787E+04*(T**(-1.672900E+00))
    DVD 2 2= -1.088135813711E+05*(T**(-2.672900E+00))*DT
    XSD 2 2=X 2 2*VD 2 2
    UXSD 2 2=DX 2 2*VD 2 2*X 2 2*VDV 2 2
    XSD 1=X 1 2*VD 1 2
    UXSD 1=X 1 2*VD 1 2*X 1 2*VDV 1 2
    XSD 2=X 1 2*VD 2 2
    UXSD 2=X 1 2*VD 2 2*X 1 2*VDV 1 2
    XSD 2=X 1 2*VD 1 2
    UXSD 2=X 1 2*VD 1 2*X 1 2*VDV 1 2
    STV 1= 4.568922191255E+05*(T**(-1.650290E+00))
    USTV 1= -7.540046603006E+05*(T**(-2.650290E+00))*DT
    XSTV 1=X 1 1*STV 1
    UXSTV 1=DX 1 1*STV 1*X 1 1*VDV 1 1
    STV 2= 2.343731689596E+05*(T**(-1.661360E+00))
    USTV 2= -3.893782079828E+05*(T**(-2.661360E+00))*DT
    XSTV 2=X 2 2*STV 2
    UXSTV 2=DX 2 2*STV 2*X 2 2*VDV 2 2
    C SPECIFIC HEAT OF THE MIXTURE. THIS FORMULA.
    CM(TIC)=C(IST+ 1)*U 1+C(IST+ 2)*U 2
    C DIFFUSION AND HEAT FLUX.
    C SEE DIXON-LEWIS.
    C 11. TRANSPORT PHENOMENA IN MULTICOMPONENT SYSTEMS.
    C LM 00+00
    Z( 1, 1)=0.0
    Z( 2, 2)=0.0
    Z( 1, 2)=XSD 1 2+ 1.400000000000E+01*X 2*5XSD 1
    Z( 2, 1)=XSD 1 2+ 1.400000000000E+01*(UX 2*5XSD 1+X 2*USXSD 1)
    Z( 1, 1)=XSD 1 2+ 7.142857142857E-02*X 1*5XSD 2
    Z( 2, 1)=XSD 1 2+ 7.142857142857E-02*(UX 1*5XSD 2+X 1*USXSD 2)
    C FIND T*, A*, R*, AND C*.

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175      TS=1/ 6.086871E+01
        DT=DT/ 6.086871E+01
        AST 1 2= 1.088500E+00*(TS**(-9.055700E-03))
        DAST 1 2= 9.857129450000E-03*DT*(TS**(-9.909443E-01))
        EX=EXP( 8.500100E-02/TS)
        BST 1 2= 1.078600E+00*EX
        DBST 1 2= -9.168208E-02*DT*EX/(TS*TS)
        EX=EXP(-1.435700E-01/TS)
        CST 1 2= 9.542600E-01*EX
        DCST 1 2= 1.370031E-01*DT*EX/(TS*TS)
C      LM 00,10 AND LM 10*00
        CT= -1.666666666667E-01*(1.2*CT 1 2-1.0)
        DCT= -2.000000000000E-01*DCST 1 2
        Z( 1, 4)=CT*XSD 1 2
        DZ 1S 4=CT*DXSD 1 2+DCT*XSD 1 2
        CT= -2.333333333333E+00*(1.2*CT 1 2-1.0)
        DCT= -2.800000000000E+00*DCST 1 2
        Z( 2, 3)=CT*XSD 1 2
        DZ 2S 3=CT*DXSD 1 2+DCT*XSD 1 2
        Z( 1, 3)=-Z( 2, 3)
        DZ 1S 3=-DZ 2S 3
        Z( 2, 4)=-Z( 1, 4)-Z( 3, 4)
        DZ 2S 4=-DZ 1S 4-DZ 3S 4
        Z( 2, 4)=-Z( 1, 4)
        DZ 2S 4=-DZ 1S 4
        Z( 3, 1)=Z( 1, 3)
        DZ 3S 1=DZ 1S 3
        Z( 3, 2)=Z( 2, 3)
        DZ 3S 2=DZ 2S 3
        Z( 4, 1)=Z( 1, 4)
        DZ 4S 1=DZ 1S 4
        Z( 4, 2)=Z( 2, 4)
        DZ 4S 2=DZ 2S 4
C      LM 01,00 AND LM 00*01
        Z( 5, 1)=0.0
        Z( 5, 2)=0.0
        Z( 6, 1)=0.0
        Z( 6, 2)=0.0
        Z( 1, 5)=0.0
        Z( 1, 6)=0.0
        Z( 2, 5)=0.0
        Z( 2, 6)=0.0
C      LM 10,10
        CT= 6.222222222222E-02*(13.75-3.0*BST 1 2-4.0*AST 1 2+CT 1 2)
        DCT=- 6.222222222222E-02*(3.0*DT*ST 1 2+4.0*(AST 1 2+DCT 1 2
          *+DAST 1 2+CT 1 2))
        Z( 3, 4)=CT*XSD 1 2
        DZ 3S 4=CT*DXSD 1 2+DCT*XSD 1 2
        Z( 4, 3)=Z( 3, 4)
        DZ 4S 3=DZ 3S 4
        CT= -4.062563477554E-02*CT 1 1
        DCT= -4.062563477554E-02*DCT 1 1
        CT 2= 2.488888888889E-01*AST 1 2*CT 1 2
        DCT 2= 2.488888888889E-01*(DAST 1 2+CT 1 2+AST 1 2+DCT 1 2)
        CT 2= 5.477777777777E+00- 2.613333333333E+00*HST 1 2+CT 2
        DCT 2=- 2.613333333333E+00*DHST 1 2+DCT 2
        Z( 3, 3)=CT*XSTV 1-XSD 1 2*CT 2

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04/15/80 14.18.15

FTN 4.8+498

76/76 OPT=1 ROUND=+*/ THACE

SUBROUTINE F

```
230      DZ 3S 3=CT*DXSTV 1+DCT*XSTV 1-DXSD 1 2*CT 2-XSD 1 2*DCST 2
      CT= -5.687588868576E-01*CZ 2 2
      DCT= -5.687588868576E-01*UCZ 2 2
      CT 1= 2.4888888888889E-01*AST 1 2*CT 1 2
      DCT 1= 2.4888888888889E-01*(DAST 1 2*CT 1 2+AST 1 2*DCST 1 2)
      CT 1= 6.4561111111111E+00- 1.3333333333333E-02*BST 1 2*CT 1
      DCT 1= 1.3333333333333E-02*BST 1 2*DCST 1
      DZ 4S 4=CT*DXSTV 2-XSD 1 2*CT 1
      DZ 4S 4=CT*DXSTV 2+DCT*XSTV 2-DXSD 1 2*CT 1-XSD 1 2*DCST 1
      C LM 10*01 AND LM 01*10
      CT= 2.970892271049E+00*AST 1 2*DCSC 2
      DCT= 2.970892271049E+00*(DAST 1 2*DCSC 2+AST 1 2*DCSC 2)
      Z( 3, 6)=XSD 1 2*CT
      DZ 3S 6=DXSD 1 2*CT+XSD 1 2*DCST
      CT= 2.122065907892E-01*AST 1 2*DCSC 1
      DCT= 2.122065907892E-01*(DAST 1 2*DCSC 1+AST 1 2*DCSC 1)
      Z( 4, 5)=XSD 1 2*CT
      DZ 4S 5=DXSD 1 2*CT+XSD 1 2*DCST
      CT= 6.465770590774E-02*DCSC 1
      DCT= 6.465770590774E-02*DCSC 1
      CT 2= 2.122065907892E-01*AST 1 2*DCSC 1
      DCT 2= 2.122065907892E-01*(DAST 1 2*DCSC 1+AST 1 2*DCSC 1)
      Z( 3, 5)=CT*XSTV 1+CT 2*XSD 1 2
      DZ 3S 5=CT*DXSTV 1+DCT*XSTV 1+CT 2*DXSD 1 2+DCT 2*XSD 1 2
      CT= 9.052078827083E-01*DCSC 2
      DCT= 9.052078827083E-01*DCSC 2
      CT 1= 2.970892271049E+00*AST 1 2*DCSC 2
      DCT 1= 2.970892271049E+00*(DAST 1 2*DCSC 2+AST 1 2*DCSC 2)
      Z( 4, 6)=CT*XSTV 2+CT 1*XSD 1 2
      DZ 4S 6=CT*DXSTV 2+DCT*XSTV 2+CT 1*DXSD 1 2+DCT 1*XSD 1 2
      Z( 5, 3)=Z( 3, 5)
      DZ 5S 3=DZ 3S 5
      Z( 5, 4)=Z( 4, 5)
      DZ 5S 4=DZ 4S 5
      Z( 6, 3)=Z( 3, 6)
      DZ 6S 3=DZ 3S 6
      Z( 6, 4)=Z( 4, 6)
      DZ 6S 4=DZ 4S 6
      C LM 01*01
      Z( 5, 6)=0.0
      Z( 6, 5)=0.0
      CTM=-6.25/CINT 1
      DCTM=6.25*DCINT 1/(CINT 1*CINT 1)
      CT= 1.551784941786E-02*DCSC 1
      DCT= 1.551784941786E-02*DCSC 1
      CT 2=1.0+ 5.456740906008E-02*AST 1 2*DCSC 1
      DCT 2= 5.456740906008E-02*(DAST 1 2*DCSC 1+AST 1 2*DCSC 1)
      SUM=CT*XSTV 1+XSD 1 1+CT 2*XSD 1 2
      USUM=DCT*XSTV 1+CT*DXSTV 1+DXSD 1 1+CT 2*DXSD 1 2+DCT 2*XSD 1 2
      Z( 5, 5)=CTM*SUM
      DZ 5S 5=DCTM*SUM+CTM*DSUM
      CTM=-6.25/CINT 2
      DCTM=6.25*DCINT 2/(CINT 2*CINT 2)
      CT= 2.172498918500E-01*DCSC 2
      DCT= 2.172498918500E-01*DCSC 2
      CT 1=1.0+ 1.069521217578E+01*AST 1 2*DCSC 2
      DCT 1= 1.069521217578E+01*(DAST 1 2*DCSC 2+AST 1 2*DCSC 2)
      Z( 5, 4)=1.069521217578E+01*AST 1 2*DCSC 2
```

```

SUM=CT*XS*STV 2*XS 2 2*CT 1*XS 1 2
DSUM=DT*XS*STV 2*CT*XS*STV 2*XS 2 2*CT 1*XS 1 2
Z( 6, 6)=CTM*SUM
DZ 6S 6=CTM*SUM+CIM*DSUM
C SOLVE FOR DIFFUSION VELOCITIES AND ENERGY FLUX.
CALL DEC( 6,30,Z,V,1PS,IER)
V( 1)=RH*DX 1/ S.0000000E-05
V( 1)=(DRH*DX 1+RH*DX 1)/ S.0000000E-05
V( 2)=RH*DX 2/ S.0000000E-05
V( 2)=(DRH*DX 2+RH*DX 2)/ S.0000000E-05
V( 3)=0.0
DV 3=0.0
V( 4)=0.0
DV 4=0.0
V( 5)=0.0
DV 5=0.0
V( 6)=0.0
DV 6=0.0
CALL SOL( 6,30,Z,V,1PS)
DV( 1)=DV 1-DZ 1S 2*V( 2)-DZ 1S 3*V( 3)-DZ 1S 4*V( 4)
DV( 2)=DV 2-DZ 2S 1*V( 1)-DZ 2S 3*V( 3)-DZ 2S 3*V( 3)-
* DZ 2S 4*V( 4)
DV( 2)=DV 2-DZ 2S 1*V( 1)-DZ 2S 3*V( 3)-DZ 2S 4*V( 4)
DV( 3)=DV 3-DZ 3S 1*V( 1)-DZ 3S 2*V( 2)-DZ 3S 3*V( 3)-
* DZ 3S 4*V( 4)-DZ 3S 5*V( 5)-DZ 3S 6*V( 6)
DV( 4)=DV 4-DZ 4S 1*V( 1)-DZ 4S 2*V( 2)-DZ 4S 3*V( 3)-
* DZ 4S 4*V( 4)-DZ 4S 5*V( 5)-DZ 4S 6*V( 6)
DV( 5)=DV 5-DZ 5S 3*V( 3)-DZ 5S 4*V( 4)-DZ 5S 5*V( 5)
DV( 6)=DV 6-DZ 6S 3*V( 3)-DZ 6S 4*V( 4)-DZ 6S 6*V( 6)
CALL SOL( 6,30,Z,DV,1PS)
VX 1=V( 1)
DVX 1=DV( 1)
VX 2=V( 2)
DVX 2=DV( 2)
V( 1)=0.0
DV 1=0.0
V( 2)=0.0
DV 2=0.0
V( 3)=X 1
DV 3=DX 1
V( 4)=X 2
DV 4=DX 2
V( 5)=X 1
DV 5=DX 1
V( 6)=X 2
DV 6=DX 2
CALL SOL( 6,30,Z,V,1PS)
DV( 1)=DV 1-DZ 1S 2*V( 2)-DZ 1S 3*V( 3)-DZ 1S 4*V( 4)
DV( 2)=DV 2-DZ 2S 1*V( 1)-DZ 2S 3*V( 3)-DZ 2S 3*V( 3)-
* DZ 2S 4*V( 4)
DV( 2)=DV 2-DZ 2S 1*V( 1)-DZ 2S 3*V( 3)-DZ 2S 4*V( 4)
DV( 3)=DV 3-DZ 3S 1*V( 1)-DZ 3S 2*V( 2)-DZ 3S 3*V( 3)-
* DZ 3S 4*V( 4)-DZ 3S 5*V( 5)-DZ 3S 6*V( 6)
DV( 4)=DV 4-DZ 4S 1*V( 1)-DZ 4S 2*V( 2)-DZ 4S 3*V( 3)-
* DZ 4S 4*V( 4)-DZ 4S 5*V( 5)-DZ 4S 6*V( 6)
DV( 5)=DV 5-DZ 5S 3*V( 3)-DZ 5S 4*V( 4)-DZ 5S 5*V( 5)
DV( 6)=DV 6-DZ 6S 3*V( 3)-DZ 6S 4*V( 4)-DZ 6S 6*V( 6)

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04/15/80 14.18.15

FIN 4.8*498

76/76 OPT=1 ROUNDO=+-*/ TRACE

SUBROUTINE F

```

345 CALL SCL( 6,30,Z,DV,1PS)
VT 1=-2.5*RH*DT*V( 1)/(T* 5.000000E-05)
VT 2=-2.5*RH*DT*V( 2)/(T* 5.000000E-05)
DDT=UPH2(NPDE)* 1.000000E+03
DVT 1=-2.5*(DRH*DT*V( 1)+RH*DDT*V( 1)-RH*DT*V( 1))*
* DT/T)/(T* 5.000000E-05)
DVT 2=-2.5*(DRH*DT*V( 2)+RH*DDT*V( 2)-RH*DT*V( 2))*
* DT/T)/(T* 5.000000E-05)
UV 1=U 1*(VX 1+VT 1)
UV 2=U 2*(VX 2+VT 2)
DUV 1=DU 1*(VX 1+VT 1)+U 1*(DVX 1+DVT 1)
DUV 2=DU 2*(VX 2+VT 2)+U 2*(DVX 2+DVT 2)
RHUV(1ST+ 1)=RH*UV 1
RHUV(1ST+ 2)=RH*UV 2
DRHUV(1ST+ 1)=DRH*UV 1+RH*DUV 1
DRHUV(1ST+ 2)=DRH*UV 2+RH*DUV 2
SUM=+X 1*V( 3)+X 2*V( 4)
USUM=+DX 1*V( 3)+X 1*DV( 3)+DX 2*V( 4)+X 2*DV( 4)
RLTRS= -1.513711E-01*SUM/T
URLTRS= -1.513711E-01*(DSUM-SUM*UT/T)/T
SUM=+X 1*V( 5)+X 2*V( 6)
USUM=+DX 1*V( 5)+X 1*DV( 5)+DX 2*V( 6)+X 2*DV( 6)
RLINT= -1.513711E-01*SUM/T
URLINT= -1.513711E-01*(DSUM-SUM*UT/T)/T
RLM=RLTRS+RLINT
URLM=URLTRS+URLINT
RHLM(1C)=RH*RLM
DRHLM(1C)=DRH*RLM+RH*URLM
SUM=+DX 1*V( 1)+DX 2*V( 2)
DSUM=+DDX 1*V( 1)+DX 1*DV( 1)+DDX 2*V( 2)+DX 2*DV( 2)
OX= -1.210968921389E+03*RH*SUM
DUX(1C)= -1.210968921389E+03*(D-H*SUM+RH*DSUM)
C FIND THE TIME DERIVATIVES.
SP=ASP+RSP*TIME
100 CONTINUE
IF (KPDE.EQ.NPDE)GO TO 150
RY= 1.0000000000E-03*P(KPDE)
UY=- 2.0000000000E+01*DRHUV(1ST+KPDE)
FVAL=SP*UPH(KPDE)+UY+RY
RETURN
150 CONTINUE
TL= 4.0000000000E+05*
* (DRHLM(1C)*UPH(NPDE)+RHLM(1C)*UPH2(NPDE))
TU=- 2.0000000000E+01*UPH(NPDE)*( +C(1ST+ 1)*RHUV(1ST+ 1) +
* C(1ST+ 2)*RHUV(1ST+ 2))
TH=- 1.0000000000E-06*( +R( 1)*H(1ST+ 1) +R( 2)*H(1ST+ 2))
TX= -2.000000000000E-02*DUX(1C)
FVAL=SP*UPH(NPDE)+(TL+TH+TD+TX)/UM(1C)
RETURN
END

```



```

1  PROGRAM LOADF(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,
    * TAPE3,TAPE9,TAPE15)
2  MAIN
3  MAIN
4  MAIN
5  C  LOADF CREATES THE SUBROUTINE F IN FLSC.
6  MAIN
7  MAIN
8  MAIN
9  DIMENSION II(72)
10  DIMENSION LB(25),W(25),AU(7,25),AL(7,25)
11  DIMENSION ALO(25),BLU(25),ABD(25,25),BBU(25,25)
12  DIMENSION LBPR(25)
13  DIMENSION III(44)
14  DIMENSION LBROT(25),SGA(25),ESK(25),UM(25),ALP(25),ZROT(25),OF(25)
15  DIMENSION AV(25),BV(25)
16  WRITE(3,1000)
17  FORMAT(1HC,2X,34HWE WANT TO AVOID DIVISION BY ZERO. )
18  WRITE(3,1012)
19  FORMAT(6X,14H00 5 K=1,NPOEM)
20  WRITE(3,1014)
21  FORMAT(6X,32HIF (ABS(U(K)).LT.SMALL)U(K)=SMALL )
22  WRITE(3,1016)
23  FORMAT(1X,1H5,4X,36HIF (ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL )
24  READ(5,12)NLINE
25  C  NLINE IS THE NUMBER OF COMMENT LINES TO BE READ AND PRINTED.
26  OO 20 K=1,NLINE
27  READ(5,22)II
28  WRITE(3,22)II
29  CONTINUE
30  FORMAT(72A1)
31  FORMAT(1X,72A1/)
32  READ(5,12)NSPC
33  NM=NSPC-1
34  LHM=1H-
35  LBU=2HU(
36  LBP=1H)
37  WRITE(3,1020)((LHM,LBU,K,LBP),K=1,NM)
38  FORMAT(6X,6HYN=1,0,8(A1,A2,12,A1),A1,2/(5X,1H*,1X,
39  * 8(A2,12,A1,A1)) )
40  WRITE(3,1025)
41  FORMAT(6X,33HCALL RT(U,YN,R,NPOE,KPDE,IC,KSKR) )
42  WRITE(3,18)NSPC
43  FORMAT(6X,4HIST=,12,7H*(IC-1) )
44  C  ASSUME AT MOST ONE POLAR SPECIES. (OIPOLE MUMENT NON-ZERO).
45  C  THEN A* AND B* CAN BE APPROXIMATED BY LENNARD-JONES COLLISION
46  C  INTEGRALS, EVEN IF THE INPUT PARAMETERS ARE STOCKMAYER.
47  DO 30 K=1,NSPC
48  READ(5,32) LB(K),W(K),OF(K),SGA(K),ESK(K),UM(K),ALP(K),ZROT(K),
49  * LBROT(K)
50  WRITE(6,34)K,LB(K),W(K),OF(K),SGA(K),ESK(K),UM(K),ALP(K),ZROT(K),
51  * LBROT(K)
52  READ(15,36)(AU(L,K),L=1,5),(III(L),L=1,5)
53  WRITE(6,36)(AU(L,K),L=1,5),(III(L),L=1,5)
54  READ(15,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(III(L),L=1,5)
55  WRITE(6,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(III(L),L=1,5)
56  READ(15,37)(AL(L,K),L=4,7),(III(L),L=1,2U)
57  WRITE(6,37)(AL(L,K),L=4,7),(III(L),L=1,2U)
58  CONTINUE
59  FORMAT(A5,7F7.0,A5)
60  FORMAT(2X,14,4X,A5,4X,7F8.2,4X,A5/)
61  FORMAT(5E15.8,5A1)

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04/15/80 14.21.28

FTN 4.8+498

PROGRAM LOADF 76/76 OPT=1 ROUND=**/ TRACE

```

37  FORMAT(4E15.8,20A1)
    READ(5,232)IPN,PHN,TMN
232  FORMAT(1P3E12.4)
    WRITE(3,27)
27   FORMAT(6X,22HIF(KSKI,GT,1)GO TO 100)
    WRITE(3,28)
28   FORMAT(6X,22HIF(KSKR,GT,1)GO TO 125 )
    READ(5,12)NLINE
    DO 40 K=1,NLINE
    READ(5,22)II
    WRITE(3,22)II
40   CONTINUE
C *****
C ENTHALPIES AND HEAT CAPACITIES.
C *****
    WRITE(3,42)
42   FORMAT(6X,24HIF(T,GT,1000.)GO TO 2000)
    DO 50 K=1,NSPC
    WRITE(3,52)K,AL(1,K),AL(2,K)
    WRITE(3,54) (AL(L,K),L=3,5)
    WRITE(3,62)K,AL(6,K),AL(1,K)
    WRITE(3,64)AL(2,K),AL(3,K)
    WRITE(3,66)AL(4,K),AL(5,K)
50   CONTINUE
52   FORMAT(6X,1HC,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
54   FORMAT(5X,1H*,1X,3(4H+T*(,1PE16.8),5H))))))
    WRITE(3,56)
56   FORMAT(6X,10HGO TO 3000)
    WRITE(3,58)
58   FORMAT(4H2000,2X,8HCONTINUE)
    DO 60 K=1,NSPC
    WRITE(3,52)K,AU(1,K),AU(2,K)
    WRITE(3,54) (AU(L,K),L=3,5)
    WRITE(3,62)K,AU(6,K),AU(1,K)
    WRITE(3,64)AU(2,K),AU(3,K)
    WRITE(3,66)AU(4,K),AU(5,K)
60   CONTINUE
62   FORMAT(6X,1H*,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
64   FORMAT(5X,1H*,1X,4H+T*(,1PE16.8,4H/2.0,4H+T*(,1PE16.8,4H/3.0)
66   * 4H/5.0,6H))))))
    WRITE(3,68)
68   FORMAT(4H3000,2X,8HCONTINUE)
    WRITE(3,134)
134  FORMAT(1HC,2X,39HSPECIFIC HEATS AND SPECIFIC ENTHALPIES. )
    DO 140 K=1,NSPC
    WRITE(3,142)K,K*W(K)
    WRITE(3,144)K,K*W(K)
140  CONTINUE
142  FORMAT(6X,6HC(1ST+,12,3H)=C,12,1H/,F6.2)
144  FORMAT(6X,6HH(1ST+,12,3H)=H,12,1H/,F6.2)
    WRITE(3,146)
146  FORMAT(1X,3H125,2X,8HCONTINUE)
C *****
C THERMAL CONDUCTIVITIES AND BINARY DIFFUSION COEFFICIENTS.
C READ IN VISCOSITY, THERMAL CONDUCTIVITY, AND BINARY DIFFUSION
C COEFFICIENTS FROM A FILE CREATED BY VALUES. CY=5.

```



```
115 C *****
      READ(5,12)NLINE
      DO 72 K=1,NLINE
      READ(5,22)II
      WRITE(3,22)II
      CONTINUE
120 72 FORMAT(1HC,5X,IHV,12,1H=,1PE14.6,5H*(T**,1PE14.6,1H) )
      READ(5,12)NLINE
      DO 70 K=1,NLINE
      READ(5,22)II
      WRITE(3,22)II
      CONTINUE
125 70 DO 80 K=1,NSPC
      READ(9,82)AV(K),BV(K),III
      WRITE(6,84)K,L8(K),AV(K),BV(K),III
      READ(9,82)ALD(K),BLD(K),III
      WRITE(6,84)K,L8(K),ALD(K),BLD(K),III
      CONTINUE
130 80 FORMAT(1P2E14.6,44A1)
      82 FORMAT(2X,I4,4X,A4,4X,1P2E14.6,44A1/)
      84 DO 76 K=1,NSPC
      WRITE(3,78)K,AV(K),BV(K)
      DO 90 K=1,NSPC
      WRITE(3,92)K,ALD(K),BLD(K)
      CONTINUE
135 90 CONTINUE
      92 FORMAT(6X,2HRL,12,1H=,1PE14.6,5H*(T**,1PE14.6,1H) )
      READ(5,12)NLINE
      DO 100 K=1,NLINE
      READ(5,22)II
      WRITE(3,22)II
      CONTINUE
140 100 NM=NSPC-1
      DO 110 I=1,NSPC
      DO 110 J=1,NSPC
      READ(9,82)ABD(I,J),HBD(1,J),III
      WRITE(6,112)I,J,LH(1),LB(J),ABD(I,J),HBD(1,J),III
      CONTINUE
145 110 CONTINUE
      112 FORMAT(2X,I4,4X,I4,4X,A4,4X,1P2E14.6,44A1/)
      HEAD(5,114)PRESS
      FORMAT(F6.0)
      WRITE(3,116)PRESS
      WRITE(6,116)PRESS
      FORMAT(1HC,2X,7HPRESS =,F6.2)
      DO 120 I=1,NSPC
      DO 120 J=1,NSPC
      ABD(I,J)=ABD(I,J)/PRESS
      WRITE(3,122)I,J,ABD(I,J),HBD(1,J)
      CONTINUE
150 120 CONTINUE
      122 FORMAT(6X,IHD,2I2,1H=,1PE14.6,5H*(T**,1PE14.6,1H) )
      C *****
      C SPACE DERIVATIVES.
      C *****
      LHP=LH*
      WRITE(3,148)
      148 FORMAT(1HC,2X,1HSPACE DERIVATIVE+S.)
      NS=NSPC+1
      WRITE(3,149)NS
155 170 MAIN
156 MAIN
157 MAIN
158 MAIN
159 MAIN
160 MAIN
161 MAIN
162 MAIN
163 MAIN
164 MAIN
165 MAIN
166 MAIN
167 MAIN
168 MAIN
169 MAIN
170 MAIN
171 MAIN
172 MAIN
```

04/15/80 14.21.28

PROGRAM LOAOF 76/76 OPT=1 ROUNO=+*/ THACE FTN 4.8+98

```

149  FORMAT(6X,4HYS=Y,I2)
150  DO 150 K=1,NSPC
151  WRITE(3,152)K,K
152  CONTINUE
153  FORMAT(6X,1HX,I2,2H=Y,I2,3H/YS)
154  DO 160 K=1,NM
155  WRITE(3,162)K,K
156  WRITE(3,164)K,K
157  WRITE(3,166)K,K
158  CONTINUE
159  FORMAT(6X,1HU,I2,3H=U(,I2,1H))
160  FORMAT(6X,2H DU,I2,5H=UPH(,I2,1H))
161  FORMAT(6X,3HDDU,I2,6H=UPH2(,I2,1H))
162  LBU=1HU
163  WRITE(3,172)NSPC,((LBM,LBU,K),K=1,NM)
164  FORMAT(6X,1HU,I2,4H=1.0,8(A1,I2),A1,2(/5X,1H*,1X,
165  * 8(A1,I2,A1)) )
166  LBDU=2H DU
167  WRITE(3,174)NSPC,((LBM,LBDU,K),K=1,NM)
168  FORMAT(6X,2H DU,I2,1H=8(A1,A2,I2),A1,2(/5X,1H*,1X,
169  * 8(A2,I2,A1)) )
170  LBDU=3HDDU
171  WRITE(3,176)NSPC,((LBM,LBDU,K),K=1,NM)
172  FORMAT(6X,3HDDU,I2,1H=8(A1,A3,I2),A1,2(/5X,1H*,1X,
173  * 8(A3,I2,A1)) )
174  DO 180 K=1,NSPC
175  WRITE(3,182)K,K,W(K)
176  CONTINUE
177  FORMAT(6X,2HDY,I2,3H=DU,I2,1H/,F6.2)
178  LBDY=2HDY
179  WRITE(3,186)((LBP,LBDY,K),K=1,NSPC)
180  FORMAT(6X,4HDYS=8(A1,A2,I2),A1,2(/5X,1H*,1X,8(A2,I2,A1)) )
181  PSR=PRESS/R2.05
182  WRITE(3,234)TPN,PHN,TMN
183  WRITE(6,234)TPN,PHN,TMN
184  FORMAT(1HC,2X,5HTPN =,1PE12.4,6X,5HPHN =,1PE12.4,6X,
185  * 5HTMN =,1PE12.4)
186  WRITE(3,226)TPN
187  FORMAT(6X,13HDT=UPH(NPDE)*,1PE12.4)
188  WRITE(3,242)PSR
189  FORMAT(6X,5HORH=,1PE18.10,21H*(U/T+DYS/YS)/(T*YS))
190  WRITE(3,1202)
191  FORMAT(6X,16HDYS=DYS/(YS*YS) )
192  DO 1250 K=1,NSPC
193  WRITE(3,1204)K,K,K
194  FORMAT(6X,2HDX,I2,3H=DY,I2,5H=YS-Y,I2,5H*DYYS )
195  A=ALO(K)*BLO(K)
196  H=HLD(K)-1.0
197  WRITE(3,1208)K,A,H
198  FORMAT(6X,2HDL,I2,1H=,1PE20.12,4H*(T*(,1PE14.6,5H))*DT )
199  HG=1.9R72
200  A=15.0*RG*AV(K)/(4.0*W(K))
201  H=HV(K)
202  WRITE(3,1212)K,A,H
203  FORMAT(6X,3HRLZ,I2,1H=,1PE20.12,4H*(T*(,1PE14.6,5H))*DT )
204  A=AH
205  H=H-1.0

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```
230      WRITE(3,1216)K,A,B
      FORMAT(6X,3HDLZ,12,1H=,1PE20.12,6H*(T**,(,1PE14.6,2H)),3H*DT )
      A=ABD(K,K)*BBD(K,K)
      B=BBD(K,K)-1.0
231      WRITE(3,1220)K,K,A,B
      FORMAT(6X,2HDD,212,1H=,1PE20.12,6H*(T**,(,1PE14.6,5H))*DT )
232      A=I.0/AV(K)
      B=-BV(K)
233      WRITE(3,1224)K,A,B
      FORMAT(6X,2HVV,12,1H=,1PE20.12,6H*(T**,(,1PE14.6,2H)) )
234      A=A*B
      B=B-1.0
235      WRITE(3,1228)K,A,B
      FORMAT(6X,3HVV,12,1H=,1PE20.12,6H*(T**,(,1PE14.6,5H))*DT )
236      WRITE(3,1232)K,K,K
      FORMAT(6X,4HXXSV,12,2H=X,12,2H*X,12,3H*VV,12)
237      WRITE(3,1236)K,K,K,K
      FORMAT(6X,5HXXSV,12,6H=2.0*X,12,3H*DX,12,3H*VV,12,2H*X,12,2H*X,
238      * 12,4H*DVV,12)
239      CONTINUE
      DO 1300 I=1,NM
240      1P=1+I
      DO 1300 J=IP,NSPC
      A=I.0/ABD(I,J)
      B=-BBD(I,J)
      WRITE(3,1258)I,J,A,B
241      FORMAT(6X,2HVD,212,1H=,1PE20.12,6H*(T**,(,1PE14.6,2H)) )
      A=A*B
      B=B-1.0
      WRITE(3,1262)I,J,A,B
242      FORMAT(6X,3HVD,212,1H=,1PE20.12,6H*(T**,(,1PE14.6,5H))*DT )
243      WRITE(3,1268)((I,J),L=1,3)
      FORMAT(6X,4HXXSD,212,2H=X,12,2H*X,12,3H*VD,212)
244      WRITE(3,1274)((I,J),L=1,7)
      FORMAT(6X,5HXXSD,212,3H=DX,12,2H*X,12,2H*X,12,2H*X,12,
245      * 3H*DX,12,3H*VD,212,2H*X,12,2H*X,12,4H*DVV,212)
      WRITE(3,1278)I,J,1,J
      FORMAT(6X,5HXXTS,212,5H=XXSD,212,2H*1)
246      WRITE(3,1282)((I,J),L=1,3)
      FORMAT(6X,5HXXTS,212,6H=DXSD,212,7H*1+XXSD,212,3H*DT)
247      CONTINUE
      C *****
      C SPECIFIC HEAT OF THE MIXTURE.
      C *****
248      WRITE(3,124)
      FORMAT(1HC,2X,44HSPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA. )
      LHC=6HC(1ST+
249      LHO=3H)*U
      WRITE(3,132)((LHPL,LHC,K,LBU,K),K=1,NSPC)
250      FORMAT(6X,7HCM(IC)=,4(A1,A6,12,A3,12),A1,
251      * 4(/5X,1H,1X,4(A6,12,A3,12,A1)) )
      C *****
      C THERMAL CONDUCTIVITY OF THE MIXTURE.
      C *****
      C BOLTZMAN CONSTANT.
      HK=1.38054E-16
252      WRITE(3,272)
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PROGRAM LOADF 76/76 OPT=I ROUND=+*/ TRACE

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272 WRITE(3,274)
274 FORMAT(1HC,2X,36HTHERMAL CONDUCTIVITY OF THE MIXTURE.)
276 WRITE(3,276)
276 FORMAT(1HC,2X,35HHIRSHFELDER METHOD FOR MONATOMICS. )
277 WRITE(3,277)
277 FORMAT(1HC,2X,39HP. 37A. TOULOUKIEN, LILEY, AND SAXENA. )
278 *NITS AS D*P/T.
278 WRITE(3,278)
278 FORMAT(1HC,2X,63HLMHDA=15*R*VISC/(4*M), WHERE R=82.05 CM**3-ATM/M
*OLE-K.
279 WRITE(3,279)
279 FORMAT(1HC,2X,69HTO CONVERT LAMHDA BACK TO CAL/CM-SEC-K, MULTIPLY
*BY 1.9872/82.05.
123 READ(5,82)AAS1,8AS1,I11
WRITE(6,123)AAS1,8AS1,I11
FORMAT(/2X,1P2E14.6,44A1)
123 READ(5,82) ABST,8BS1,I11
WRITE(6,123)ABST,8BS1,I11
282 WRITE(3,282)8AST
282 FORMAT(6X,11HTAS1LJ=1**(.1PE14.6,1H) )
284 WRITE(3,284)88ST
284 FORMAT(6X,11HTBS1LJ=1**(.1PE14.6,1H) )
BM=8AST-1.0
310 WRITE(3,1382)8AST,8M
310 FORMAT(6X,6HDTAST=,1PE14.6,8H*DT*1**(.1PE14.6,1H) )
BM=88ST-1.0
1384 WRITE(3,1384)88ST,8M
1384 FORMAT(6X,6HDT8ST=,1PE14.6,8H*DT*1**(.1PE14.6,1H) )
OO 280 I=1,NM
IP=1+1
DO 280 J=1P,NSPC
A=16.0*W(1)*W(J)/(25.0*(W(1)+W(J))*(W(1)+W(J))*PRESS)
B=13.75
ESK1J=SQRT(ESK(1)*ESK(J))
IF(UM(1).EQ.0.0.AND.UM(J).EQ.0.0)GO TO 287
C COMBINING RULE. P. 528, REID AND SHERWOOD.
IF(UM(1).NE.0.0)LP=1
IF(UM(J).NE.0.0)LP=J
IF(LP.EQ.1)LP=J
IF(LP.EQ.J)LP=1
UMP=UM(LP)*1.0E-18
SGC=SGA(LP)*1.0E-8
TPSTAR=UMP*UMP/(ESK(LP)*RK*SGC*SGC*SGC*SORT(8.0))
FC=1.0+(1.0/SORT(2.0))* (ALP(LNP)*TPSTAR/(SGA(LNP)**3))*
* SORT(ESK(LP)/ESK(LNP))
1234 WRITE(6,1234)1J,LP,LNP,FC
FORMAT(4I4,1PE12.4)
ESK1J=ESK1J*FC*FC
287 CONTINUE
C=3.0*8HST/(ESK1J**8HST)
D=4.0*8AAS1/(ESK1J**8AAS1)
AH=A*R
AC=A*C
AU=A*U
340 WRITE(3,286)AH,AC,AU
286 FORMAT(6X,5HCNST=,1PE20.12,1H-,1PE20.12,1H*,/5X,1H*,1X,

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345      * 7HTBSTLJ-,IPE20.12,7H*TASTLJ)
      WRITE(3,1386)AC,AD
1386     FORMAT(6X,6HDCNST=,IH-,IPE20.12,IH*,6HDTBST-,IPE20.12,6H*DTAST)
      WRITE(3,288)I,J,I,J
288     FORMAT(6X,2HZ(,I2,IH,12,IH,12,12H)=CONST*XXTSU,2I2)
      WRITE(3,290)I,J,I,J,I,J,I,J
290     FORMAT(6X,2HDZ,12,IHS,12,IH=CNST*DXTSU,2I2,
      * 12H*DCNST*XXTSU,2I2 )
      WRITE(3,292)J,I,I,J
292     FORMAT(6X,2HZ(,I2,IH,12,4H)=Z(,I2,IH,12,IH) )
      WRITE(3,294)J,I,I,J
294     FORMAT(6X,2HDZ,12,IHS,12,3H=OZ,I2,IHS,I2)
280     CONTINUE
      DO 300 I=I,NSPC
      DO 295 K=I,NSPC
      IF(I.EQ.K)GO TO 295
      IMIN=MIN0(I,K)
      IMAX=MAX0(I,K)
      C=16.0/(25.0*(W(I)+W(K))*(W(I)+W(K))*PRESS)
      U=7.5*W(I)*W(I)+6.25*W(K)*W(K)
      ESKIK=SQRT(ESK(I)*ESK(K))
      IF(UM(I).EQ.0.0.AND.UM(K).EQ.0.0)GO TO 299
      C COMBINING RULE. P. 528, REID AND SHERWOOD.
      IF(UM(I).NE.0.0)LP=I
      IF(UM(K).NE.0.0)LP=K
      IF(LP.EQ.I)LNP=K
      IF(LP.EQ.K)LNP=I
      UMP=UM(LP)*I.0E-18
      SGC=SGA(LP)*I.0E-8
      TPSTAR=UMP*UMP/(ESK(LP)*RK*SGC*SGC*SGC*SQRT(8.0))
      FC=1.0*(1.0/SQRT(2.0))*(ALP(LNP)*TPSTAR/(SGA(LNP)**3))*
      * SQRT(ESK(LP)/ESK(LNP))
      WRITE(6,1234)I,J,LP,LNP,FC
      ESKIK=ESKIK*FC*FC
299     CONTINUE
      E=3.0*W(K)*W(K)*AHST/(ESKIK**BBST)
      F=4.0*W(I)*W(K)*AAST/(ESKIK**BAST)
      CD=C*D
      CE=C*E
      CF=C*F
380
385     WRITE(3,296)CD,CE,CF
      FORMAT(6X,6HDCNST=,IPE20.12,IH*,IPE20.12,IH*,5X,IH*,IX,
      * 7HTBSTLJ-,IPE20.12,7H*TASTLJ )
      WRITE(3,1396)CE,CF
1396     FORMAT(6X,6HDCNST=,IPE20.12,IH*,6HDTBST-,IPE20.12,6H*DTAST)
      WRITE(3,297)K,IMIN,IMAX
297     FORMAT(6X,IHT,I2,7H=-XXTSU,2I2,5H*CNST)
      WRITE(3,298)K,IMIN,IMAX,IMIN,IMAX
298     FORMAT(6X,2HDT,I2,7H=-DXTSU,2I2,5H*CNST,6H-XXTSU,2I2,6H*DCNST )
295     CONTINUE
      LBL=IH
      LBT=IHT
395     C GAS CONSTANT IN CM**3-ATM/MOLE-K.
      RGA=82.05
      A=-16.0*W(I)/(15.0*RGA)
      WRITE(3,302)I,I,A,I
302     FORMAT(6X,2HZ(,I2,IH,12,2H)=,I,20.12,5H*XXSV,12,1H-)

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PROGRAM LOAUF 76/76 OPT=1 KOUNO=**/ TRACE

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400      LBLP=1H(
304      IF(1.EQ.1)WRITE(3,304)LBLP,((LBHL,LBPL,LBT,K),K=2,NSPC),LBP
      FORMAT(5X,1H*,IX,2A1,10(2A1,12,A1),A1,/5X,1H*,IX,10(2A1,12,A1) )
      IF(1.EQ.NSPC)WRITE(3,304)LBLP,((LBHL,LBPL,LBT,K),K=1,NM),LBP
      IF(1.EQ.1.OR.1.EQ.NSPC)GO TO 307
      IM=1-1
      IP=1+1
      WRITE(3,304)LBLP,((LBHL,LBPL,LBT,K),K=1,1M),((LBHL,LBPL,LBT,K),
      * K=IP,NSPC),LBP
307      CONTINUE
      WRITE(3,305)1,1,A,1
305      FORMAT(6X,2H0Z,12,1H5,12,1H=,1PE20,12,6H*0XXSV,12,1H- )
      LBDT=2H0T
306      IF(1.EQ.1)WRITE(3,306)LBLP,((LBHL,LBPL,LBT,K),K=2,NSPC),LBP
      FORMAT(5X,1H*,IX,2A1,10(A1,A2,12,A1),A1,/5X,1H*,1X,
      * 10(A1,A2,12,A1) )
415      IF(1.EQ.NSPC)WRITE(3,306)LBLP,((LBHL,LBPL,LBT,K),K=1,NM),LBP
      IF(1.EQ.1.OR.1.EQ.NSPC)GO TO 309
      IM=1-1
      IP=1+1
      WRITE(3,306)LBLP,((LBHL,LBPL,LBT,K),K=1,1M),((LBHL,LBPL,LBT,K),
      * K=IP,NSPC),LBP
309      CONTINUE
300      CONTINUE
      OO 310 K=1,NSPC
425      WRITE(3,312)K,K
310      CONTINUE
312      FORMAT(6X,2HV,(,12,3H)=X,12)
      NDIM=20
      WRITE(3,428)NSPC,NDIM
430      WRITE(3,432)NSPC,NDIM
      LBX=1HX
      LBV=3H*V(
      C  CONVERT RLM FROM CM**3-ATM/CM-SEC-K TO CAL/CM-SEC-K.
      A=-4.0*RG/RGA
435      WRITE(3,316)A,((LBHL,LBPL,LBX,K,LBV,K,LBP),K=1,NSPC),LBP
      FORMAT(6X,4HRLM=,1PE14.6,2H*(,4(3A1,12,A3,12,A1),2A1,2(/5X,1H*,1X,
      * 5(A1,12,A3,12,3A1)) )
      LR0Z=2H0Z
      LBV=3H*V(
440      LBP=1H)
      LHS=1HS
      LBSP=1HS
      DO 320 I=1,NSPC
445      WRITE(3,322)1,1,((LBHL,LBDZ,1,LB'S,J,LBV,J,LBP),J=1,NSPC)
      CONTINUE
320      CONTINUE
322      * 5(/5X,1H*,1X,4(A2,12,A1,12,A3,12,A1),2,A3,12,A1),A1,
      WRITE(3,546)NSPC,NDIM
      LBHL=1H
      LBX=1HX
      LBV=4H*DV(
450      LR0X=2H0X
      LBV=3H*V(
      * K=1,NSPC),LBP
      FORMAT(6X,5H0RLM=,1PE14.6,2H*(,4(3A1,12,A4,12,2A1,A2,12,A3,12,A1,
      * 5(A1,12,A3,12,3A1)) )
455      * 5(A1,12,A3,12,3A1)) )

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460      * 2A1,10(/5X,1H*,1X,2(A1,12,A4,12,2A1,A2,12,A3,12,3A1)) )
C THE ABOVE IS THE THERMAL CONDUCTIVITY FOR A MIXTURE OF MONATOMIC
C GASES. COMPUTE THE CORRECTION FACTOR FOR POLYATOMIC GASES.
      I=1
      LBX=IHX
      LBDV=3H*VD
      LHDV=2HDX
      LHDVD=4H*DVD
      IF (DF(1).EQ.0.0160 TO 725)
        WRITE(3,702)((LBPL,LBX,J,LBVD,I,J),J=2,NSPC)
        FORMAT(6X,4HSUM=,5(2A1,12,A3,2I2),A1,3(/5X,1H*,1X,
702      * 5(A1,12,A3,2I2,A1)) )
        WRITE(3,706)((LBPL,LHDV,J,LBVD,I,J,LBPL,LBX,J,LBDVD,I,J),J=2,NSPC)
        FORMAT(6X,5HDSUM=,2(A1,A2,12,A3,2I2,A1,12,A4,2I2),A1,
470      * 9(/5X,1H*,1X,2(A2,12,A3,2I2,2A1,12,A4,2I2,A1)) )
        WRITE(3,710)1,1,1
        FORMAT(6X,6H8=1.0,1H0,2I2,6H*SUM/X,12)
710      * 1H0,2I2,6H*SUM/X,12)
        WRITE(3,714)((1),L=1,1)
        FORMAT(6X,5H8=DU,2I2,6H*SUM/X,12,2H*DU,2I2,7H*DSUM/X,12,
475      * 2H*DU,2I2,7H*SUM*DX,12,3H/(X,12,2H*X,12,1H) )
        WRITE(3,718)1,1
        FORMAT(6X,11HRLM=RLM*(RL,12,4H*RLZ,12,3H)/B )
718      * 11HRLM=RLM*(RL,12,4H*RLZ,12,3H)/B )
        WRITE(3,722)1,1,1
        FORMAT(6X,13HDLRM=DRLM*(DL,12,4H*DLZ,12,5H)/B-,(2HRL,12,4H*RLZ,
480      * 12,10H)*DB/(B*B) )
722      * 12,10H)*DB/(B*B) )
725      CONTINUE
      DO 730 I=2,NM
      IF (DF(1).EQ.0.0160 TO 730)
        I=I-1
        I=I+1
        WRITE(3,702)((LBPL,LBX,J,LBVD,I,J),J=1,IM),
485      * ((LBPL,LBX,J,LBVD,I,J),J=1,NSPC)
        WRITE(3,706)((LBPL,LHDV,J,LBVD,I,J,LBPL,LBX,J,LBDVD,I,J),J=1,IM),
490      * ((LBPL,LHDV,J,LBVD,I,J,LBPL,LBX,J,LBDVD,I,J),J=1,NSPC)
        WRITE(3,710)1,1,1
        WRITE(3,714)((1),L=1,1,1)
        WRITE(3,718)1,1
        WRITE(3,722)1,1,1,1
        CONTINUE
730      I=NSPC
      IF (DF(1).EQ.0.0160 TO 735)
        WRITE(3,702)((LBPL,LBX,J,LBVD,I,J),J=1,NM)
        WRITE(3,706)((LBPL,LHDV,J,LBVD,I,J,LBPL,LBX,J,LBDVD,I,J),J=1,NM)
500      * ((LBPL,LHDV,J,LBVD,I,J,LBPL,LBX,J,LBDVD,I,J),J=1,NM)
        WRITE(3,710)1,1,1
        WRITE(3,714)((1),L=1,1,1)
        WRITE(3,718)1,1
        WRITE(3,722)1,1,1,1
        CONTINUE
735      I=NSPC
        WRITE(3,738)
738      * 15HRLM(IC)=RH*RLM
        WRITE(3,742)
742      * 15HRLM(IC)=RH*RLM
C *****
C SOLVE FOR UV.
C *****
400      WRITE(3,400)
        FORMAT(1HC,2X,13HSOLVE FOR UV.)
510      * 13HSOLVE FOR UV.)

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402 WRITE(3,402)NSPC
   FORMAT(6X,2HV(,I2,5H)=0.0 )
   DO 405 K=1,NM
     WRITE(3,408)K,K,PHW
   CONTINUE
408   FORMAT(6X,2HV(,I2,4H)=DX,I2,4H*KH/,IPEI2.4 )
   DO 410 K=1,NSPC
     WRITE(3,412)NSPC,K,K
     WRITE(3,414)NSPC,K,K
   CONTINUE
410   FORMAT(6X,2HZ(,I2,IH,,I2,3H)=U,I2)
412   FORMAT(6X,2HDZ,I2,IHS,I2,3H=DU,I2)
414   DO 415 I=1,NM
     IP=I+1
     DO 415 J=IP,NSPC
       WRITE(3,416)I,J,I,J
       FORMAT(6X,2HZ(,I2,IH,,I2,6H)=XXSD,2I2)
       IF(J.NE.NSPC)WRITE(3,416)J,I,I,J
       WRITE(3,418)I,J,I,J
       FORMAT(6X,2HDZ,I2,IHS,I2,6H=DXSD,2I2)
       IF(J.NE.NSPC)WRITE(3,418)J,I,I,J
       CONTINUE
       I=1
       LBXXSD=4HXXSD
       WRITE(3,422)I,I,((LBM,LBXXSD,I,J),J=2,NSPC)
       FORMAT(6X,2HZ(,I2,IH,,I2,2H)=,4(AI,A4,2I2),AI,
         * 3(/5X,IH*,IX,5(A4,2I2,AI)) )
       LBDS=5HDXSD
       WRITE(3,424)I,I,((LBM,LBD,I,J),J=2,NSPC)
       FORMAT(6X,2HDZ,I2,IHS,I2,IH=,4(AI,A5,2I2),AI,
         * 3(/5X,IH*,IX,5(A5,2I2,AI)) )
       DO 420 I=2,NM
         IM=I-1
         IP=I+1
         WRITE(3,422)I,I,((LBM,LBXXSD,J,I),J=1,IM),
           * ((LBM,LBXXSD,I,J),J=IP,NSPC)
         WRITE(3,424)I,I,((LBM,LBD,J,I),J=1,IM),((LBM,LBD,I,J),J=IP,NSPC)
         CONTINUE
       WRITE(3,428)NSPC,NDIM
       FORMAT(6X,9HCALL DEC(,I2,IH,,I2,1IH,Z,IPS,IER) )
       WRITE(3,432)NSPC,NDIM
       FORMAT(6X,9HCALL SOL(,I2,IH,,I2,9H,Z,V,IPS) )
       DO 435 K=1,NSPC
         WRITE(3,438)K,K,K
       CONTINUE
       FORMAT(6X,2HUV,I2,2H=U,I2,3H*V(,I2,IH) )
       DO 440 K=1,NSPC
         WRITE(3,442)K,K
       CONTINUE
       FORMAT(6X,9HRHUV(IST,.,I2,7H)=RH*UV,I2)
       C *****
       C SOLVE FOR THE SPACE DERIVATIVE OF UV.
       C *****
       WRITE(3,522)
       FORMAT(1HC,2X,30HSPACE DER OF UTILITY TIMES UV.)
       DO 500 K=1,NSPC
         WRITE(3,502)K,K,K(K)
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PROGRAM LOADF 76/76 OPT=I ROUNO=***/ TRACE

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500 CONTINUE
502 FORMAT(6X,3HDDY,I2,4H=DDU,I2,IH/,F6.2)
LDDY=3HDDY
506 WRITE(3,506)((LHPL,LHDDY,K),K=1,NSPC)
575 FORMAT(6X,5HDDYS=,8(A1,A3,I2),A1,2(/5X,1H*,1X,8(A3,I2,A1)) )
510 WRITE(3,510)
510 FORMAT(6X,18HDDYSU=(DYS/YS)**2 )
DO 515 K=1,NSPC
515 WRITE(3,518)K,K,K,K,K
580 CONTINUE
518 FORMAT(6X,3HDDX,I2,5H=(DDY,I2,7H-2.0*DY,I2,13H*DY/YS+2.0*Y,
* 12.9H*DYYSO-Y,I2,12H*DDYS/YS)/YS )
LDDZ=2HDDZ
LDDV=3H*V(
LBS=IHS
585 LBS=IHS
DO 525 I=1,NM
525 WRITE(3,528)I,I,I,PHN,((LBM,LDDZ,I,LBS,J,LBV,J,LBP),J=1,NSPC)
CONTINUE
528 FORMAT(6X,3HDDV(I,I2,9H)=(RH*DDX,I2,7H*DRH*DX,I2,2H)/,
* 1PE12.4,A1,A2,I2,A1,I2,A3,I2,2A1,5(/5X,1H*,1X,
* 4(A2,I2,A1,I2,A3,I2,2A1)) )
I=NSPC
532 WRITE(3,532)I,((LBM,LDDZ,I,LBS,J,LBV,J,LBP),J=1,NSPC)
595 FORMAT(6X,3HDDV(I,I2,2H)=,3(A1,A2,I2,A1,I2,A3,I2,A1),A1,
* 5(/5X,1H*,1X,4(A2,I2,A1,I2,A3,I2,2A1)) )
WRITE(3,546)NSPC,NDIM
546 FORMAT(6X,9HCALL SOL(,I2,IH,I2,10H,Z,DV,IPS) )
DO 550 K=1,NSPC
550 WRITE(3,552)K,K,K,K,K
552 FORMAT(6X,3HDDV,I2,2H=U,I2,4H*DV(,I2,4H)+DU,I2,3H*V(,I2,IH) )
DO 810 K=1,NSPC
560 WRITE(3,812)K,K,K
605 CONTINUE
810 FORMAT(6X,10HDRHUV(IST,,I2,8H)=DRH*UV,I2,7H*RH*DUV,I2)
812 *****
C FIND THE TIME DERIVATIVES.
C *****
610 WRITE(3,612)
612 FORMAT(1HC,2X,26HFINO THE TIME DERIVATIVES.)
622 WRITE(3,622)
622 FORMAT(6X,15HSP=ASP+RSP*TIME)
TMSPH2=TMN/(PHN*PHN)
615 WRITE(3,628)
628 FORMAT(1X,3H100,2X,6HCONTINUE)
632 WRITE(3,632)
632 FORMAT(6X,25HIF(KPDE.EQ.NPDE)GO TO 150)
636 WRITE(3,636)TMN
620 FORMAT(6X,3HRY=,1PE20.10,8H*(KPDE) )
TMSPH=TMN/PHN
638 WRITE(3,638)TMSPH
638 FORMAT(6X,4HUY=,1PE20.10,16H*DU+HUV(IST*KPDE) )
642 WRITE(3,642)
642 FORMAT(6X,23HVAL=SP*UPH(KPDE)+UY+RY)
646 WRITE(3,646)
646 FORMAT(6X,6HRETURN)

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FIN 4.8+49H

PROGRAM LOADF 76/76 OPT=I ROUNO=***/ TRACE

```

630      WRITE(3,648)
        FORMAT(IX,3H150,2X,4HCONTINUE)
        WRITE(3,662)TMSPH2
662      FORMAT(6X,3HTL=,IPE20,I0,IH*)
        WRITE(3,664)
664      FORMAT(5X,IH*,IX,4IH(DRHLM(IC)*UPH(NPDE)+RHLM(IC)*UPH2(NPDE)))
        LBL=IH
        LHC=6HC(IST+
        LBRHUV=10H)*RHUV(ISI
        WRITE(3,668)TMSPH,((LBBL,LBPL,LHC,K,LBRHUV,LBPL,K,LBP),K=1,NSPC)
        * ,LBP
668      FORMAT(6X,4HTD=,IPE20,I0,I2H*UPH(NPDE)*(.2AI,A6,I2,A10,AI,I2,3AI,
        * I0,I/5X,IH*,IX,2(A6,I2,A10,AI,I2,3AI)) )
        TMSPT=TMN/TPN
        LBR=2HR(
        LBH=8H)*H(IST+
        WRITE(3,672)TMSPT,((LBBL,LBPL,LBR,K,LBH,K,LBP),K=1,NSPC),LBP
672      FORMAT(6X,4HTR=,IPE20,I0,2H* (.2(2AI,A2,I2,A8,I2,A1),2AI,
        * 9(I/5X,IH*,IX,2(A2,I2,A8,I2,3AI)) )
        WRITE(3,676)
676      FORMAT(6X,3SHFVAL=SP*UPH(NPDE)+ (TL+TR+TD)/CM(IC) )
        STOP
        END
650
629      MAIN
630      MAIN
631      MAIN
632      MAIN
633      MAIN
634      MAIN
635      MAIN
636      MAIN
637      MAIN
638      MAIN
639      MAIN
640      MAIN
641      MAIN
642      MAIN
643      MAIN
644      MAIN
645      MAIN
646      MAIN
647      MAIN
648      MAIN
649      MAIN
650      MAIN
651      MAIN

```

BLOCK	ADDRESS	LENGTH	FILE
LOADF	110	12777	LGO
/STP.END/	13107	1	SL-F-TNLIH
/FCL.C./	13110	30	SL-F-TNLIH
/QB.I0./	13140	144	SL-F-TNLIH
Q2NTRY=	13304	4	SL-F-TNLIH
CUMIO=	13310	10	SL-F-TNLIH
FECMSK=	13320	41	SL-F-TNLIH
FEFST=	13361	3	SL-F-TNLIH
FLTIN=	13364	156	SL-F-TNLIH
FLTOUT=	13542	315	SL-F-TNLIH
FMTAP=	14057	377	SL-F-TNLIH
FORSYS=	14456	300	SL-F-TNLIH
FORUTL=	14756	45	SL-F-TNLIH
GETFIT=	15023	54	SL-F-TNLIH
INCOM=	15077	144	SL-F-TNLIH
INPC=	15243	173	SL-F-TNLIH
KODER=	15436	476	SL-F-TNLIH
KRAKER=	16134	454	SL-F-TNLIH
OUTC=	16610	155	SL-F-TNLIH
OUTCOM=	16765	204	SL-F-TNLIH
ERRCAP=	17171	317	SL-F-TNLIH
FERCAP=	17510	171	SL-F-TNLIH
ALOG.	17701	63	SL-F-TNLIH
EXP.	17764	73	SL-F-TNLIH
EXP.MSG	20057	16	SL-F-TNLIH
SQRT	20075	6	SL-F-TNLIH
SQRT.	20103	32	SL-F-TNLIH
SYS.AID=	20135	1	SL-F-TNLIH
SYS=IST	20136	65	SL-F-TNLIH
SYS=AID	20223	7	SL-F-TNLIH
XIOY*	20232	11	SL-F-TNLIH
XIOY.	20243	32	SL-F-TNLIH

1	H2	2.00	2.00	2.92	38.00	0.00	.79	280.00	CNST
.31001901E+01	.51119464E+03	.52644210E-07	-.34909973E-10	.36945345E-14	H2				
-.87738042E+03	-.19629421E+01	.30574451E+01	.26765200E-02	-.58099162E-05	H2				
.55210391E-08	-.18122739E-11	-.98890474E+03	-.22997056E+01		H2				
2	N2	28.00	2.00	3.62	97.50	0.00	0.00	15.70	VAR
.28963194E+01	.15154866E-02	-.57235277E-06	.99807393E-10	-.65223555E-14	N2				
-.90586184E+03	.61615148E+01	.36748261E+01	-.12081500E-02	.23240102E-05	N2				
-.63217559E-09	-.22577253E-12	-.10611588E+04	.23580424E+01		N2				
1	H2	2.188700E-06	6.502900E-01		H2				VISCOSITY.
1	H2	6.357900E-06	7.383300E-01		H2				HERMAL CONDUCTIVITY.
2	N2	4.266700E-06	6.613600E-01		N2				VISCOSITY.
2	N2	6.407700E-07	7.999600E-01		N2				HERMAL CONDUCTIVITY.

1	1	H2	H2	1.119300E-04	1.661400E+00	H2	H2	BINARY DIFFUSION.
1	2	H2	N2	5.951700E-05	1.663800E+00	H2	N2	BINARY DIFFUSION.
2	2	N2	N2	1.537400E-05	1.672900E+00	N2	N2	BINARY DIFFUSION.

PRESS = 1.00
 TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03
 1.088500E+00 9.055700E-03 A* P. 1128, HIRSHFELDER, ET. AL.
 1.129600E+00 -1.022500E-02 B* P. 1128, HIRSHFELDER, ET. AL.

```

1 SUBROUTINE F (TIME,PH,U,UPH,UPH2,FVAL,NPDE,KPDE,IC,KSKT,KSKR)
  DIMENSION Z(20,20),IPS(20)
  DIMENSION V(20),DV(20)
  DIMENSION U(NPDE),UPH(NPDE),UPH2(NPDE)
  COMMON/TARAB/ASP,ASP,TPN,PHN,IMN,TMSPH,TMSPH2,TMSTP,TPENT
  COMMON/TARP/PRESS,PSK,NPDEM
  COMMON/TARSM/SMALL
  COMMON/TARAM/YAB,WAB
  DIMENSION R(20)
  DIMENSION C(I000),H(I000),RHLM(I00),ORHLM(I00),CM(I00)
  COMMON/TABCT/RL,CPMK,H0(20),R2D(20),R2DM(20)
  COMMON/TARMF/RHUV(I000),ORHUV(I000)
  COMMON/TARRY/T,RH,Y1,Y2,Y3,Y4,Y5,Y6,Y7,Y8,Y9,Y10
  C AT EACH CALL THE TIME RATE OF CHANGE FOR ONE PUE IS RETURNED IN FVAL.
  C WE WANT TO AVOID DIVISION BY ZERO.
    00 5 K=I,NPDEM
    IF (ABS(U(K)).LT.SMALL)U(K)=SMALL
    IF (ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL
  5 C TEST CASE. BINARY MIX OF H2 AND N2. TRANSPORT WARNATZ PAR.
  C U = MASS FRACTIONS. Y = MASS FRACTIONS / MOLECULAR WEIGHTS.
    YN=1.0-U( 1)
    CALL RT(U,YN,R,NPDE,KPDE,IC,KSKK)
    IST= 2*(IC-I)
    IF (KSKT.GT.1)GO TO 100
    IF (KSKR.GT.1)GO TO 125
  25 C NTIS ENTHALPIES AND HEAT CAPACITIES.
    IF (T.GT.1000.)GO TO 2000
    C I=1.9872*( 3.05744510E+00+T*( 2.67652000E-03
      *+T*( -5.80991620E-06+T*( 5.52103910E-09+T*( -1.81227390E-12))))))
    H 1=1.9872*( -9.88904740E+02+T*( 3.05744510E+00
      *+T*( 2.67652000E-03/2.0+T*( -5.80991620E-06/3.0
      *+T*( 5.52103910E-09/4.0+T*( -1.81227390E-12/5.0))))))
    C 2=1.9872*( 3.67482610E+00+T*( -1.20815000E-03
      *+T*( 2.32401020E-06+T*( -6.32175590E-10+T*( -2.25772530E-13))))))
    H 2=1.9872*( -1.06115880E+03+T*( 3.67482610E+00
      *+T*( -1.20815000E-03/2.0+T*( 2.32401020E-06/3.0
      *+T*( -6.32175590E-10/4.0+T*( -2.25772530E-13/5.0))))))
    GO TO 3000
  2000 CONTINUE
    C I=1.9872*( 3.10019010E+00+T*( 5.11194640E-04
      *+T*( 5.26442100E-08+T*( -3.49099730E-11+T*( 3.69453450E-15))))))
    H 1=1.9872*( -8.77380420E+02+T*( 3.10019010E+00
      *+T*( 5.11194640E-04/2.0+T*( 5.26442100E-08/3.0
      *+T*( -3.49099730E-11/4.0+T*( 3.69453450E-15/5.0))))))
    C 2=1.9872*( 2.89631940E+00+T*( 1.51548660E-03
      *+T*( -5.7235270E-07+T*( 9.98073930E-11+T*( -6.52235550E-15))))))
    H 2=1.9872*( -9.05861840E+02+T*( 2.89631940E+00
      *+T*( 1.51548660E-03/2.0+T*( -5.7235270E-07/3.0
      *+T*( 9.98073930E-11/4.0+T*( -6.52235550E-15/5.0))))))
    3000 CONTINUE
  3000 C SPECIFIC HEATS AND SPECIFIC ENTHALPIES.
    C(IST+ 1)=C I/ 2.00
    H(IST+ 1)=H I/ 2.00
    C(IST+ 2)=C 2/ 28.00
    H(IST+ 2)=H 2/ 28.00
  125 CONTINUE
  C VISCOSITY FROM WARNATZ ST PAR.

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FTN 4.8+498

SUBROUTINE F 76/76 OPT=1 ROUNDO=+*/ TRACE

```

60      C LEAST SQUARES FIT, T=300,2000.
        C THERMAL CONDUCTIVITIES FROM WARNATZ ST PAR.
        C LEAST SQUARES FIT, T=300,2000.
        C V 1= 2.188700E-06*(T** 6.502900E-01)
        C V 2= 4.266700E-06*(T** 6.613600E-01)
        C RL 1= 6.357900E-06*(T** 7.383300E-01)
        C RL 2= 6.407700E-07*(T** 7.999400E-01)
65      C BINARY DIFFUSION COEFFICIENTS FROM WARNATZ ST PAR.
        C LEAST SQUARES FIT, T=300,2000.
        C PRESS = 1.00
        D 1 1= 1.119300E-04*(T** 1.661400E+00)
        D 1 2= 5.951700E-05*(T** 1.663800E+00)
        D 2 2= 1.537400E-05*(T** 1.672900E+00)
70      C SPACE DERIVATIVES.
        YS=Y 3
        X 1=Y 1/Y5
        X 2=Y 2/Y5
        U 1=U( 1)
        DU 1=UPH( 1)
        DUU 1=UPH2( 1)
        U 2=1.0-U 1
        DU 2=-DU 1
        DUU 2=-DUU 1
        DY 1=DU 1/ 2.00
        DY 2=DU 2/ 28.00
        DYS=+DY 1+DY 2
80      C TPN = 1.0000E+03      PHN = 5.0000E-05      TMN = 1.0000E-03
        DT=UPH(NPDE)* 1.0000E+03
        DRH=- 1.2187690433E-02*(DT/T+DYS/YS)/(T*YS)
        DYS=DYS/(YS*YS)
        DX 1=DY 1/YS-Y 1*DYSY
        DL 1= 4.694228307000E-06*(T**(-2.616700E-01))*DT
        RLZ 1= 8.155096200000E-06*(T**(-6.502900E-01))
        DLZ 1= 5.303177507898E-06*(T**(-3.497100E-01))*DT
        DD 1 1= 1.859605020000E-04*(T**(-6.614000E-01))*DT
        VV 1= 4.568922191255E+05*(T**(-6.502900E-01))
        DVV 1= -2.971124411751E+05*(T**(-1.650290E+00))*DT
        XXSV 1=X 1*X 1*VV 1
        DXXSV 1=2.0*X 1*DX 1*VV 1+X 1*X 1*DVV 1
        DX 2=DY 2/YS-Y 2*DYSY
        DL 2= 5.125903692000E-07*(T**(-2.000400E-01))*DT
        RLZ 2= 1.13551728571E-06*(T**(-6.613600E-01))
        DLZ 2= 7.510084912080E-07*(T**(-3.386400E-01))*DT
        DD 2 2= 2.571916460000E-05*(T**(-6.729000E-01))*DT
        VV 2= 2.343731689596E+05*(T**(-6.613600E-01))
        DVV 2= -1.550050390231E+05*(T**(-1.661360E+00))*DT
        XXSV 2=X 2*X 2*VV 2
        DXXSV 2=2.0*X 2*DX 2*VV 2+X 2*X 2*DVV 2
        VD 1 2= 1.680192213989E+04*(T**(-1.663800E+00))
        DVD 1 2= -2.795503805635E+04*(T**(-2.663800E+00))*DT
        XXSD 1 2=X 1*X 2*VD 1 2
        DXXSD 1 2=DX 1*X 2*VD 1 2+X 1*DX 2*VD 1 2+X 1*X 2*DVD 1 2
        XXTSD 1 2=XXSD 1 2*1
        DATSD 1 2=DXSD 1 2*T+XXSD 1 2*1
        C SPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA.
        CM(IC)=+C(IST+ 1)*U 1+C(IST+ 2)*U 2
        C THERMAL CONDUCTIVITY OF THE MIXTURE.

```



```
115 C HIRSHFELDER METHOD FOR MDNATDMICS.
C P. 37A, TOULDUKLEN, LILEY, AND SAXENA.
C NOTE IN THE FORMULA, LAMBDA MUST BE IN THE SAME UNITS AS D*P/T.
C LAMBDA=15*PI*VISC/(4*PI)*R, WHERE R=B2.05 CM**3-ATM/MOLE-K.
C TO CONVERT LAMBDA BACK TO CAL/CM-SEC-K, MULTIPLY BY 1.9872/82.05.
120 TASTLJ=T*( 9.055700E-03)
TASTLJ=T*( -1.022500E-02)
DIATL= 9.055700E-03*DIAT**(-9.909443E-01)
DTBST= -1.022500E-02*DT**(-1.010225E+00)
CNST= 5.475555555555555E-01- 1.407397773742E-01*
* TASTLJ- 1.670532689818E-01*TASTLJ
DCNST=- 1.407397773742E-01*DTBST- 1.670532689818E-01*DIATL
Z( 1, 2)=CNST*XTSD 1 2
DZ 1S 2=CNST*DXTSO 1 2+DCNST*XTSD 1 2
Z( 2, 1)=Z( 1, 2)
DZ 2S 1=DZ 1S 2
CNST=- 3.505777777777777E+00+ 1.970356883238E+00*
* TASTLJ- 1.670532689818E-01*TASTLJ
DCNST= 1.970356883238E+00*DTBST- 1.670532689818E-01*DIATL
T 2=-XTSD 1 2*CNST
DT 2=-DXTSO 1 2*CNST-XTSD 1 2*DCNST
Z( 1, 1)= -2.600040625635E-02*XXSV 1-
* ( +T 2)
DZ 1S 1= -2.600040625635E-02*DXXSV 1-
* ( +DT 2)
CNST=- 4.199111111111111E+00+ 1.005284124101E-02*
* TASTLJ- 1.670532689818E-01*TASTLJ
DCNST= 1.005284124101E-02*DTBST- 1.670532689818E-01*DIATL
T 1=-XTSD 1 2*CNST
DT 1=-DXTSO 1 2*CNST-XTSD 1 2*DCNST
Z( 2, 2)= -3.640056875889E-01*XXSV 2-
* ( +T 1)
DZ 2S 2= -3.640056875889E-01*DXXSV 2-
* ( +DT 1)
V( 1)=X 1
V( 2)=X 2
CALL DEC( 2,20,Z,IPS,IER)
CALL SCL( 2,20,Z,V,IPS)
RLM= -9.687751E-02*( +X 1*V( 1) +X 2*V( 2))
DV( 1)=DX 1-DZ 1S 1*V( 1)-DZ 1S 2*V( 2)
DV( 2)=DX 2-DZ 2S 1*V( 1)-DZ 2S 2*V( 2)
CALL SCL( 2,20,Z,DV,IPS)
DRLM= -9.687751E-02*( +X 1*DV( 1)+DX 1*V( 1) +
* X 2*DV( 2)+DX 2*V( 2))
SUM=+X 2*VD 1 2
DSUM=+DX 2*VD 1 2+X 2*DVD 1 2
B=1.0+D 1 1*SUM/X 1
DH=DD 1 1*SUM/X 1+D 1 1*DSUM/X 1-D 1 1*SUM*DX 1/(X 1*X 1)
RLM=RLM+(RL 1-RLZ 1)/H
DRLM=DRLM+(DL 1-DLZ 1)/H-(RL 1-RLZ 1)*DH/(B*B)
SUM=+X 1*VD 1 2+X 3*VD 2 3
DSUM=+DX 1*VD 1 2+X 1*DVD 1 2+X 3*VD 2 3
H=1.0+D 2 2*SUM/X 2
DH=DD 2 2*SUM/X 2+D 2 2*DSUM/X 2-D 2 2*SUM*DX 2/(X 2*X 2)
RLM=RLM+(RL 2-RLZ 2)/H
DRLM=DRLM+(DL 2-DLZ 2)/H-(RL 2-RLZ 2)*DH/(B*B)
SUM=+X 1*VD 1 2
```

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SUBROUTINE F 76/76 OPT=1 ROUNO=+--*/ TRACE

```

175      USUM=DX 1*VD 1 2*X 1*DVD 1 2
      B=1.0+D 2 2*SUM/X 2
      DB=DD 2 2*SUM/X 2+D 2 2*DSUM/X 2-D 2 2*SUM*DX 2/(X 2*X 2)
      RLM=RLM+(RL 2-RLZ 2)/B
      DRLM=DRLM+(DL 2-DLZ 2)/B-(RL 2-RLZ 2)*DH/(B*B)
      RMLM(IC)=RH*RLM
      DRMLM(IC)=RH*DRLM+DRH*RLM
      C SOLVE FOR UV.
      V( 2)=0.0
      V( 1)=DX 1*RH/ 5.0000E-05
      Z( 2, 1)=U 1
      DZ 25 1=DU 1
      Z( 2, 2)=U 2
      DZ 25 2=DU 2
      Z( 1, 2)=XXSD 1 2
      DZ 15 2=DXSD 1 2
      Z( 1, 1)=-XXSD 1 2
      DZ 15 1=-DXSD 1 2
      Z( 2, 2)=-XXSD 1 2-XXSD 2 3
      DZ 25 2=-DXSD 1 2-DXSD 2 3
      CALL DEC( 2,20,Z,1PS,1ER)
      CALL SOL( 2,20,Z,V,1PS)
      UV 1=U 1*( 1)
      UV 2=U 2*( 2)
      RHUV(IST+ 1)=RH*UV 1
      RHUV(IST+ 2)=RH*UV 2
      C SPACE DER OF DENSITY TIMES UV.
      DDY 1=DDU 1/ 2.00
      DDY 2=DDU 2/ 28.00
      DDYS=DDY 1*DDY 2
      DYSYSQ=(DYS/YS)**2
      DDY 1=(DDY 1-2.0*DY 1*DYS/YS+2.0*Y 1*DYSYSQ-Y 1*DDYS/YS)/YS
      DDY 2=(DDY 2-2.0*DY 2*DYS/YS+2.0*Y 2*DYSYSQ-Y 2*DDYS/YS)/YS
      DV( 1)=(RH*DDX 1+DRH*DX 1)/ 5.0000E-05-DZ 15 1*( 1)-
      * DZ 15 2*( 2)
      DV( 2)=-DZ 25 1*( 1)-DZ 25 2*( 2)
      CALL SOL( 2,20,Z,DV,1PS)
      DUV 1=U 1*DV( 1)+DU 1*( 1)
      DUV 2=U 2*DV( 2)+DU 2*( 2)
      DRHUV(IST+ 1)=DRH*UV 1+RH*DUV 1
      DRHUV(IST+ 2)=DRH*UV 2+RH*DUV 2
      C FIND THE TIME DERIVATIVES.
      SP=ASP+BSP*TIME
      100 CONTINUE
      IF(KPDE.EQ.NPDE)GO TO 150
      RY= 1.000000000E-03*(KPDE)
      DY=- 2.000000000E+01*DRHUV(IST+KPDE)
      FVAL=SP*UPH(KPDE)+DY*RY
      RETURN
      150 CONTINUE
      TL= 4.000000000E+05*
      * (DRHLM(IC)*UPH(NPDE)+RMLM(IC)*UPH2(NPDE))
      TD=- 2.000000000E+01*UPH(NPDE)*C(IST+ 1)*RHUV(IST+ 1)+
      * C(IST+ 2)*RHUV(IST+ 2))
      TR=- 1.000000000E-06*( +P( 1)*H(IST+ 1) +H( 2)*H(IST+ 2))
      FVAL=SP*UPH(NPDE)+(TL+TR+TD)/CM(IC)
      RETURN

```

SUBROUTINE F
76/76 OPT=1 ROUNDED=+--*/ IPACE
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END
F 230

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FTN 4.8+498

PROGRAM LOADF 76/76 OPT=1 ROUND=**/ TRACE

```

1      PROGRAM LOADF (INPUT,OUTPUT,TAPE4=INPUT,TAPE6=OUTPUT,
2      * TAPE3,TAPE9,TAPE15)
3      C  LOADF CREATES THE SUBROUTINE F IN FLSC.
4      DIMENSION II(72)
5      DIMENSION III(44)
6      DIMENSION LB(25),W(25),AU(7,25),AL(7,25)
7      DIMENSION ALD(25),HLD(25),ABD(25,25),BBD(25,25)
8      DIMENSION AV(25),BV(25)
9      DIMENSION LBPR(25)
10     WRITE(3,1000)
11     FORMAT(1HC,2X,63HFOR THE COMPLETE TRANSPORT CASE, WE DO NOT WANT T
12     *HE U VALUES OR)
13     WRITE(3,1005)
14     FORMAT(1HC,2X,62HTHEIR FIRST DERIVATIVES TO BE ZERO. THIS CAN LEA
15     *D TO DIVISION)
16     WRITE(3,1010)
17     FORMAT(1HC,2X,8HBY ZERO.)
18     WRITE(3,1012)
19     FORMAT(6X,14HDO 5 K=1,NPDEM)
20     WRITE(3,1014)
21     FORMAT(6X,32HF(ABS(U(K)).LT.SMALL)U(K)=SMALL)
22     WRITE(3,1016)
23     FORMAT(1X,1H5,4X,36HF(ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL)
24     READ(5,12)NLINE
25     C  NLINE IS THE NUMBER OF COMMENT LINES TO BE READ AND PRINTED.
26     DO 20 K=1,NLINE
27     READ(5,22)II
28     WRITE(3,22)II
29     CONTINUE
30     FORMAT(72A1)
31     FORMAT(/1X,72A1/)
32     READ(5,12)NSPC
33     NM=NSPC-1
34     LBM=1H-
35     LBU=2HU(
36     LBP=1H)
37     WRITE(3,1020)((LHM,LHU,K,LBP),K=1,NM)
38     FORMAT(6X,6HYN=1,0,8(A1,A2,I2,A1),A1,2(/5X,IH*,1X,
39     * 8(A2,I2,A1,A1)) )
40     WRITE(3,1025)
41     FORMAT(6X,33HCALL RT(U,YN,R,NPUE,KPDE,IC,KSKR) )
42     WRITE(3,18)NSPC
43     FORMAT(6X,4HIST=,I2,7H*(IC-I) )
44     DO 30 K=1,NSPC
45     READ(5,32)LB(K),W(K)
46     WRITE(6,34)K,LB(K),W(K)
47     READ(15,36)(AU(L,K),L=1,5),(III(L),L=1,5)
48     WRITE(6,36)(AU(L,K),L=1,5),(III(L),L=1,5)
49     READ(15,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(III(L),L=1,5)
50     WRITE(6,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(III(L),L=1,5)
51     READ(15,37)(AL(L,K),L=4,7),(III(L),L=1,20)
52     WRITE(6,37)(AL(L,K),L=4,7),(III(L),L=1,20)
53     CONTINUE
54     FORMAT(A5,7F7,0)
55     FORMAT(/2X,I4,4X,A15,4X,F8,2/)
56     FORMAT(5F15,8,5A1)
57
58

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37  FORMAT(4E15.8,20A1)
60  READ(5,232)TPN,PHN,1MN
232  FORMAT(1P3E12.4)
27  WRITE(3,27)
27  FORMAT(6X,22HIF(KSKT.GT.1)GO TO 100)
28  WRITE(3,28)
28  FORMAT(6X,22HIF(KSKK.GT.1)GO TO 125 )
65  READ(5,12)NLINE
    DO 40 K=1,NLINE
    READ(5,22)II
    WRITE(3,22)II
40  CONTINUE
70  C *****
    C ENTHALPIES AND HEAT CAPACITIES.
    C *****
42  WRITE(3,42)
    FORMAT(6X,24HIF(T.GT.1000.)GO TO 2000)
75  DO 50 K=1,NSPC
    WRITE(3,52)K,AL(1,K),AL(2,K)
    WRITE(3,54) (AL(L,K),L=3,5)
    WRITE(3,62)K,AL(6,K),AL(1,K)
    WRITE(3,64)AL(2,K),AL(3,K)
    WRITE(3,66)AL(4,K),AL(5,K)
80  CONTINUE
50  FORMAT(6X,1HC,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
52  FORMAT(5X,1H*,1X,3(4H+T*(,1PE16.8),5H))))))
54  WRITE(3,56)
56  FORMAT(6X,10HG TO 3000)
85  WRITE(3,58)
58  FORMAT(4H2000,2X,8HCONTINUE)
    DO 60 K=1,NSPC
    WRITE(3,52)K,AU(1,K),AU(2,K)
    WRITE(3,54) (AU(L,K),L=3,5)
    WRITE(3,62)K,AU(6,K),AU(1,K)
    WRITE(3,64)AU(2,K),AU(3,K)
    WRITE(3,66)AU(4,K),AU(5,K)
90  CONTINUE
60  FORMAT(6X,1HH,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
62  FORMAT(5X,1H*,1X,4H+T*(,1PE16.8,4H+T*(,1PE16.8,4H+T*(,1PE16.8)
64  FORMAT(5X,1H*,1X,4H+T*(,1PE16.8,4H+T*(,1PE16.8,4H+T*(,1PE16.8,
66  * 4H/5.0,6H))))))
    WRITE(3,68)
100  FORMAT(4H3000,2X,8HCONTINUE)
    WRITE(3,134)
134  FORMAT(1HC,2X,39HSPECIFIC HEATS AND SPECIFIC ENTHALPIES. )
    DO 140 K=1,NSPC
    WRITE(3,142)K,K,W(K)
    WRITE(3,144)K,K,W(K)
105  CONTINUE
140  FORMAT(6X,6HC(IST,12,3H)=C,12,1H/,F6.2)
142  FORMAT(6X,6HH(IST,12,3H)=H,12,1H/,F6.2)
144  WRITE(3,146)
146  FORMAT(1X,3HI25,2X,8HCONTINUE)
110  C *****
    C THERMAL CONDUCTIVITIES AND BINARY DIFFUSION COEFFICIENTS.
    C READ IN VISCOSITY, THERMAL CONDUCTIVITY, AND BINARY DIFFUSION
    C COEFFICIENTS FROM A FILE CREATED BY VALUES, CY=6.

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04/15/80 14.46.06

FTN 4.8+498

PROGRAM LOADF 76/76 OPT=1 ROUNO=**/ TRACE

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115 C *****
116 READ(5,12)NLINE
117 DO 72 K=1,NLINE
118 READ(5,22)I1
119 WRITE(6,22)I1
120 72 WRITE(3,22)I1
121 FORMAT(1HC,5X,IHV,12,IH=,IPEI4.6,5H*(T**,IPEI4.6,IH) )
122 79 READ(5,12)NLINE
123 DO 70 K=1,NLINE
124 READ(5,22)I1
125 WRITE(3,22)I1
126 WRITE(6,22)I1
127 CONTINUE
128 DO 80 K=1,NSPC
129 READ(9,82)AV(K),HV(K),I11
130 WRITE(6,84)K,LR(K),AV(K),BV(K),I11
131 READ(9,82)ALD(K),BLD(K),I11
132 WRITE(6,84)K,LB(K),ALD(K),BLD(K),I11
133 CONTINUE
134 FORMAT(IP2EI4.6,44A1)
135 82 FFORMAT(12X,I4,4X,A4,4X,IP2EI4.6,44A1/)
136 84 DO 78 K=1,NSPC
137 WRITE(3,79)K,AV(K),BV(K)
138 CONTINUE
139 DO 90 K=1,NSPC
140 WRITE(3,92)K,ALD(K),BLD(K)
141 CONTINUE
142 90 FFORMAT(6X,2HRL,12,IH=,IPEI4.6,5H*(T**,IPEI4.6,IH) )
143 92 READ(5,12)NLINE
144 DO 100 K=1,NLINE
145 READ(5,22)I1
146 WRITE(3,22)I1
147 WRITE(6,22)I1
148 CONTINUE
149 NM=NSPC-1
150 DO 110 I=1,NSPC
151 DO 110 J=1,NSPC
152 READ(9,82)ABD(I,J),HBD(I,J),I11
153 WRITE(6,112)I,J,LR(I),LB(J),ABD(I,J),HBD(I,J),I11
154 CONTINUE
155 FFORMAT(12X,I4,4X,I4,4X,A4,4X,A4,4X,IP2EI4.6,44A1/)
156 112 FFORMAT(5,114)PRESS
157 FFORMAT(F6.0)
158 114 WRITE(3,116)PRESS
159 FFORMAT(1HC,2X,7HPRESS =,F6.2)
160 116 DO 120 I=1,NM
161 1P=I+1
162 DO 120 J=1P,NSPC
163 ABD(I,J)=ABD(I,J)/PRESS
164 WRITE(3,122)I,J,ABD(I,J),HBD(I,J)
165 CONTINUE
166 120 FFORMAT(1HC,5X,IHV,12,IH=,IPEI4.6,5H*(T**,IPEI4.6,IH) )
167 122 C *****
168 C SPACE DERIVATIVES.
169 C *****
170 LbPL=1H+
WRITE(3,144)

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148  FORMAT(1HC,2X,18HSPACE DERIVATIVES.)
      NS=NSPC*1
      WRITE(3,149)NS
149  FORMAT(6X,4HYS=Y,I2)
      DO 150 K=1,NSPC
      WRITE(3,152)K,K
150  CONTINUE
152  FORMAT(6X,1HX,I2,2H=Y,I2,3H/YS)
      DO 160 K=1,NM
      WRITE(3,162)K,K
      WRITE(3,164)K,K
      WRITE(3,166)K,K
160  CONTINUE
162  FORMAT(6X,1HU,I2,3H=U(I2,1H))
164  FORMAT(6X,2HOU,I2,5H=UPH(I2,1H))
166  FORMAT(6X,3HODU,I2,6H=UPH2(I2,1H))
      LBU=1HU
172  WRITE(3,172)NSPC,((LBM,LBU,K)*K=1,NM)
      * 8(A1,I2,A1)) )
      LBDU=2HOU
174  WRITE(3,174)NSPC,((LBM,LBDU,K)*K=1,NM)
      FORMAT(6X,2HOU,I2,1H=8(A1,A2,I2),A1,2(/5X,1H*,1X,
      * 8(A2,I2,A1)) )
      LBDU=3HODU
176  WRITE(3,176)NSPC,((LBM,LBDU,K)*K=1,NM)
      FORMAT(6X,3HODU,I2,1H=8(A1,A3,I2),A1,2(/5X,1H*,1X,
      * 8(A3,I2,A1)) )
      DO 180 K=1,NSPC
      WRITE(3,182)K,K,W(K)
180  CONTINUE
182  FORMAT(6X,2HXY,I2,3H=DU,I2,1H/F6.2)
      LBDY=2HXY
186  WRITE(3,186)((LBP,LBDY,K)*K=1,NSPC)
      FORMAT(6X,4HYS=8(A1,A2,I2),A1,2(/5X,1H*,1X,8(A2,I2,A1)) )
      PSR=PRESS/82.05
      WRITE(3,234)TPN,PHN,TMN
      WRITE(6,234)TPN,PHN,TMN
234  FORMAT(1HC,2X,5HTPN =,1PE12.4,6X,5HPHN =,1PE12.4,6X,
      * 5HTMN =,1PE12.4)
      WRITE(3,226)TPN
226  FORMAT(6X,13HDT=UPH(NPDE)*,1PE12.4)
      WRITE(3,242)PSR
242  FORMAT(6X,5HDRH=,1PE18.10,21H*(DT/T*OYS/YS)/(T*YS))
      DO 815 I=1,NSPC
      DO 815 J=1,NSPC
      IF(1.E0.J)GO TO 815
      A=1.0/ABD(I,J)
      B=-880(I,J)
      WRITE(3,818)I,J,A,B
815  CONTINUE
818  FORMAT(6X,2HVD,I2,1H=,1PE16.8,6X,(T**(.1PE16.8,2H)) )
      DO 820 I=1,NSPC
      DO 820 J=1,NSPC
      IF(1.E0.J)GO TO 820
      A=1.0/ABD(I,J)
      H=-880(I,J)

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FTN 4.8+498

76/76 OPT=I ROUND=+*/ TRACE

PROGRAM LOADF

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230      A=A*B
      H=B-I.0
      WRITE(3,822)I,J,A,H
      CONTINUE
820      FORMAT(6X,3H0V0,2I2,1H=,1PEI6.8,6H*(T**(.1PEI6.8,5H))=DT)
822      C *****
      C SPECIFIC HEAT OF THE MIXTURE.
      C *****
235      WRITE(3,124)
124      FORMAT(1HC,2X,44HSPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA. )
      LHC=6HC(1ST+
      LBU=3H)*U
240      WRITE(3,132)((LBP,LHC,K,LHU,K),K=I,NSPC)
132      FORMAT(6X,7HCM(1C)=,4(AI,A6,I2,AJ,I2),AI,
      * 4(/5X,1H=,IX,4(A6,I2,A3,I2,AI)) )
      C *****
      C THERMAL CONDUCTIVITY OF THE MIXTURE.
      C *****
245      WRITE(3,272)
272      FORMAT(1HC,2X,36HTHERMAL CONDUCTIVITY OF THE MIXTURE.)
274      FORMAT(1HC,2X,24HMASON AND SAXENA METHOD. )
      WRITE(3,252)
252      FORMAT(1HC,2X,55HLMIX=SUM(I) (L 1/(1.0+(SUM(J)P I J*X J)/X I))
      *I,NE,J )
      WRITE(3,254)
254      FORMAT(1HC,2X,69HP I J=(1.065/SUMT(8.0*(1.0+M I/M J)))*(1.0+SQRT((
      *M J*V I)/(M I*V J))* )
      WRITE(3,255)
255      FORMAT(1HC,2X,23HSQRT(SQRT(M I/M J))**2 )
      WRITE(3,256)
256      FORMAT(1HC,2X,45HP 1 J IS A FUNCTION OF T AND CONSTANTS. )
      WRITE(3,258)
258      FORMAT(1HC,2X,45HFOR CONVENIENCE, P I J = A*(1.0+B*T**C)**2 )
      DO 275 I=1,NSPC
      DO 275 J=1,NSPC
      IF(1.EQ.J)GO TO 275
      A=1.065/(2.0*SQRT(2.0*(1.0+W(I)/W(J))))
      B=SQRT(AV(I)/AV(J))*SQRT(SQRT(W(J)/W(I)))
      C=(BV(I)-BV(J))/2.0
      WRITE(3,271)B,C
271      FORMAT(6X,8HBTIC=1.0,1PE20.10,5H*T**(.1PE20.10,1H) )
      WRITE(3,278)I,J,A
      D=2.0*A*B*C
      E=C-I.0
      WRITE(3,279)I,J,D,E
275      CONTINUE
278      FORMAT(6X,1HP,12,1HS,I2,1H=,1PE20.10,7H*BTIC**2)
279      FORMAT(6X,2HDP,12,1HS,I2,1H=,1PE20.10,5H*T**(.1PE20.10,8H)*BTIC*U)
      LBP=1HP
      LHX=2H*X
      LHP=1HS
      K=1
      WRITE(3,282)K,((LHP,LHPS,K,LBSP,J,LHX,J),J=2,NSPC)
282      FORMAT(6X,4HSUMP,I2,1H=,5(2A1,I,4A1,I2,A2,I2),A1,
      * 3(/5X,1H=,IX,5(A1,I2,A1,I2,A2,I2,A1)) )
      IF((NM.EQ.1)GO TO 284
284      LOADF

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290      DO 280 K=2,NM
          KM=K-1
          KP=K+1
          WRITE(3,282)K,((LBPL,LBPS,K,LBSP,J,LBX,J),J=1,KM),
          * ((LBPL,LBPS,K,LBSP,J,LBX,J),J=KP,NSPC)
          CONTINUE
280      CONTINUE
284      K=NSPC
          WRITE(3,282)K,((LBPL,LBPS,K,LBSP,J,LBX,J),J=1,NM)
          DO 285 K=1,NSPC
          WRITE(3,288)K,K,K
          CONTINUE
285      CONTINUE
288      FORMAT(6X,1H8,I2,9H=1.0+SUMP,I2,2H/X,I2)
          LBRL=2HRL
          LBSB=2H/B
          WRITE(3,292) ((LBPL,LBRL,K,LBSB,K),K=1,NSPC)
          FORMAT(6X,4HRLM=,6(A1,A2,I2,A2,I2),A1,3(/5X,1H*,1X,
292      * 6(A2,I2,A2,I2,A1)) )
          WRITE(3,306)
          FORMAT(6X,15HRLM(IC)=RH*RLM)
          C *****
          C DERIVATIVE OF THE THERMAL CONDUCTIVITY OF THE MIXTURE.
          C *****
          WRITE(3,312)
          FORMAT(1HC,2X,40HSPACE DER OF DENSITY TIMES THERMAL COND.,)
          DO 740 K=1,NSPC
          A=ALD(K)*BLD(K)
          B=BLD(K)-1.0
          WRITE(3,742)K,A,B
          CONTINUE
          FORMAT(6X,3HDL,I2,1H=,1PE14.6,6H*(T**(:,1PE14.6,5H))*DT )
          WRITE(3,745)
          FORMAT(6X,16HDYSY=DYS/(YS*YS) )
          DO 750 K=1,NSPC
          WRITE(3,752)K,K,K
          CONTINUE
          FORMAT(6X,2HDY,I2,3H=DY,I2,5H/Y5-Y,I2,5H*DY5Y )
          LBX=2H*X
          LBPS=1HP
          LBUP=2HDP
          K=1
          WRITE(3,762)K,((LBPL,LBUP,K,LBSP,J,LBX,J,LBPL,LBPS,K,LBSP,J,
          * LBX,J),J=2,NSPC)
          IF (NM.EQ.1)GO TO 761
          DO 760 K=2,NM
          KM=K-1
          KP=K+1
          WRITE(3,762)K,((LBPL,LBUP,K,LBSP,J,LBX,J,LBPL,LBPS,K,LBSP,J,LBX,
          * J),J=1,KM),((LBPL,LBUP,K,LBSP,J,LBX,J,LBPL,LBPS,K,LBSP,J,LBX,J),
          * J=KP,NM)
          CONTINUE
          CONTINUE
          K=NSPC
          WRITE(3,762)K,((LBPL,LBUP,K,LBSP,J,LBX,J,LBPL,LBPS,K,LBSP,
          * J,LBX,J),J=1,NM)
          FORMAT(6X,5HDSUMP,I2,1H=,2(A1,I2,A1,I2,A2,I2,2A1,I2,A1,I2,A3,
762

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345      * I2,A1,9(/5X,IH*,IX*2(A2,I2,A1,I2,A2,I2,2A1,I2,A1,I2,A3,I2,A1)) ) MAIN
      DO 765 K=1,NSPC
      WRITE(3,76R)K,K,K,K,K,K
      CONTINUE
      FORMAT(6X,2HDR,I2,IH=,6H(OSUMP,I2,5H-SUMP,I2,3H*OX,I2,2H/X,I2,
346      * 3H)/X,I2)
      DO 770 K=1,NSPC
      WRITE(3,772)K,K,K,K,K,K
      CONTINUE
      FORMAT(6X,IHT,I2,5H=(ORL,I2,3H-RL,I2,3H*OB,I2,2H/B,I2,3H)/B,I2)
      LBT=IHT
      WRITE(3,776)((LBPL,LHT,K),K=1,NSPC)
      FORMAT(6X,5HORLM=,10(2A1,I2),A1,/5X,IH*,IX,10(A1,I2,A1) )
      WRITE(3,778)
      FORMAT(6X,25HORLM(IC)=ORH*RLM+K*H*DRLM)
      C *****
      C SOLVE FOR UV.
      C ZERO ORDER BORIS AND OHAN APPROXIMATION.
      C *****
      WRITE(3,400)
      FORMAT(1HC,2X,I3HSOLVE FOR UV.)
      LBX=IHX
      LBVD=3H*VD
      K=1
      WRITE(3,402)K,((LBPL,LBX,J,LBVD,K,J),J=2,NSPC)
      FORMAT(6X,3HSUM,I2,IH=,5(2A1,I2,3,2I2),A1,3(/5X,IH*,IX,
347      * 5(A1,I2,A3,2I2,A1)) )
      IF(NM.EQ.1)GO TO 412
      DO 410 K=2,NM
      KM=K-1
      KP=K+1
      WRITE(3,402)K,((LBPL,LBX,J,LBVD,J,K),J=1,KM),((LBPL,LBX,J,
348      * LBVD,K,J),J=KP,NSPC)
      CONTINUE
      CONTINUE
      K=NSPC
      WRITE(3,402)K,((LBPL,LBX,J,LBVD,J,K),J=1,NM)
      DO 415 K=1,NSPC
      WRITE(3,418)K,K,K,PHN
      CONTINUE
      FORMAT(6X,IHB,I2,2H=X,I2,4H*SUM,I2,IH*,1PLEI2.4)
      DO 420 K=1,NSPC
      WRITE(3,422)K,K
      CONTINUE
      FORMAT(6X,IHT,I2,IH=-RH*(1.0-U,I2,IH) )
      DO 425 K=1,NSPC
      WRITE(3,428)K,K,K
      CONTINUE
      FORMAT(6X,3HFAC,I2,2H=T,I2,2H/B,I2)
      DO 465 K=1,NSPC
      WRITE(3,468)K,K,K
      CONTINUE
      FORMAT(6X,IHV,I2,4H=FAC,I2,3H*UX,I2)
      DO 470 K=1,NSPC
      WRITE(3,472)K,K,K
      CONTINUE
      FORMAT(6X,2HUV,I2,2H=U,I2,2H*V,I2)

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400      LBUV=2HUV
      WRITE(3,476)((LBML, LBUV,K),K=1,NSPC)
476      FORMAT(6X,3HDV=,8(A1,A2,12),A1,2(/5X,1H*,1X,8(A2,12,A1)))
      DO 480 K=1,NSPC
      WRITE(3,482)K,K,K
      CONTINUE
480      FORMAT(6X,2HUV,12,3H=UV,12,5H+UV*U,12)
482      DO 485 K=1,NSPC
      WRITE(3,488)K,K
      CONTINUE
485      FORMAT(6X,9HRHUV(1ST,12,7H)=RH*UV,12)
488      C *****
      C SOLVE FOR THE SPACE DERIVATIVE OF UV.
      C *****
      WRITE(3,522)
522      FORMAT(1HC,2X,30HSPACE DER OF DENSITY TIMES UV.)
      DO 500 K=1,NSPC
      WRITE(3,502)K,K,K
      CONTINUE
500      FORMAT(6X,3HDDY,12,4H=DDU,12,1H/,F6.2)
502      LBDDY=3HDDY
      WRITE(3,506)((LBPL, LBDDY,K),K=1,NSPC)
506      FORMAT(6X,5HDDYS=,8(A1,A3,12),A1,2(/5X,1H*,1X,8(A3,12,A1)))
      WRITE(3,510)
510      FORMAT(6X,18HDYSYSO=(DYS/Y)*2)
      DO 515 K=1,NSPC
      WRITE(3,518)K,K,K,K
      CONTINUE
515      FORMAT(6X,3HDDX,12,5H=(DDY,12,7H=2.0*DY,12,13H*DY/YS+2.0*Y,
518      * 12,9H*DYYSO-Y,12,12H*DDYS/YS)/YS)
      LBDX=2HDX
      LBVD=3H*VD
      LBX=1HX
      LBVDV=4H*DVD
      K=1
      WRITE(3,532)K,((LBPL, LBDX,J, LBVD,K,J), LBPL, LBX,J, LBDDV,K,J),
      * J=2,NSPC)
532      FORMAT(6X,4HDSUM,12,1H=,2(A1,A2,12,A3,212,2A1,12,A4,212),A1,
      * 9(/5X,1H*,1X,2(A2,12,A3,212,2A1,12,A4,212,A1)))
      IF(NM.EQ.1)GO TO 541
      DO 535 K=2,NM
      KN=K-1
      KP=K+1
      WRITE(3,532)K,((LBPL, LBDX,J, LBVD,K,J), LBPL, LBX,J, LBDDV,K,J),
      * J=1,KM),((LBPL, LBDX,J, LBVD,K,J), LBPL, LBX,J, LBDDV,K,J), J=KP,NSPC)
535      CONTINUE
      K=NSPC
      WRITE(3,532)K,((LBPL, LBDX,J, LBVD,K,J), LBPL, LBX,J, LBDDV,K,J), J=1,NM)
      DO 540 K=1,NSPC
      WRITE(3,542)K,K,K,K
      CONTINUE
540      CONTINUE
541      FORMAT(6X,2HDS,12,1H=,1PE12.4,4H*(DX,12,4H*SUM,12,2H+X,12,
542      * 5H*DSUM,12,1H) )
      DO 545 K=1,NSPC
      WRITE(3,548)K,K,K
      CONTINUE
545      CONTINUE

```

```

548  FORMAT(6X,2HDT,I2,I2H=-0RH*(1.0-U,I2,7H)+RH*DU,I2)
DO 550 K=1,NSPC
  WRITE(3,552)(K,L=1,7)
550  CONTINUE
552  * 3H/(B,I2,2H*B,I2,1H)
      DO 590 K=1,NSPC
        WRITE(3,592)K,K,K,K,K
590  CONTINUE
592  FORMAT(6X,2HUV,I2,5H=DFAC,I2,3H*UX,I2,4H+FAC,I2,4H*OXX,I2)
      DO 595 K=1,NSPC
        WRITE(3,598)K,K,K,K,K
595  CONTINUE
598  FORMAT(6X,3HUV,I2,3H=DU,I2,2H*V,I2,2H+U,I2,3H*DV,I2)
      LDUV=3HUV
802  WRITE(3,802)((LHM,LBDUV,K),K=1,NSPC)
      FORMAT(6X,4HDDV=,8(A1,A3,I2),A1,2(/5X,IH*,IX,8(A3,I2,A1)))
      DO 805 K=1,NSPC
        WRITE(3,808)K,K,K,K,K
805  CONTINUE
808  FORMAT(6X,3HUV,I2,4H=DUV,I2,6H+UV*DU,I2,6H+DDV*U,I2)
      DO 810 K=1,NSPC
        WRITE(3,812)K,K,K
810  CONTINUE
812  FORMAT(6X,10HURUV(IST*,I2,8H)=URH*UV,I2,7H+RH*DUV,I2)
C *****
C  FIND THE TIME DERIVATIVES.
C *****
485  WRITE(3,612)
612  FORMAT(1HC,2X,26HFINO THE TIME DERIVATIVES.)
      WRITE(3,622)
622  FORMAT(6X,15HSP=ASP*8SP*TIME)
      TMSPH2=TMN/(PHN*PHN)
      WRITE(3,628)
628  FORMAT(1X,3H100,2X,8HCONTINUE)
      WRITE(3,632)
632  FORMAT(6X,25HIF(KPDE.EQ.NPDE)GO TO 150)
      WRITE(3,636)TMN
636  FORMAT(6X,3HRY=,IPEZU.10,8H*(KPDE) )
      TMSPH=TMN/PHN
      WRITE(3,638)TMSPH
638  FORMAT(6X,4HUY=,IPEZU.10,16H*URHUV(IST*+KPDE) )
      WRITE(3,642)
642  FORMAT(6X,23HFVAL=SP*UPH(KPDE)+UY*RY)
      WRITE(3,646)
646  FORMAT(6X,6HRETURN)
      WRITE(3,648)
648  FORMAT(1X,3H150,2X,8HCONTINUE)
      DO 650 K=1,NM
        WRITE(3,652)K,K
650  CONTINUE
652  FORMAT(6X,2HUU,I2,5H=UPH(,I2,1H) )
      K=NSPC
      LDUV=2HUU
      WRITE(3,656)K,((LBM,LDDU,J),J=1,NM)
656  FORMAT(6X,2HUU,I2,IH=,8(A1,A2,1/),A1,2(/5X,IH*,IX,8(A2,I2,A1)) )
      WRITE(3,662)TMSPH2

```

PROGRAM	LOADF	76/76	OPT=1	ROUND=+--*/	TRACE	FTN	4.8+498	04/15/80	14.46.06	PAGE	10
515	662	FORMAT(6X,3HTL=,1PE20.10,1H*)						MAIN	507		
		WRITE(3,664)						MAIN	508		
	664	FORMAT(5X,1H*,1X,41H(ORHLM(1C)*UPH(NPDE)+RHLM(1C)*UPH2(NPDE)))						MAIN	509		
		LBBL=1H						MAIN	510		
		LBC=6HC(1ST+						MAIN	511		
		LBRHUV=10H)*RHUV(1ST						MAIN	512		
520		WRITE(3,668)TMSPH,((LBBL,LBPL,LHC,K,LBRHUV,LBPL,K,LBP),K=1,						MAIN	513		
		* NSPC),LBP						MAIN	514		
	668	FORMAT(6X,4HID=-,1PE20.10,12H*UPH(NPDE))*((2A1,A6,12,A10,A1,12,						MAIN	515		
		* 3A1,10(/5X,1H*,1X,2(A6,12,A10,A1,12,3A1)))						MAIN	516		
		TMSHP=TMN/TPN						MAIN	517		
525		LBR=2HR(MAIN	518		
		LH=8H)*H(1ST+						MAIN	519		
		WRITE(3,672)TMSTP,((LBBL,LBPL,LHC,K,LBP),K=1,NSPC),LBP						MAIN	520		
	672	FORMAT(6X,4HTR=-,1PE20.10,2H*((2A1,A2,12,A8,12,A1),2A1,						MAIN	521		
		* 9(/5X,1H*,1X,2(A2,12,A8,12,3A1)))						MAIN	522		
		WRITE(3,676)						MAIN	523		
530	676	FORMAT(6X,3SHFVAL=SP*UPH(NPDE))*((TL+TR*TD)/CM(1C))						MAIN	524		
		STOP						MAIN	525		
		END						MAIN	526		

SCOPE 2 LOAD MAP

BLOCK	ADDRESS	LENGTH	FILE
LOADF	110	11104	LGO
/STP.END/	11214	1	SL-F-TNLI1
/FCL.C./	11215	30	SL-F-TNLI1
/Q8.10./	11245	144	SL-F-TNLI1
Q2NTRY=	11411	4	SL-F-TNLI1
COM10=	11415	10	SL-F-TNLI1
FECMSK=	11425	41	SL-F-TNLI1
FEIFST=	11466	3	SL-F-TNLI1
FLFLIN=	11471	156	SL-F-TNLI1
FLFIOUT=	11647	315	SL-F-TNLI1
FMTAP=	12164	377	SL-F-TNLI1
FORSYS=	12563	300	SL-F-TNLI1
FORUTL=	13063	45	SL-F-TNLI1
GETFIT=	13130	54	SL-F-TNLI1
IINCOM=	13204	144	SL-F-TNLI1
INPC=	13350	173	SL-F-TNLI1
KOOR=	13543	476	SL-F-TNLI1
KRAKER=	14241	454	SL-F-TNLI1
UUTC=	14715	155	SL-F-TNLI1
UUTCOM=	15072	204	SL-F-TNLI1
ERRCAP=	15276	317	SL-F-TNLI1
FERCAP=	15615	171	SL-F-TNLI1
EXP.MSG	16006	16	SL-F-TNLI1
ISORT	16024	6	SL-F-TNLI1
ISORT.	16032	32	SL-F-TNLI1
SYS:=	16064	1	SL-F-TNLI1
SYS:=	16065	65	SL-F-TNLI1

1	H2	2.00
---	----	------

H2	-.31001901E+01	.51119464E-03	.52644210E-07	-.34909973E-10	.36945345E-14
H2	-.87738042E+03	-.19629421E+01	.30574451E+01	.26765200E-02	-.58099162E-05
H2	.55210391E-08	-.18122739E-11	-.98890474E+03	-.22997056E+01	

2	2N	28.00
---	----	-------

28963194E+01	15154866E-02	5723277E-06	99807393E-10	65223555E-14
-90586184E+03	61615148E+01	36748261E+01	12081500E-02	23240102E-05
-63217595E-09	-22577253E-12	-10611588E+04	23580424E+01	

LEAST SQUARES FIT, $T=300,2000$.
THERMAL CONDUCTIVITIES FROM WARNATZ ST PAR.
LEAST SQUARES FIT, $T=300,2000$.

1	H2	2.188700E-06	6.502900E-01	H2	VISCOSITY.
---	----	--------------	--------------	----	------------

2 N2 4.266700E-06 6.613600E-01 192 VISCOSITY.

BINARY DIFFUSION COEFFICIENTS FROM WARNATZ ST PAR.
 LEAST SQUARES FIT, $T=300.2000$.

1	1	H2	H2	1.119300E-04	1.661400E+00	H2	H2	BINARY DIFFUSION.
1	2	H2	N2	5.951700E-05	1.663800E+00	H2	N2	BINARY DIFFUSION.
2	2	N2	N2	1.537400E-05	1.672900E+00	N2	N2	BINARY DIFFUSION.

TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03

04/15/80 14.46.29

FTN 4.8+498

76/76 OPT=1 ROUNO=-*/ THACE

SUBROUTINE F

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1  SUBROUTINE F(TIME,PH,U,UPH,UPH2,FVAL,NPDE,KPDE,IC,KSKT,KSKR)
2  DIMENSION U(NPDE),UPH(NPDE),UPH2(NPDE)
3  COMMON/TABAB/ASP,RSP,TPN,PHN,TMN,TMSPH,TMSTP,TPENT
4  COMMON/TARP/PRESS,PSK,NPDEM
5  COMMON/TARSM/SMALL
6  COMMON/TARAM/YAB,WAH
7  DIMENSION R(20)
8  DIMENSION C(1000),H(1000),RHLN(100),DRHLM(100),CM(100)
9  COMMON/TABCT/RL,CPMA,HO(20),R2D(20),R2DM(20)
10 COMMON/TABMF/RHUV(1000),DRHUV(1000)
11 COMMON/TABRY/T,RH,Y1,Y2,Y3,Y4,Y5,Y6,Y7,Y8,Y9,Y10
12 C AT EACH CALL THE TIME RATE OF CHANGE FOR ONE PDE IS RETURNED IN FVAL.
13 C FOR THE COMPLETE TRANSPORT CASE, WE DO NOT WANT THE U VALUES OR
14 C THEIR FIRST DERIVATIVES TO BE ZERO. THIS CAN LEAD TO DIVISION
15 C BY ZERO.
16 DO 5 K=1,NPDEM
17 IF (ABS(U(K)).LT.SMALL)U(K)=SMALL
18 IF (ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL
19 S TEST CASE. BINARY MIX OF H2 AND N2. TRANSPORT WARNATZ PAR.
20 C U = MASS FRACTIONS. Y = MASS FRACTIONS / MOLECULAR WEIGHTS.
21 YN=1.0-U( 1)
22 CALL RT(U,YN,R,NPDE,KPDE,IC,KSKR)
23 IST= 2*(IC-1)
24 IF(KSKT.GT.1)GO TO 100
25 IF(KSKR.GT.1)GO TO 125
26 C NTLS ENTHALPIES AND HEAT CAPACITIES.
27 IF(T.GT.1000.)GO TO 2000
28 C 1=1.9872*( 3.05744510E+00+T*( 2.67652000E-03
29 * +T*( -5.80991620E-06+T*( 5.52103910E-09+T*( -1.81227390E-12))))
30 H 1=1.9872*( -9.88904740E+02+T*( 3.05744510E+00
31 * +T*( 2.67652000E-03/2.0+T*( -5.80991620E-06/3.0
32 * +T*( 5.52103910E-09/4.0+T*( -1.81227390E-12/5.0))))))
33 C 2=1.9872*( 3.67482610E+00+T*( -1.20815000E-03
34 * +T*( 2.32401020E-06+T*( -6.32175590E-10+T*( -2.25772530E-13))))
35 H 2=1.9872*( -1.06115880E+03+T*( 3.67482610E+00
36 * +T*( -1.20815000E-03/2.0+T*( 2.32401020E-06/3.0
37 * +T*( -6.32175590E-10/4.0+T*( -2.25772530E-13/5.0))))))
38 GO TO 3000
39 2000 CONTINUE
40 C 1=1.9872*( 3.10019010E+00+T*( 5.11194640E-04
41 * +T*( 5.26442100E-08+T*( -3.49099730E-11+T*( 3.69453450E-15))))))
42 H 1=1.9872*( -8.77380420E+02+T*( 3.10019010E+00
43 * +T*( 5.11194640E-04/2.0+T*( 5.26442100E-08/3.0
44 * +T*( -3.49099730E-11/4.0+T*( 3.69453450E-15/5.0))))))
45 C 2=1.9872*( 2.89631940E+00+T*( 1.51548660E-03
46 * +T*( -5.72352770E-07+T*( 9.98073930E-11+T*( -6.52235550E-15))))))
47 H 2=1.9872*( -9.05861840E+02+T*( 2.89631940E+00
48 * +T*( 1.51548660E-03/2.0+T*( -5.72352770E-07/3.0
49 * +T*( 9.98073930E-11/4.0+T*( -6.52235550E-15/5.0))))))
50 3000 CONTINUE
51 C SPECIFIC HEATS AND SPECIFIC ENTHALPIES.
52 C(1ST+ 1)=C 1/ 2.00
53 H(1ST+ 1)=H 1/ 2.00
54 C(1ST+ 2)=C 2/ 24.00
55 H(1ST+ 2)=H 2/ 24.00
56 125 CONTINUE
57 C VISCOSITY FROM WARNATZ ST PAR.
58

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60 C LEAST SQUARES FIT, T=300.2000.
C THERMAL CONDUCTIVITIES FROM WARNATZ ST PAR.
C LEAST SQUARES FIT, T=300.2000.
C V 1= 2.188700E-06*(T** 6.502900E-01)
C V 2= 4.266700E-06*(T** 6.613600E-01)
C RL 1= 6.357900E-06*(T** 7.383300E-01)
C RL 2= 6.407700E-07*(T** 7.999600E-01)
65 C BINARY DIFFUSION COEFFICIENTS FROM WARNATZ ST PAR.
C LEAST SQUARES FIT, T=300.2000.
C PRESS = 1.00
C D 1 2= 5.951700E-05*(T** 1.663800E+00)
C SPACE DERIVATIVES.
70 YS=Y 3
X 1=Y 1/YS
X 2=Y 2/YS
U 1=U( 1)
DU 1=UPH( 1)
DUU 1=UPH2( 1)
U 2=1.0-U 1
DU 2=-DU 1
DUU 2=-DUU 1
DY 1=DU 1/ 2.00
DY 2=DU 2/ 28.00
DYS=+DY 1+DY 2
80 C TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03
DT=UPH(NPDE)* 1.0000E+03
DRH=- 1.2187690433E-02*(DT/T+DYS/YS)/(T*YS)
VD 1 2= 1.68019221E+04*(T**(-1.66380000E+00))
DU 1 2= -2.79550381E+04*(T**(-2.66380000E+00))*DT
85 C SPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA.
CM(IC)=C(IST+ 1)*U 1+C(1ST+ 2)*U 2
C THERMAL CONDUCTIVITY OF THE MIXTURE.
C MASON AND SAXENA METHOD.
90 C LMIX=SUM(I)/(L 1/(1.0+(SUM(J)P 1 J*X J)/X 1)) 1.NE.J
C P 1 J=(1.065/SQRT(8.0*(1.0+M 1/M J)))*(1.0+SQRT((M J*V 1)/(M 1*V J)))*
C SRT(SQRT(M 1/M J))**2
C P 1 J IS A FUNCTION OF T AND CONSTANTS.
C FOR CONVENIENCE, P 1 J = A*(1.0+B*T**C)**2
95 HTC=1.0+ 1.3854124113E+00*T**(-5.5350000000E-03)
P 1S 2= 3.6376675219E-01*HTC**2
UP 1S 2= -5.5789143943E-03*T**(-1.0055350000E+00)*HTC*DT
HTC=1.0+ 7.2180672836E-01*T**(-5.5350000000E-03)
P 2S 1= 9.7220753957E-02*HTC**2
UP 2S 1= 7.7683275937E-04*T**(-9.9446500000E-01)*HTC*DT
SUMP 1=P 1S 2*X 2
SUMP 2=P 2S 1*X 1
B 1=1.0+SUMP 1/X 1
H 2=1.0+SUMP 2/X 2
RLM=+RL 1/B 1+KL 2/B 2
RHLM(IC)=RH*RLM
C SPACE DER OF DENSITY TIMES THERMAL COND.
100 DRL 1= 4.694228E-06*(T**(-2.616700E-01))*DT
DRL 2= 5.125904E-07*(T**(-2.000400E-01))*DT
DYS=DYS/(YS*YS)
DX 1=DY 1/YS-Y 1*DYYS
DX 2=DY 2/YS-Y 2*DYYS
105 USUMP 1=+OP 1S 2*X 2+P 1S 2*DX 2
110
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115      USUMP 2=+DP 2S 1*X 1+P 2S 1*DX 1
      DH 1=(DSUMP 1-SUMP 1*DX 1/X 1)/X 1
      DH 2=(DSUMP 2-SUMP 2*DX 2/X 2)/X 2
      T 1=(URL 1-RL 1*UH 1/B 1)/H 1
      T 2=(URL 2-RL 2*UH 2/B 2)/H 2
120      DRLM=+T 1+T 2
      DRHLM(1C)=DRH*KLM+RH*DRLM
      C SOLVE FOR UV.
      SUM 1=+X 2*VD 1 2
      SUM 2=+X 1*VD 1 2
      H 1=X 1*SUM 1* 5.0000E-05
      H 2=X 2*SUM 2* 5.0000E-05
      T 1=-RH*(1.0-U 1)
      T 2=-RH*(1.0-U 2)
      FAC 1=T 1/B 1
      FAC 2=T 2/B 2
      V 1=FAC 1*DX 1
      V 2=FAC 2*DX 2
      UV 1=U 1*V 1
      UV 2=U 2*V 2
      UV=-UV 1-UV 2
      UV 1=UV 1+DV*U 1
      UV 2=UV 2+DV*U 2
      RHUV(1ST+ 1)=RH*UV 1
      RHUV(1ST+ 2)=RH*UV 2
140      C SPACE DER OF DENSITY TIMES UV.
      DUY 1=DUU 1/ 2*00
      DUY 2=DUU 2/ 28*00
      DUYS=+DDY 1+DDY 2
      UYSQ=(UY/YS)**2
      DUX 1=(DDY 1-2*0*UY 1*UY/YS+2*0*Y 1*UY/YS)/YS
      DUX 2=(DDY 2-2*0*UY 2*UY/YS+2*0*Y 2*UY/YS)/YS
      DSUM 1=+DX 2*VD 1 2+X 2*DVD 1 2
      DT 1=-DRH*(1.0-U 1)+HH*DU 1
      DT 2=-DRH*(1.0-U 2)+HH*DU 2
      DFAC 1=DT 1/B 1-T 1*UH 1/B 1*(B 1*B 1)
      DFAC 2=DT 2/B 2-T 2*UH 2/B 2*(B 2*B 2)
      UV 1=DFAC 1*DX 1+FAC 1*DDX 1
      UV 2=DFAC 2*DX 2+FAC 2*DDX 2
      UUV 1=DUU 1*V 1+U 1*UV 1
      UUV 2=DUU 2*V 2+U 2*UV 2
      DUUV=-DUV 1-DUV 2
      UUV 1=DUV 1+DV*DUU 1+DUV*U 1
      UUV 2=DUV 2+DV*DUU 2+DUV*U 2
      DRHUV(1ST+ 1)=DRH*UUV 1+RH*DUV 1
      DRHUV(1ST+ 2)=DRH*UUV 2+RH*DUV 2
160      C FIND THE TIME DERIVATIVES.
      SP=ASP+RSP*TIME
100      CONTINUE
      IF(KPDE.EQ.NPDE)GO TO 150
      HY= 1.000000000E-03*(KPDE)
      DY=- 2.000000000E+01*(DRHUV(1-T*KPDE)
      FVAL=SP*UPH(KPDE)+DY+HY
      RETURN
150      CONTINUE
      DU 1=UPH( 1)
      DU 2=-DU 1

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```

      TL= 4.0000000000E+05*
      * (URHLM(IC)*UPH(NPDE)+RHLM(IC)*UFH2(NPDE))
      TD=- 2.0000000000E+01*UPH(NPDE)*( +C(IST+ 1)*RHUV(IST+ 1) +
      * C(IST+ 2)*RHUV(IST+ 2))
      TH=- 1.0000000000E-06*( +R( 1)*H(IST+ 1) +R( 2)*H(IST+ 2))
      FVAL=SP*UPH(NPDE)+(TL+TR*TD)/CM(IC)
      RETURN
      END

```

```

      F      173
      F      174
      F      175
      F      176
      F      177
      F      178
      F      179
      F      180

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175

04/15/80 14.10.20

FTN 4.8+498

TRACE

76/76

PROGRAM LOAD

OPT=1

KOUND=+-*/

```

1      PROGRAM LOADF (INPUT,OUTPUT,TAPE4=INPUT,TAPE6=OUTPUT,
2      * TAPE3,TAPE9,TAPE15)
3      C LOADF CREATES THE SUBROUTINE F IN FLSC.
4      DIMENSION I1(72)
5      DIMENSION I11(44)
6      DIMENSION LB(25),W(25),AU(7,25),AL(7,25)
7      DIMENSION ALD(25),RLD(25),ARD(25,25),RHU(25,25)
8      DIMENSION AV(25),RV(25)
9      DIMENSION LBPR(25)
10     WRITE(3,1000)
11     FORMAT(1HC,2X,63HFOR THE COMPLETE TRANSPORT CASE, WE DO NOT WANT T
12     *HE U VALUES OR)
13     WRITE(3,1005)
14     FORMAT(1HC,2X,62HTHEIR FIRST DERIVATIVES TO BE ZERO. THIS CAN LEA
15     *D TO DIVISION)
16     WRITE(3,1010)
17     FORMAT(1HC,2X,8HHY ZERO.)
18     WRITE(3,1012)
19     FORMAT(6X,14HDO 5 K=1,NPDEM)
20     WRITE(3,1014)
21     FORMAT(6X,32HF(ABS(U(K)).LT.SMALL)U(K)=SMALL)
22     WRITE(3,1016)
23     FORMAT(1X,1H5,4X,36HF(ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL)
24     READ(5,12)NLINE
25     C NLINE IS THE NUMBER OF COMMENT LINES TO BE READ AND PRINTED.
26     DO 20 K=1,NLINE
27     READ(5,22)I1
28     WRITE(3,22)I1
29     CONTINUE
30     FORMAT(72A1)
31     FORMAT(/1X,72A1/)
32     READ(5,12)NSPC
33     NM=NSPC-1
34     LHM=1H-
35     LBU=2HU(
36     LHP=1H)
37     WRITE(3,1020)((LHM,LHU,K,LHP),K=1,NM)
38     FORMAT(6X,6HYN=1.0,R(A1,A2,12,A1),A1,2(/5X,1H*,1X,
39     * R(A2,12,A1,A1)) )
40     WRITE(3,1025)
41     FORMAT(6X,33HCALL RT(U,YN,R,NPDE,KPUE,IC,KSKH) )
42     WRITE(3,18)NSPC
43     FORMAT(6X,4HIST=.12,7H*(IC-1) )
44     DO 30 K=1,NSPC
45     READ(5,32)LB(K),W(K)
46     WRITE(6,34)K,LB(K),W(K)
47     READ(15,36)(AU(L,K),L=1,5),(I11(L),L=1,5)
48     WRITE(6,36)(AU(L,K),L=1,5),(I11(L),L=1,5)
49     READ(15,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(I11(L),L=1,5)
50     WRITE(6,36)(AU(L,K),L=6,7),(AL(L,K),L=1,3),(I11(L),L=1,5)
51     READ(15,37)(AL(L,K),L=4,7),(I11(L),L=1,20)
52     WRITE(6,37)(AL(L,K),L=4,7),(I11(L),L=1,20)
53     CONTINUE
54     FORMAT(A5,7F7.0)
55     FORMAT(/2X,14,4X,A5,4X,F8.2/)
56     FORMAT(5E15,8,5A1)
57
58

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37  FORMAT(4E15.8,20A1)
    HEAD(5,232)TPN,PHN,TMN
232  FORMAT(1P3E12.4)
    WRITE(3,27)
27   FORMAT(6X,22HIF(KSK1,GT,1)GO TO 100)
    WRITE(3,28)
28   FORMAT(6X,22HIF(KSKR,GT,1)GO TO 125 )
    HEAD(5,12)NLINE
    DO 40 K=1,NLINE
    HEAD(5,22)11
    WRITE(3,22)11
40   CONTINUE
C *****
C  C ENTHALPIES AND HEAT CAPACITIES.
C *****
    WRITE(3,42)
42   FORMAT(6X,24HIF(T,GT,1000.)GO TO 2000)
    DO 50 K=1,NSPC
    WRITE(3,52)K,AL(1,K),AL(2,K)
    WRITE(3,54)AL(L,K),L=3,5)
    WRITE(3,62)K,AL(6,K),AL(1,K)
    WRITE(3,64)AL(2,K),AL(3,K)
    WRITE(3,66)AL(4,K),AL(5,K)
50   CONTINUE
52   FORMAT(6X,1HC,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
54   FORMAT(5X,1H*,1X,3(4H+T*(,1PE16.8),5H))))
    WRITE(3,56)
56   FORMAT(6X,10HGO TO 3000)
    WRITE(3,58)
58   FORMAT(4H2000,2X,8HCCONTINUE)
    DO 60 K=1,NSPC
    WRITE(3,52)K,AL(1,K),AL(2,K)
    WRITE(3,54)AL(L,K),L=3,5)
    WRITE(3,62)K,AL(6,K),AL(1,K)
    WRITE(3,64)AL(2,K),AL(3,K)
    WRITE(3,66)AL(4,K),AL(5,K)
60   CONTINUE
62   FORMAT(6X,1HH,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
64   FORMAT(5X,1H*,1X,4H+T*(,1PE16.8,4H/2.0,4H+T*(,1PE16.8,4H/3.0)
66   * 4H/5.0,6H))))))
    WRITE(3,68)
68   FORMAT(4H3000,2X,8HCCONTINUE)
    WRITE(3,134)
134  FORMAT(1HC,2X,39HSPECIFIC HEATS AND SPECIFIC ENTHALPIES. )
    DO 140 K=1,NSPC
    WRITE(3,142)K,K,W(K)
    WRITE(3,144)K,K,W(K)
140  CONTINUE
142  FORMAT(6X,6HC(1ST,12,3H)=C,12,1H/,F6.2)
144  FORMAT(6X,6HH(1ST,12,3H)=H,12,1H/,F6.2)
    WRITE(3,146)
146  FORMAT(1X,3H125,2X,8HCCONTINUE)
C *****
C  C THERMAL CONDUCTIVITIES AND BINARY DIFFUSION COEFFICIENTS.
C  C HEAD IN VISCOSITY, THERMAL CONDUCTIVITY, AND BINARY DIFFUSION
C  C COEFFICIENTS FROM A FILE CREATED BY VALUES, CY=6.

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04/15/80 14.10.20

FTN 4.8+498

PROGRAM LOADF 76/76 OPT=I ROUNO=-*/ TRACE

```

115 C *****
      READ(5,12)NLINE
      DO 72 K=1,NLINE
120      READ(5,22)I1
        WRITE(6,22)I1
121      WRITE(3,22)I1
122      FORMAT(1HC,5X,IHV,12,IH=,1PE14.6,5H*(T**,1PE14.6,IH) )
123      READ(5,12)NLINE
124      DO 70 K=1,NLINE
125      READ(5,22)I1
        WRITE(3,22)I1
        WRITE(6,22)I1
126      CONTINUE
127      DO 80 K=1,NSPC
128      READ(9,82)AV(K),BV(K),I1I
129      WRITE(6,84)K,LB(K),AV(K),BV(K),I1I
130      READ(9,82)ALD(K),BLD(K),I1I
131      WRITE(6,84)K,LB(K),ALD(K),BLD(K),I1I
132      CONTINUE
133      FORMAT(1P2E14.6,44A1)
134      DO 78 K=1,NSPC
135      READ(1,2X,I4,4X,A4,4X,1P2E14.6,44A1/)
        DO 78 K=1,NSPC
136      WRITE(3,79)K,AV(K),BV(K)
137      CONTINUE
138      DO 90 K=1,NSPC
139      WRITE(3,92)K,ALD(K),BLD(K)
140      CONTINUE
141      FORMAT(6X,2HRL,12,IH=,1PE14.6,5H*(T**,1PE14.6,IH) )
142      READ(5,12)NLINE
143      DO 100 K=1,NLINE
144      READ(5,22)I1
145      WRITE(3,22)I1
        WRITE(6,22)I1
146      CONTINUE
147      NM=NSPC-1
148      DO 110 I=1,NSPC
149      DO 110 J=1,NSPC
150      READ(9,82)ABD(I,J),HBD(I,J),I1I
151      WRITE(6,112)I,J,LB(I),LB(J),ABD(I,J),HBD(I,J),I1I
152      CONTINUE
153      FORMAT(2X,I4,4X,I4,4X,A4,4X,1P2E14.6,44A1/)
154      READ(5,114)PRESS
155      FORMAT(F6.0)
156      WRITE(3,116)PRESS
157      FORMAT(1HC,2X,7HPRESS =,F6.2)
158      DO 120 I=1,NM
159      IP=I+1
160      DO 120 J=IP,NSPC
161      ABD(I,J)=ABD(I,J)/PRESS
162      WRITE(3,122)I,J,ABD(I,J),HBD(I,J)
163      CONTINUE
164      FORMAT(1HC,5X,IHV,12,IH=,1PE14.6,5H*(T**,1PE14.6,IH) )
165      C *****
166      C SPACE DERIVATIVES.
167      C *****
168      LPL=1H+
169      WRITE(3,I4R)
170

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175      148  FORMAT(IHC,2X,IHSPACE DERIVATIVE,S.)
           NS=NSPC+I
           WRITE(3,I49)NS
180      149  FORMAT(6X,4HYS=Y,I2)
           DO 150 K=1,NSPC
           WRITE(3,I52)K,K
           CONTINUE
           FORMAT(6X,IHX,I2,2H=Y,I2,3H/Y,S)
           DO 160 K=1,NM
           WRITE(3,I62)K,K
           WRITE(3,I64)K,K
           WRITE(3,I66)K,K
           CONTINUE
           FORMAT(6X,IHU,I2,3H=U(I2,IH))
           FORMAT(6X,2HUU,I2,5H=UPH(I2,IH))
           FORMAT(6X,3HDDU,I2,6H=UPH2(I2,IH))
           LHU=IHU
           WRITE(3,I72)NSPC,((LBM,LBU,K),K=1,NM)
           FORMAT(6X,IHU,I2,4H=1.0,8(AI,AI,I2),AI,2(/5X,IH*,IX,
           * 8(AI,I2,AI)))
           LBDU=2HUU
           WRITE(3,I74)NSPC,((LBM,LBDU,K),K=1,NM)
           FORMAT(6X,2HUU,I2,IH=,8(AI,A2,I2),AI,2(/5X,IH*,IX,
           * 8(A2,I2,AI)))
           LHDDU=3HDDU
           WRITE(3,I76)NSPC,((LBM,LHDDU,K),K=1,NM)
           FORMAT(6X,3HDDU,I2,IH=,8(AI,A3,I2),AI,2(/5X,IH*,IX,
           * 8(A3,I2,AI)))
           DO 180 K=1,NSPC
           WRITE(3,I82)K,K,w(K)
           CONTINUE
           FORMAT(6X,2HDY,I2,3H=DU,I2,IH=/f6.2)
           LBU=2HDY
           WRITE(3,I86)((LHPL,LBDY,K),K=1,IUSPC)
           FORMAT(6X,4HDYS=,8(AI,A2,I2),AI,2(/5X,IH*,IX,8(A2,I2,AI))
           PSR=PRESS/82.05
           WRITE(3,I234)IPN,PHN,IMN
           WRITE(6,I234)IPN,PHN,IMN
           FORMAT(IHC,2X,5HTPN =,IPEI2.4,6X,5HPHN =,IPEI2.4,6X,
           * 5HTMN =,IPEI2.4)
           WRITE(3,I226)IPN
           FORMAT(6X,I3HOT=UPH(NPDE)*,IPEI2.4)
           WRITE(3,I242)PSR
           FORMAT(6X,5HDRH=,IPEI8.10,2IH*(I/T/I+DYS/Y,S)/(T*YS))
           DO 800 K=1,NSPC
           A=ALD(K)*BLD(K)
           H=BLD(K)-I.0
           WRITE(3,I803)K,A,H
           CONTINUE
           FORMAT(6X,3HDL,I2,IH=,IPEI6.8,HH*(T*(,IPEI6.8,5H)))*DT)
           DO 805 K=1,NSPC
           A=I.0/ALD(K)
           H=-BLD(K)
           WRITE(3,I808)K,A,H
           CONTINUE
           FORMAT(6X,2HVL,I2,IH=,IPEI6.8,HH*(T*(,IPEI6.8,2H))
           DO 809 K=1,NSPC

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04/15/80 14.10.20

FTN 4.8*49H

OPT=1 ROUND=+-*/ TRACE

75/76

PROGRAM LOADF

```

230      A=1.0/ALD(K)
231      H=-BLD(K)
232      A=A*B
233      H=B-1.0
234      WRITE(3,813)K,A,H
235      CONTINUE
236      FORMAT(6X,3HVD,2I2,1H=,1PE16.8,6H*(T**(.1PE16.8,5H))*DT)
237      DO 815 I=1,NSPC
238      DO 815 J=1,NSPC
239      IF(1.EQ.J)GO TO 815
240      A=1.0/ABD(1,J)
241      H=-BRD(1,J)
242      WRITE(3,818)I,J,A,B
243      CONTINUE
244      FORMAT(6X,2HVD,2I2,1H=,1PE16.8,6H*(T**(.1PE16.8,2H)) )
245      DO 820 I=1,NSPC
246      DO 820 J=1,NSPC
247      IF(1.EQ.J)GO TO 820
248      A=1.0/ABD(1,J)
249      H=-BRD(1,J)
250      A=A*B
251      H=B-1.0
252      WRITE(3,822)I,J,A,B
253      CONTINUE
254      FORMAT(6X,3HVD,2I2,1H=,1PE16.8,6H*(T**(.1PE16.8,5H))*DT)
255      C *****
256      C SPECIFIC HEAT OF THE MIXTURE.
257      C *****
258      WRITE(3,124)
259      FORMAT(1HC,2X,44HSPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA. )
260      LBC=6HC(1ST+
261      LBU=3H)*U
262      WRITE(3,132)((LHPL,LBC,K,LBU,K),K=1,NSPC)
263      FORMAT(6X,7HCM(1C)=,4(A1,A6,12,A3,12),A1,
264      * 4(/5X,1H*,1X,4(A6,12,A3,12,A1)) )
265      C *****
266      C THERMAL CONDUCTIVITY OF THE MIXTURE.
267      C *****
268      WRITE(3,272)
269      WRITE(3,274)
270      FORMAT(1HC,2X,36HTHERMAL CONDUCTIVITY OF THE MIXTURE.)
271      FORMAT(1HC,2X,46HAVERAGE OF LINEAR AND RECIPROCAL MIXING RULES. )
272      LHX=1HX
273      LHPL=1H+
274      LRL=3H*RL
275      LBMIX=5HRLSUM
276      WRITE(3,260)LBMIX,((LHPL,LHX,K,L*RL,K),K=1,NSPC)
277      FORMAT(6X,A5,1H=,6(2A1,12,A3,12),A1,2(/5X,1H*,1X,
278      * 8(A1,12,A3,12,A1)) )
279      LBSRL=3H*VL
280      LBMIX=5HRLSIV
281      WRITE(3,260)LBMIX,((LHPL,LHX,K,L*SRL,K),K=1,NSPC)
282      WRITE(3,265)
283      FORMAT(6X,15HRLSIV=1.0/RLSIV )
284      WRITE(3,270)
285      FORMAT(6X,21HRLM=0.5*(RLSUM+RLSIV) )
286      WRITE(3,306)

```

```

306  FORMAT(6X,15HRHLM(IC)=RH*RLM)
C *****
C  DERIVATIVE OF THE THERMAL CONDUCTIVITY OF THE MIXTURE.
C *****
290  WRITE(3,312)
312  FORMAT(1HC,2X,40HSPACE DER OF DENSITY TIMES THERMAL COND.)
      WRITE(3,745)
745  FORMAT(6X,16HDYSY=DYS/(YS*YS) )
      DO 750 K=1,NSPC
750  WRITE(3,752)K,K,K
752  CONTINUE
      FORMAT(6X,2HDX,12,3H=0Y,12,5H/Y5-Y,12,5H*UYSY )
      LBDR=4H*DRL
      LBHX=2HDX
      LHM1X=5HDLSUM
      WRITE(3,760)LM1X,((LBPL,LBX,K,LBDR,LK,LBPL,LBDX,K,LBRL,K),
      * K=1,NSPC)
760  FORMAT(6X,A5,1H=,2(2A1,12,A4,12,A1,A2,12,A3,12),A1,
      * 6(/5X,1H*,1X,3(A1,12,A4,12,A1,A2,12,A3,12,A1)) )
      LBPAR=1H)
      LBMI1X=5HDLS1V
      LBVDL=4H*DVL
      WRITE(3,765)LBMI1X,((LBPL,LBDX,K,LBSRL,K,LBPL,LBX,K,LBDVL,K),
      * K=1,NSPC)
765  FORMAT(6X,A5,1H=,2(A1,A2,12,A3,12,2A1,12,A4,12),A1,
      * 6(/5X,1H*,1X,3(A2,12,A3,12,2A1,12,A4,12,A1)) )
      WRITE(3,770)
770  FORMAT(6X,24HDLS1V=-RLS1V*RLS1V*ULS1V )
      WRITE(3,775)
775  FORMAT(6X,22HDRLM=0.5*(DLSUM*ULS1V) )
      WRITE(3,778)
778  FORMAT(6X,25HDRHLM(IC)=DRH*RLM*RH*DRLM)
C *****
C  SOLVE FOR UV.
C  HIRSHFELDER AND CURTISS APPROXIMATION.
C  THE VELOCITY OF THE LAST SPECIES IS DETERMINED ONLY BY THE RELATION
C  SUM Y1*V1 = 0.0
C *****
325  WRITE(3,400)
400  FORMAT(1HC,2X,13HSOLVE FOR UV.)
      LBX=1HX
      LBVD=3H*VD
      K=1
402  WRITE(3,402)K,((LBPL,LBX,J,LBVD,K,J),J=2,NSPC)
      FORMAT(6X,3HSUM,12,1H=,5(2A1,12,A3,212),A1,
      * 3(/5X,1H*,1X,5(A1,12,A3,212,A1)) )
      IF(NM.EQ.1)GO TO 412
      DO 410 K=2,NM
      KM=K-1
      KP=K+1
      WRITE(3,402)K,((LBPL,LBX,J,LBVD,K,J),J=1,KM),((LBPL,LBX,J,
      * LBVD,K,J),J=KP,NSPC)
      CONTINUE
410  CONTINUE
412  I=0
415  K=I+NM
      WRITE(3,418)K,K,K,P-IN
      CONTINUE
340  CONTINUE
341  CONTINUE

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04/15/80 14.10.20

FTN 4.8+498

PROGRAM LOADF 76/76 OPT=1 KOUND=+*/ IRACE

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345 418 FORMAT(6X,IHB,I2,2H=X,I2,4H=SUM,I2,1H*,1PEI2,4)
      DO 420 K=1,NM
      WRITE(3,422)K,K
      CONTINUE
420 422 FORMAT(6X,1HT,I2,11H=-RH*(1.0-U,I2,1H) )
      DO 425 K=1,NM
      WRITE(3,428)K,K,K
      CONTINUE
425 428 FORMAT(6X,3HFA, I2,2H=T,I2,2H/B,I2)
      DO 465 K=1,NM
      WRITE(3,468)K,K,K
      CONTINUE
465 468 FORMAT(6X,1HV,I2,4H=FA, I2,3H*U, I2)
      DO 470 K=1,NM
      WRITE(3,472)K,K,K
      CONTINUE
470 472 FORMAT(6X,2HUV,I2,2H=U,I2,2H*V,I2)
      LBUV=2HUV
      LBM=1H-
      WRITE(3,476)NSPC,((LBM,LBUV,K),K=1,NM)
476 476 FORMAT(6X,2HUV,I2,1H=,I0(A1,A2,I2),A1,5X,1H*,1X,I0(A2,I2,A1))
      DO 485 K=1,NSPC
      WRITE(3,488)K,K
      CONTINUE
485 488 FORMAT(6X,9HRHUV(1ST,I2,7H)=HH*UV,I2)
      C *****
      C SOLVE FOR THE SPACE DERIVATIVE OF UV.
      C *****
      WRITE(3,522)
522 522 FORMAT(1HC,2X,30HSPACE DER OF DENSITY TIMES UV.)
      DO 500 K=1,NSPC
      WRITE(3,502)K,K,W(K)
      CONTINUE
500 502 FORMAT(6X,3HDDY,I2,4H=DDU,I2,1H/,F6,2)
      LDDY=3HDDY
      WRITE(3,506)((LHPL,LDDY,K),K=1,NSPC)
506 506 FORMAT(6X,5HDDYS=,8(A1,A3,I2),A1,2(/5X,1H*,1X,8(A3,I2,A1)) )
      WRITE(3,510)
510 510 FORMAT(6X,18HDDYSU=(DYS/YS)**2 )
      DO 515 K=1,NSPC
      WRITE(3,518)K,K,K,K,K
      CONTINUE
515 518 FORMAT(6X,3HDDX,I2,5H=(DUY,I2,7H-2.0*UY,I2,13H*DYS/YS+2.0*Y,
      * I2,9H*DYSU-Y,I2,12H*DDYS/YS)/YS )
      LBDX=2HDX
      LBDY=3H*VD
      LBDVD=4H*DVD
      LBA=1HX
      K=1
      WRITE(3,532)K,((LHPL,LHDX,J,LBVD,K,J,LHPL,LHX,J,LBDVD,K,J),J=2,
      * NSPC)
532 532 FORMAT(6X,4HDSUM,I2,1H=,2(A1,A2,I2,A3,2I2,2A1,I2,A4,2I2),A1,
      * 9(/5X,1H*,1X,2(A2,I2,A3,2I2,2A1,I2,A4,2I2,A1)) )
      IF(NM.EQ.1)GO TO 537
      DO 535 K=2,NM
      KM=K-1
      KP=K+1

```

Line	Code	Statement	Column
343	41R	FORMAT(6X,1HB,12,2H=X,12,4H*SUM,12,1H*,1PE12,4)	MAIN
345		DO 420 K=1,NM	MAIN
346	420	WRITE(3,422)K,K	MAIN
347		CONTINUE	MAIN
348	422	FORMAT(6X,1HT,12,1IH=-RH*(1,0-U,12,1H))	MAIN
349		DO 425 K=1,NM	MAIN
350		WRITE(3,42R)K,K,K	MAIN
351	425	CONTINUE	MAIN
352	42R	FORMAT(6X,3HFAC,12,2H=T,12,2H/B,12)	MAIN
353		DO 465 K=1,NM	MAIN
354	465	WRITE(3,46R)K,K,K	MAIN
355	46R	CONTINUE	MAIN
356		FORMAT(6X,1HV,12,4H=FAC,12,3H*U,12)	MAIN
357		DO 470 K=1,NM	MAIN
358	470	WRITE(3,472)K,K,K	MAIN
359	472	CONTINUE	MAIN
360		FORMAT(6X,2HUV,12,2H=U,12,2H*V,12)	MAIN
361		LUV=2HUV	MAIN
362		LHM=1H-	MAIN
363	476	WRITE(3,476)NSPC,((LHM,LBUV,K),K=1,NM)	MAIN
364		FORMAT(6X,2HUV,12,1H=,10(A1,A2,12),A1,5X,1H*,1X,10(A2,12,A1))	MAIN
365		DO 485 K=1,NSPC	MAIN
366		WRITE(3,48R)K,K	MAIN
367	485	CONTINUE	MAIN
368	48R	FORMAT(6X,9HRHUV(1ST*,12,7H)=RH*UV,12)	MAIN
369	C	*****	MAIN
370	C	SOLVE FOR THE SPACE DERIVATIVE OF UV.	MAIN
371		*****	MAIN
372		WRITE(3,522)	MAIN
373	522	FORMAT(1HC,2X,30HSPACE DER OF DENSITY TIMES UV,)	MAIN
374		DO 500 K=1,NSPC	MAIN
375		WRITE(3,502)K,K,W(K)	MAIN
376	500	CONTINUE	MAIN
377	502	FORMAT(6X,3HDDY,12,4H=DDU,12,1H*,F6.2)	MAIN
378		LDDY=3HDDY	MAIN
379		WRITE(3,506)((LBPL,LDDY,K),K=1,NSPC)	MAIN
380	506	FORMAT(6X,5HDDYS=8(A1,A3,12),A1,2(5X,1H*,1X,8(A3,12,A1)))	MAIN
381		WRITE(3,510)	MAIN
382	510	FORMAT(6X,18HDYSYSU=(DYS/Y5)**2)	MAIN
383		DO 515 K=1,NSPC	MAIN
384		WRITE(3,51R)K,K,K,K	MAIN
385	515	CONTINUE	MAIN
386	51R	FORMAT(6X,3HDDX,12,5H=(DDY,12,7H=2,0*UY,12,13H*UYS/Y5+2,0*Y,	MAIN
387		* 12,9H*DYYSO-Y,12,12H*DDYS/Y5)/Y5)	MAIN
388		LBDX=2HDX	MAIN
389		LBDV=3H*VD	MAIN
390		LBDVD=4H*DVD	MAIN
391		LHX=1HX	MAIN
392		K=1	MAIN
393		WRITE(3,532)K,((LHPL,LBDX,J,LBDV,K,J,LHPL,LHX,J,LBDVD,K,J),J=2,	MAIN
394		* NSPC)	MAIN
395	532	FORMAT(6X,4HDSUM,12,1H=,2(A1,A2,12,A3,2I2,2A1,12,A4,2I2),A1,	MAIN
396		* 9(5X,1H*,1X,2I2,12,A3,2I2,2A1,12,A4,2I2,A1)))	MAIN
397		IF(NM.EQ.1)GO TO 537	MAIN
398		DO 535 K=2,NM	LOADFX3
399		KN=K-1	MAIN
400		KP=K+1	MAIN

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400      WRITE(3,532)K,((LHPL,LBDX,J,LHVL,J,K,LBPL,LHX,J,LHDVD,J,K),J=I,KM)
      * ,((LHPL,LBDX,J,LHVL,J,K,LBPL,LHX,J,LHDVD,K,J),J=KP,NSPC)
      CONTINUE
535      CONTINUE
537      DO 540 K=I,NM
      WRITE(3,542)K,PHN,K,K,K,K
      CONTINUE
540      CONTINUE
542      * 5H*DSUM,I2,IH) )
      DO 545 K=I,NM
      WRITE(3,548)K,K,K,K
      CONTINUE
545      CONTINUE
548      FORMAT(6X,2HDT,I2,12H=-DRH*(I,0-U,I2,7H)+RH*DU,I2)
      DO 550 K=I,NM
      WRITE(3,552) (K,L=I,7)
      CONTINUE
550      CONTINUE
552      FORMAT(6X,4HDFAC,I2,1H=-2HDT,I2,2H/B,I2,2H-T,I2,3H*DB,I2,
      * 3H/(H,I2,2H*B,I2,IH) )
      DO 590 K=I,NM
      WRITE(3,592)K,K,K,K,K
      CONTINUE
590      CONTINUE
592      FORMAT(6X,2HUV,I2,5H=DFAC,I2,3H*UX,I2,4H*FAC,I2,4H*DDX,I2)
      DO 595 K=I,NM
      WRITE(3,598)K,K,K,K,K
      CONTINUE
595      CONTINUE
598      FORMAT(6X,3HUV,I2,3H=DU,I2,2H*V,I2,2H+U,I2,3H*DV,I2)
      LBUV=3HUV
      WRITE(3,802)NSPC,((LBM,LBDUV,K),K=I,NM)
      * 9(A3,I2,A1) )
      DO 810 K=I,NSPC
      WRITE(3,812)K,K,K
      CONTINUE
810      CONTINUE
812      FORMAT(6X,10HURHUV(I2+,I2,8H)=UH*UV,I2,7H+RH*DUV,I2)
      C *****
      C FIND THE TIME DERIVATIVES.
      C *****
      WRITE(3,612)
      FORMAT(1H,2X,26HFIND THE TIME DERIVATIVES.)
      WRITE(3,622)
      FORMAT(6X,15HSP=ASP+RSP*TIME)
      TMSPH2=TMN/(PHN*PHN)
      WRITE(3,628)
      FORMAT(1X,3HI00,2X,RHCONTINUE)
      WRITE(3,632)
      FORMAT(6X,25HIF(KPDE.EQ.NPDE)GO TO I50)
      WRITE(3,636)TMN
      FORMAT(6X,3HRY=,IPE20,I0,8H*H(KPDE) )
      TMSPH=TMN/PHN
      WRITE(3,638)TMSPH
      FORMAT(6X,4HUY=-,IPE20,I0,16H*URHUV(I2+KPDE) )
      WRITE(3,642)
      FORMAT(6X,23HFVAL=SP*UPH(KPDE)*IUY+RY)
      WRITE(3,646)
      FORMAT(6X,6HRETUHH)
      WRITE(3,648)
      FORMAT(1X,3HI50,2X,RHCONTINUE)

```


BLOCK	ADDRESS	LENGTH	FILE
LOADF	110	10331	LGO
/STP.END/	10441	1	SL-FTNL1B
/FCL.C./	10442	30	SL-FTNL1B
/J8.I0./	10472	144	SL-FTNL1B
QENTRY=	10636	4	SL-FTNL1B
COMIO=	10642	10	SL-FTNL1B
FECMSK=	10652	41	SL-FTNL1B
FEIFST=	10713	3	SL-FTNL1B
FLIN=	10716	156	SL-FTNL1B
FLIOUT=	11074	315	SL-FTNL1B
FMTAP=	11411	377	SL-FTNL1B
FORSYS=	12010	300	SL-FTNL1B
FORUTL=	12310	45	SL-FTNL1B
GETFIT=	12355	54	SL-FTNL1B
INCOM=	12431	144	SL-FTNL1B
INPC=	12575	173	SL-FTNL1B
KODER=	12770	476	SL-FTNL1B
KRAKER=	13466	454	SL-FTNL1B
OUTC=	14142	155	SL-FTNL1B
OUTCOM=	14317	204	SL-FTNL1B
ERRCAP=	14523	317	SL-FTNL1B
FERCAP=	15042	171	SL-FTNL1B
SYSALD=	15233	1	SL-FTNL1B

1 H2 2.00
 .31001901E+01 .5119464E+03 .52644210E-07 -.34909973E-10 .36945345E-14 H2
 -.87738042E+03 -.19629421E+01 .30574451E+01 .26765200E-02 -.58099162E-05 H2
 .55210391E-08 -.18122739E-11 -.98890474E+03 -.22997056E+01 H2

2 N2 28.00
 .28963194E+01 .15154866E-02 -.57235277E-06 .99807393E-10 -.65223555E-14 N2
 -.90586184E+03 .61615148E+01 .36748261E+01 -.12081500E-02 .23240102E-05 N2
 -.63217559E-09 -.22577253E-12 -.10611588E+04 .23580424E+01 N2

VISCOSITY FROM WARMATZ ST PAR.
 LEAST SQUARES FIT, T=300.2000.
 THERMAL CONDUCTIVITIES FROM WARMATZ ST PAR.
 LEAST SQUARES FIT, T=300.2000.

1 H2 2.188700E-06 6.502900E-01 H2 VISCOSITY.
 1 H2 6.357900E-06 7.383300E-01 H2 THERMAL CONDUCTIVITY.
 2 N2 4.266700E-06 6.613600E-01 N2 VISCOSITY.
 2 N2 6.407700E-07 7.999600E-01 N2 THERMAL CONDUCTIVITY.

BINARY DIFFUSION COEFFICIENTS FROM WARMATZ ST PAR.
 LEAST SQUARES FIT, T=300.2000.

1	2	H2	N2	5.951700E-05	1.663800E+00	H2	N2	MINARY DIFFUSION.
2	2	N2	N2	1.537400E-05	1.672900E+00	N2	N2	MINARY DIFFUSION.

TPN = 1.0000E+03 PHIN = 5.0000E-05 TMN = 1.0000E-03

```

1  SUBROUTINE F(TIME,PH,U,UPH,UPH2,FVAL,NPUE,KPUE,IC,KSKT,KSKR)
   DIMENSION U(NPUE),UPH(NPUE),UPH2(NPUE)
   COMMON/TARAH/ASP,ASP,IPN,PHN,IM3,IMSPH,IMSPH2,IMSTP,TPENT
   COMMON/TARP/PRESS,PSM,NPDEM
   COMMON/TARSM/SMALL
   DIMENSION R(20)
   DIMENSION C(1000),H(1000),RHM(100),DRHLM(100),CM(100)
   COMMON/TABCT/RL,CPMX,H0(20),R2D(20),R2DM(20)
   COMMON/TARMF/RHUV(1000),DRHUV(1000)
   COMMON/TABRY/T,RH,Y1,Y2,Y3,Y4,Y5,Y6,Y7,Y8,Y9,Y10
10  C AT EACH CALL THE TIME RATE OF CHANGE FOR ONE PDE IS RETURNED IN FVAL.
   C FOR THE COMPLETE TRANSPORT CASE, WE DO NOT WANT THE U VALUES OR
   C THEIR FIRST DERIVATIVES TO BE ZERO. THIS CAN LEAD TO DIVISION
   C BY ZERO.
15  DO 5 K=1,NPDEM
   IF (ABS(U(K)).LT.SMALL)U(K)=SMALL
5  IF (ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL
   C TEST CASE. BINARY MIX OF H2 AND N2. TRANSPORT WARNATZ PAR.
   C U = MASS FRACTIONS. Y = MASS FRACTIONS / MOLECULAR WEIGHTS.
   YN=1.0-U( 1)
   CALL RT(U,YN,R,NPUE,KPUE,IC,KSKR)
   IST= 2*(IC-1)
   IF(KSKT.GT.1)GO TO 100
   IF(KSKR.GT.1)GO TO 125
   C NTIS ENTHALPIES AND HEAT CAPACITIES.
   IF(T.GT.1000.)GO TO 2000
   C 1=1.9872*( 3.05744510E+00+T*( 2.67652000E-03
   *+T*( -5.80991620E-06+T*( 5.52103910E-09+T*( -1.81227390E-12))))))
   H 1=1.9872*( -9.84904740E+02+T*( 3.05744510E+00
   *+T*( 2.67652000E-03/2.0+T*( -5.80991620E-06/3.0
   *+T*( 5.52103910E-09/4.0+T*( -1.81227390E-12/5.0))))))
   C 2=1.9872*( 3.67482610E+00+T*( -1.20815000E-03
   *+T*( 2.32401020E-06+T*( -6.32175590E-10+T*( -2.25772530E-13))))))
   H 2=1.9872*( -1.06115880E+03+T*( 3.67482610E+00
   *+T*( -1.20815000E-03/2.0+T*( 2.32401020E-06/3.0
   *+T*( -6.32175590E-10/4.0+T*( -2.25772530E-13/5.0))))))
   GO TO 3000
2000 CONTINUE
   C 1=1.9872*( 3.10019010E+00+T*( 5.11194640E-04
   *+T*( 5.26442100E-08+T*( -3.49099730E-11+T*( 3.69453450E-15))))))
   H 1=1.9872*( -8.77380420E+02+T*( 3.10019010E+00
   *+T*( 5.11194640E-04/2.0+T*( 5.26442100E-08/3.0
   *+T*( -3.49099730E-11/4.0+T*( 3.69453450E-15/5.0))))))
   C 2=1.9872*( 2.89631940E+00+T*( 1.51548660E-03
   *+T*( -5.72352770E-07+T*( 9.98073930E-11+T*( -6.52235550E-15))))))
   H 2=1.9872*( -9.05861840E+02+T*( 2.89631940E+00
   *+T*( 1.51548660E-03/2.0+T*( -5.72352770E-07/3.0
   *+T*( 9.98073930E-11/4.0+T*( -6.52235550E-15/5.0))))))
3000 CONTINUE
   C SPECIFIC HEATS AND SPECIFIC ENTHALPIES.
   C(IST+ 1)=C 1/ 2.00
   H(IST+ 1)=H 1/ 2.00
   C(IST+ 2)=C 2/ 24.00
   H(IST+ 2)=H 2/ 24.00
125 CONTINUE
   C VISCOSITY FROM WARNATZ ST PAR.
   C LEAST SQUARES FIT, I=300,2000.

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60      C THERMAL CONDUCTIVITIES FROM WARMATZ ST PAR.
      C LEAST SQUARES FIT, T=300.2000.
      C V 1= 2.144700E-06*(T** 6.502900E-01)
      C V 2= 4.266700E-06*(T** 6.613600E-01)
      C RL 1= 6.357900E-06*(T** 7.383300E-01)
      C RL 2= 6.407700E-07*(T** 7.999400E-01)
65      C BINARY DIFFUSION COEFFICIENTS FROM WARMATZ ST PAR.
      C LEAST SQUARES FIT, T=300.2000.
      C PRESS = 1.00
      C D 1 2= 5.9517000E-05*(T** 1.4638000E+00)
      C SPACE DERIVATIVES.
      C YS=Y 3
      C X 1=Y 1/YS
      C X 2=Y 2/YS
      C U 1=U( 1)
      C DU 1=UPH( 1)
      C DUU 1=UPH2( 1)
      C U 2=1.0-U 1
      C DU 2=-DU 1
      C DUU 2=-DUU 1
      C DY 1=DU 1/ 2.00
      C DY 2=DU 2/ 28.00
      C DYS=+DY 1+DY 2
80      C TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03
      C DT=UPH(NPDE)* 1.0000E+03
      C DRH=- 1.2187690433E-02*(DT/T+DYS/YS)/(T*YS)
      C DHL 1= 4.69422831E-06*(T**(-2.6167000E-01))*DT
      C DHL 2= 5.12590369E-07*(T**(-2.0004000E-01))*DT
      C VL 1= 1.57284638E+05*(T**(-7.3433000E-01))
      C VL 2= 1.56062238E+06*(T**(-7.9996000E-01))
      C DVL 1= -1.16127967E+05*(T**(-1.7383300E+00))*DT
      C DVL 2= -1.24843548E+06*(T**(-1.7999600E+00))*DT
      C VD 1 2= 1.68019221E+04*(T**(-1.6638000E+00))
      C DVD 1 2= -2.79550381E+04*(T**(-2.6638000E+00))*DT
90      C SPECIFIC HEAT OF THE MIXTURE. NTIS FORMULA.
      C CM(IC)=C(IST+ 1)*U 1+C(IST+ 2)*U 2
      C THERMAL CONDUCTIVITY OF THE MIXTURE.
      C AVERAGE OF LINEAR AND RECIPROCAL MIXING RULES.
      C RLSUM=X 1*RL 1+X 2*VL 2
      C RLSIV=X 1*VL 1+X 2*VL 2
      C RLSIV=1.0/RLSIV
      C RLM=0.5*(RLSUM+RLSIV)
      C RMLM(IC)=RMLM
      C DYSY=DYS/(YS*YS)
100      C SPACE DER OF DENSITY TIMES THERMAL COND.
      C DX 1=DY 1/YS-Y 1*DYSY
      C DX 2=DY 2/YS-Y 2*DYSY
      C DLSUM=X 1*DLR 1+DX 1*RL 1+X 2*DLR 2+DX 2*RL 2
      C DLSIV=DX 1*VL 1+X 1*DLVL 1+DX 2*VL 2+X 2*DLVL 2
      C DLSIV=-RLSIV*RLSIV*DLVL 1
      C DRLM=0.5*(DLSUM+DLSIV)
      C DRMLM(IC)=DRH+RLM+RMLM*DRMLM
110      C SOLVE FOR UV.
      C SUM 1=X 2*VD 1 2
      C H 1=X 1*SUM 1* 5.0000E-05
      C T 1=-H*(1.0-U 1)
      C FAC 1=T 1/R 1

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04/15/80 14.10.34

FTN 4.8+498

76/76 OPT=1 ROUNDED=+*/ 1+ACE

SUBROUTINE F

```

115      V 1=FAC 1*DX 1
      UV 1=U 1*V 1
      UV 2=-UV 1
      RHUV(1ST+ 1)=RH*UV 1
      RHUV(1ST+ 2)=RH*UV 2
120      C SPACE DER OF DENSITY TIMES UV.
      DDY 1=DDU 1/ 2*00
      DDY 2=DDU 2/ 28*00
      DDYS=+DDY 1+DDY 2
      DYSYSQ=(DYS/YS)**2
      DDY 1=(DDY 1-2*0*DY 1*DYS/YS+2*0*Y 1*DYSYSQ-Y 1*DDYS/YS)/YS
      DDY 2=(DDY 2-2*0*DY 2*DYS/YS+2*0*Y 2*DYSYSQ-Y 2*DDYS/YS)/YS
      USUM 1=+DX 2*VD 1 2+X 2*DVD 1 2
      DB 1= 5*000E-05*(DX 1*SUM 1+X 1*DSUM 1)
      DT 1=-DRH*(1.0-U 1)+RH*DU 1
      DFAC 1=DT 1/8 1-T 1*UH 1/(H 1*B 1)
      DV 1=DFAC 1*DX 1+FAC 1*DDX 1
      DUV 1=DU 1*V 1+U 1*UV 1
      DUV 2=-DUV 1
      DRHUV(1ST+ 1)=DRH*UV 1+RH*DUV 1
      DRHUV(1ST+ 2)=DRH*UV 2+RH*DUV 2
130      C FIND THE TIME DERIVATIVES.
      SP=ASP+BSP*TIME
100      CONTINUE
      IF (KPDE.EQ.NPDE)GO TO 150
      KY= 1.000000000E-03*R(KPDE)
      DY=- 2.000000000E+01*DRHUV(1ST+KPDE)
      FVAL=SP*UPH(KPDE)+DY*RY
      RETURN
150      CONTINUE
      DU 1=UPH( 1)
      DU 2=-DU 1
      TL= 4.000000000E+05*
      * (DRHLM(1C)*UPH(NPDE)+RHLM(1C)*UPH2(NPDE))
      TD=- 2.000000000E+01*UPH(NPDE)*( +C(151+ 1)*RHUV(1ST+ 1) +
      * C(1ST+ 2)*RHUV(1ST+ 2))
      TR=- 1.000000000E-06*( +R( 1)*H(1ST+ 1) +R( 2)*H(1ST+ 2))
      FVAL=SP*UPH(NPDE)+(TL+TR+TD)/CM(1C)
      RETURN
      END

```

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1  PROGRAM LOADF (INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,
2  * TAPE3,TAPE9,TAPE15)
3  C  LOADF CREATES THE SUBROUTINE F IN FLSC.
4  DIMENSION I1(72)
5  DIMENSION I11(44)
6  DIMENSION LB(25),W(25),AU(7,25),AL(7,25)
7  DIMENSION LBTHD(25)
8  DIMENSION ESK(25)
9  DIMENSION ALD(25),BLU(25),ABD(25,25),BBU(25,25)
10 DIMENSION AV(25),BV(25)
11 DIMENSION LBPR(25)
12 DIMENSION SGA(25),UM(25),ALP(25)
13 C  BOLIZMAN CONSTANT.
14 RK=1.38054E-16
15 WRITE(3,1000)
16 1000 FORMAT(1HC,2X,63HF, 'THE COMPLETE TRANSPORT CASE. WE DO NOT WANT T
17 *HE U VALUES OR)
18 WRITE(3,1005)
19 1005 FORMAT(1HC,2X,62HTHEIR FIRST DERIVATIVES TO BE ZERO. THIS CAN LEA
20 *D TO DIVISION)
21 WRITE(3,1010)
22 1010 FORMAT(1HC,2X,8HBY ZERO.)
23 WRITE(3,1012)
24 1012 FORMAT(6X,14HDO 5 K=1,NPDEM)
25 1014 FORMAT(6X,32HIF (ABS(U(K)).LT.SMALL)U(K)=SMALL)
26 WRITE(3,1016)
27 1016 FORMAT(1X,1H5,4X,36HIF (ABS(UPH(K)).LT.SMALL)UPH(K)=SMALL)
28 READ(5,12)NLINE
29 12 FORMAT(10I4)
30 C  NLINE IS THE NUMBER OF COMMENT LINES TO BE READ AND PRINTED.
31 DO 20 K=1,NLINE
32 READ(5,22)I1
33 WRITE(3,22)I1
34 CONTINUE
35 20 FORMAT(72A1)
36 22 FORMAT(1X,72A1/)
37 24 READ(5,12)NSPC
38 NM=NSPC-1
39 LBM=1H-
40 LBU=2HU(
41 LBP=1H)
42 WRITE(3,1020)((LBM,LBU,K,LBP),K=1,NM)
43 1020 FORMAT(6X,6HYN=1.0,M(1A1,A2,12,A1),A1,2(/5X,1H*,1X,
44 * 8(A2,12,A1,A1)) )
45 WRITE(3,1025)
46 1025 FORMAT(6X,33HCALL RT(U,YN,R,NPUE,KPUE,IC,KSKR) )
47 WRITE(3,18)NSPC
48 18 FORMAT(6X,4HIST=,12,7H*(IC-1) )
49 DO 30 K=1,NSPC
50 READ(5,32)LB(K),LBTHD(K),W(K),SGA(K),ESK(K),UM(K),ALP(K)
51 32 FORMAT(2A5,1P5E12.4)
52 WRITE(6,34)K,LB(K),LBTHD(K),W(K),SGA(K),ESK(K),UM(K),ALP(K)
53 34 FORMAT(/5X,14,2(SX,A5),1P5E12.4/)
54 C  COMPUTE AN APPROXIMATION FOR THERMAL DIFFUSION FOR THOSE SPECIES
55 C  WITH LBTHD = THOFF.
56 READ(15,36)(AU(L,K),L=1,5),(I11(L),L=1,5)
57 36 FORMAT(15,36)
58

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04/15/80 13.55.29

FTN 4.8*498

PROGRAM LOADF 76/76 OPT=I ROUNO=+*/* TRACE

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60      WRITE(6,36) (AU(L,K),L=1,5), (III(L),L=1,5)
      READ(15,36) (AU(L,K),L=6,7), (AL(L,K),L=1,3), (III(L),L=1,5)
      WRITE(6,36) (AU(L,K),L=6,7), (AL(L,K),L=1,3), (III(L),L=1,5)
      READ(15,37) (AL(L,K),L=4,7), (III(L),L=1,20)
      WRITE(6,37) (AL(L,K),L=4,7), (III(L),L=1,20)
      CONTINUE
30      FORMAT(5E15.8,5A1)
36      FORMAT(4E15.8,20A1)
37      READ(5,232) TPN,PHN,TMN
232      FORMAT(1P3E12.4)
      WRITE(3,27)
27      FORMAT(6X,22HIF(KSKI,GT,1)GO TO 100)
      WRITE(3,28)
28      FORMAT(6X,22HIF(KSKR,GT,1)GO TO 125 )
      READ(5,12) NLINE
      DO 40 K=1,NLINE
70      READ(5,22) II
      WRITE(3,22) II
40      CONTINUE
      C *****
      C ENTHALPIES AND HEAT CAPACITIES.
      C *****
80      WRITE(3,42)
42      FORMAT(6X,24HIF(T,GT,1000.)GO TO 2000)
      DO 50 K=1,NSPC
      WRITE(3,52) K,AL(1,K),AL(2,K)
      WRITE(3,54) (AL(L,K),L=3,5)
      WRITE(3,62) K,AL(6,K),AL(1,K)
      WRITE(3,64) AL(2,K),AL(3,K)
      WRITE(3,66) AL(4,K),AL(5,K)
50      CONTINUE
52      FORMAT(6X,1HC,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
54      FORMAT(5X,1H*,1X,3(4H+T*(,1PE16.8,5H))))))
      WRITE(3,56)
56      FORMAT(6X,10HGO TO 3000)
      WRITE(3,58)
58      FORMAT(4H2000,2X,4HCONTINUE)
      DO 60 K=1,NSPC
      WRITE(3,52) K,AU(1,K),AU(2,K)
      WRITE(3,54) (AU(L,K),L=3,5)
      WRITE(3,62) K,AU(6,K),AU(1,K)
      WRITE(3,64) AU(2,K),AU(3,K)
      WRITE(3,66) AU(4,K),AU(5,K)
100      CONTINUE
60      FORMAT(6X,1HH,12,9H=1.9872*(,1PE16.8,4H+T*(,1PE16.8)
62      FORMAT(5X,1H*,1X,4H+T*(,1PE16.8,4H/2.0,4H+T*(,1PE16.8,4H/3.0)
64      FORMAT(5X,1H*,1X,4H+T*(,1PE16.8,4H/4.0,4H+T*(,1PE16.8,
66      * 4H/5.0,6H))))))
      WRITE(3,68)
68      FORMAT(4H3000,2X,4HCONTINUE)
      WRITE(3,134)
134      FORMAT(1HC,2X,3HSPCIFIC HEATS AND SPECIFIC ENTHALPIES. )
      DO 140 K=1,NSPC
      WRITE(3,142) K,K,K(K)
      WRITE(3,144) K,K,K(K)
140      CONTINUE
142      FORMAT(6X,6HC(1ST*,12,3H)=C,12,1H*/F6.2)

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```
115      144  FORMAT(6X,6H(1ST,12,3H)=H,12,1H/,F6.2)
          WRITE(3,146)
116      146  FORMAT(1X,3H125,2X,8HCONTINUE)
117      C *****
118      C THERMAL CONDUCTIVITIES AND BINARY DIFFUSION COEFFICIENTS.
119      C READ IN VISCOSITY, THERMAL CONDUCTIVITY, AND BINARY DIFFUSION
120      C COEFFICIENTS FROM A FILE CREATED BY VALUES, CY=6.
121      C *****
122      READ(5,12)NLINE
123      DO 72 K=1,NLINE
124      READ(5,22)I1
125      WRITE(6,22)I1
126      72  WRITE(3,22)I1
127      79  FORMAT(1HC,5X,1HV,12,1H=,1PE14.6,5H*(T**,1PE14.6,1H) )
128      READ(5,12)NLINE
129      DO 70 K=1,NLINE
130      READ(5,22)I1
131      WRITE(3,22)I1
132      WRITE(6,22)I1
133      70  CONTINUE
134      DO 80 K=1,NSPC
135      READ(9,82)AV(K),BV(K),III
136      WRITE(6,84)K,LB(K),AV(K),BV(K),III
137      READ(9,82)ALD(K),BLD(K),III
138      WRITE(6,84)K,LB(K),ALD(K),BLD(K),III
139      CONTINUE
140      80  FORMAT(1P2E14.6,44AI)
141      82  FORMAT(/2X,14,4X,A4,4X,1P2E14.6,44AI/)
142      84  DO 78 K=1,NSPC
143      WRITE(3,79)K,AV(K),BV(K)
144      CONTINUE
145      DO 90 K=1,NSPC
146      WRITE(3,92)K,ALD(K),BLD(K)
147      CONTINUE
148      90  CONTINUE
149      92  FORMAT(6X,2HRL,12,1H=,1PE14.6,5H*(T**,1PE14.6,1H))
150      READ(5,12)NLINE
151      DO 100 K=1,NLINE
152      READ(5,22)I1
153      WRITE(3,22)I1
154      WRITE(6,22)I1
155      CONTINUE
156      NM=NSPC-1
157      DO 110 I=1,NSPC
158      DO 110 J=1,NSPC
159      READ(9,82)ABD(1,J),BBU(1,J),III
160      WRITE(6,112)I,J,LB(1),LB(J),ABU(1,J),BBU(1,J),III
161      CONTINUE
162      110  FORMAT(/2X,14,4X,14,4X,A4,4X,1P2E14.6,44AI/)
163      READ(5,114)PRESS
164      114  FORMAT(F6.0)
165      WRITE(3,116)PRESS
166      116  FORMAT(1HC,2X,7HPRESS =,F6.2)
167      DO 120 I=1,NM
168      IP=I+1
169      DO 120 J=1P,NSPC
170      ABU(1,J)=ABD(1,J)/PRESS
171      WRITE(3,122)I,J,ABU(1,J),+BD(1,J)
172
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04/15/80 13.55.29

FTN 4.8*498

PROGRAM LOADF 76/76 OPT=1 ROUNO=***/ TRACE

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175      120      CONTINUE
176      122      FORMAT(1HC,5X,1HU,212,1H=,1PE14.6,5H*(1*,1PE14.6,1H) )
177      READ(5,279)ARTP,CRTP,III
178      WRITE(6,123)ARTP,CRTP,III
179      READ(5,279)ACST,CCST,III
180      WRITE(6,123)ACST,CCST,III
181      FORMAT(1P2E14.6,44A1)
182      123      FORMAT(/2X,1P2E14.6,44A1)
183      C *****
184      C SPACE DERIVATIVES.
185      C *****
186      LBPL=1H*
187      WRITE(3,148)
188      FORMAT(1HC,2X,18HSPACE DERIVATIVES.)
189      NS=NSPC+1
190      WRITE(3,149)NS
191      FORMAT(6X,4HYS=Y,12)
192      DO 150 K=1,NSPC
193      WRITE(3,152)K,K
194      CONTINUE
195      FORMAT(6X,1HX,12,2H=Y,12,3H/Y5)
196      DO 160 K=1,NM
197      WRITE(3,162)K,K
198      WRITE(3,164)K,K
199      WRITE(3,166)K,K
200      CONTINUE
201      FORMAT(6X,1HU,12,3H=U(,12,1H))
202      FORMAT(6X,2HOU,12,5H=UPH(,12,1H))
203      FORMAT(6X,3HODU,12,6H=UPH2(,12,1H))
204      LBU=1HU
205      WRITE(3,172)NSPC,((LBM,LBU,K),K=1,NM)
206      FORMAT(6X,1HU,12,4H=1.0,8(A1,A1,12),A1,2(/5X,1H*,1X,
207      * 8(A1,12,A1)) )
208      LBU=2HOU
209      WRITE(3,174)NSPC,((LBM,LBU,K),K=1,NM)
210      FORMAT(6X,2HOU,12,1H=,8(A1,A2,12),A1,2(/5X,1H*,1X,
211      * 8(A2,12,A1)) )
212      LBU=3HODU
213      WRITE(3,176)NSPC,((LBM,LBU,K),K=1,NM)
214      FORMAT(6X,3HODU,12,1H=,8(A1,A3,12),A1,2(/5X,1H*,1X,
215      * 8(A3,12,A1)) )
216      DO 180 K=1,NSPC
217      WRITE(3,182)K,K,K,K
218      CONTINUE
219      LBU=2HOU
220      FORMAT(6X,2HOU,12,3H=DU,12,1H=/,6,2)
221      LBU=2HUY
222      WRITE(3,186)((LBPL,LBU,K),K=1,NM)
223      FORMAT(6X,4HYS=,8(A1,A2,12),A1,2(/5X,1H*,1X,8(A2,12,A1)) )
224      PS=PRESS/82.05
225      WRITE(3,234)TPN,PHN,IMN
226      WRITE(6,234)TPN,PHN,IMN
227      FORMAT(1HC,2X,5HTPN =,1PE12.4,6X,5HPHN =,1PE12.4,6X,
228      * 5HTMN =,1PE12.4)
229      WRITE(3,226)TPN
230      FORMAT(6X,13HDT=UPH(NPDE)*,1PE12.4)
231      WRITE(3,227)TPN
232      FORMAT(6X,15HDT=UPH2(NPDE)*,1PE12.4)

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230      WRITE(3,242)PSR
231      FORMAT(6X,5HDIRH=-,1PE18.10,21H*(DT/T+UYS/YS)/(T*YS))
232      DO 807 K=1,NSPC
233      A=1.0/ALD(K)
234      B=-BLD(K)
235      WRITE(3,809)K,A,B
236      CONTINUE
237      FORMAT(6X,2HVL,12,1H=,1PE16.8,6H*(T**(.1PE16.8,2H)) )
238      DO 740 K=1,NSPC
239      A=ALD(K)*BLD(K)
240      B=BLD(K)-1.0
241      WRITE(3,742)K,A,B
242      CONTINUE
243      FORMAT(6X,3HDL,12,1H=,1PE14.6,6H*(T**(.1PE14.6,5H))*DT )
244      DO 747 K=1,NSPC
245      A=1.0/ALD(K)
246      B=-BLD(K)
247      A=A*B
248      B=B-1.0
249      WRITE(3,749)K,A,B
250      CONTINUE
251      FORMAT(6X,3HDL,12,1H=,1PE14.6,6H*(T**(.1PE14.6,5H))*DT )
252      WRITE(3,745)
253      FORMAT(6X,16HDSY=DYS/(YS*YS) )
254      DO 750 K=1,NSPC
255      WRITE(3,752)K,K,K
256      CONTINUE
257      FORMAT(6X,2HDX,12,3H=DY,12,5H/YS-Y,12,5H*UYSY )
258      DO 500 K=1,NSPC
259      WRITE(3,502)K,K,K
260      CONTINUE
261      FORMAT(6X,3HDDY,12,4H=DDU,12,1H/,F6.2)
262      LBODY=3HDDY
263      WRITE(3,506)((LHPL,LBODY,K),K=1,NSPC)
264      FORMAT(6X,5HDDYS=,8(A1,A3,12),A1,2/(5X,1H*,1X,8(A3,12,A1)) )
265      WRITE(3,510)
266      FORMAT(6X,18HDSYSQ=(DYS/YS)**2 )
267      DO 515 K=1,NSPC
268      WRITE(3,518)K,K,K,K,K
269      CONTINUE
270      * 12,9H*DSYSQ-Y,12,12H*DDYS/YS )
271      DO 815 I=1,NSPC
272      IF(1.E0,J)GO TO 815
273      A=1.0/ABD(1,J)
274      B=-BBD(1,J)
275      WRITE(3,818)I,J,A,B
276      CONTINUE
277      FORMAT(6X,2HVD,212,1H=,1PE16.8,6H*(T**(.1PE16.8,2H)) )
278      DO 820 I=1,NSPC
279      DO 820 J=1,NSPC
280      IF(1.E0,J)GO TO 820
281      A=1.0/ABD(1,J)
282      B=-BBD(1,J)
283      A=A*B
284      B=B-1.0
285      H=H-1.0
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820 WRITE(3,822)I,J,A,B
821 CONTINUE
822 FORMAT(6X,3HVD,2I2,IH=,IPEI6.8,6H*(T**,(IPEI6.8,5H)))*DI)
C *****
290 C SPECIFIC HEAT OF THE MIXTURE.
C *****
      WRITE(3,I24)
      FORMAT(IHC,2X,4HSPCIFIC HEAT OF THE MIXTURE. NTIS FORMULA. )
      LBC=6HC(IST+
      LHU=3H)*U
295
      WRITE(3,I32)((LBPL,LHC,K,LBU,K),K=I,NSPC)
      FORMAT(6X,7HCM(IC)=*4(AI,A6,I2,A3,I2),AI,
      * 4(/5X,IH*,IX,4(A6,I2,A3,I2,AI)) )
300 C *****
C THERMAL CONDUCTIVITY OF THE MIXTURE.
C *****
      WRITE(3,272)
      WRITE(3,274)
272 FORMAT(IHC,2X,36HTHERMAL CONDUCTIVITY OF THE MIXTURE.)
274 FORMAT(IHC,2X,4HHAVERAGE OF LINEAR AND RECIPROCAL MIXING RULES. )
      LBX=IHX
      LBPL=IH*
      LBRL=3H*RL
      LBMLX=5HRLSUM
310
      WRITE(3,260)LBMLX,((LBPL,LBX,K,LRRL,K),K=I,NSPC)
      FORMAT(6X,A5,IH=,6(2AI,I2,A3,I2) ,AI,2(/5X,IH*,IX,
      * 8(AI,I2,A3,I2,AI)) )
      LRSRL=3H*VL
      LBMLX=5HRLSIV
315
      WRITE(3,265)
      FORMAT(6X,I5HRLSIV=I.0/RLSIV )
      WRITE(3,270)
      FORMAT(6X,2IHRLM=0.5*(RLSUM*RLSIV))
320
      WRITE(3,306)
      FORMAT(6X,I5HRLM(IC)=RH*RLM )
C *****
C DERIVATIVE OF THE THERMAL CONDUCTIVITY OF THE MIXTURE.
C *****
      WRITE(3,312)
      FORMAT(IHC,2X,40HSPACE DER OF DENSITY TIMES THERMAL COND.)
      LBURL=4H*DRL
      LBDX=2HDX
      LBMLX=5HDLSUM
330
      WRITE(3,760)LBMLX,((LBPL,LBX,K,LHDLR,K,LBPL,LHDX,K,LBRL,K),
      * K=I,NSPC)
      FORMAT(6X,A5,IH=,2(2AI,I2,A4,I2,AI,A2,I2,A3,I2),AI,6(/5X,IH*,IX,
      * 3(AI,I2,A4,I2,AI,A2,I2,A3,I2,AI)) )
      LBPAR=IH)
      LBMLX=5HDLSIV
      LHDLVL=4H*DVL
335
      WRITE(3,765)LBMLX,((LBPL,LHDX,K,LHSLR,K,LBPL,LHX,K,LHDLVL,K),
      * K=I,NSPC)
      FORMAT(6X,A5,IH=,2(AI,A2,I2,A3,I2,A4,I2,A4,I2),AI,6(/5X,IH*,IX,
      * 3(AI,I2,A3,I2,AI,I2,A4,I2,AI)) )
      WRITE(3,770)
      FORMAT(6X,24HDL SIV=-RLSIV*RLSIV )
770

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PROGRAM LOADF	76/76	OPT=1	ROUND=+*/	TRACE	FTN 4.8+498	04/15/80	13.55.29	PAGE	8
400	532	* J=2,NSPC)				MAIN	399		
		FORMAT(6X,4HDSUM,I2,1H=,2(A1,A2,I2,A3,2I2,2A1,I2,A4,2I2),A1,				MAIN	400		
		* 9/(5X,IH*,1X,2(A2,I2,A3,2I2,2A1,I2,A4,2I2,A1)))				MAIN	401		
		1F(NM,EQ.1)GO TO 537				TPC	3		
405		DO 535 K=2,NM				MAIN	402		
		KM=K-1				MAIN	403		
		KP=K+1				MAIN	404		
		WRITE(3,532)K,((LBPL,LHDX,J,LBVD,J,K,LBPL,LBX,J,LBVD,J,K),				MAIN	405		
410	535	* J=1,KM),((LBPL,LHDX,J,LBVD,K,J,LBPL,LBX,J,LBVD,K,J),J=KP,NSPC)				MAIN	406		
	537	CONTINUE				MAIN	407		
		CONTINUE				TPC	4		
		K=NSPC				MAIN	408		
		WRITE(3,532)K,((LBPL,LHDX,J,LBVD,J,K,LBPL,LBX,J,LBVD,J,K),J=1,NM)				MAIN	409		
415		DO 540 K=1,NSPC				MAIN	410		
		WRITE(3,542)K,PHN,K,K,K,K				MAIN	411		
	540	CONTINUE				MAIN	412		
	542	FORMAT(6X,2HDB,I2,1H=,1PEI2,4,4H*(DX,I2,4H*SUM,I2,2H*X,I2,				MAIN	413		
		* 5H*DSUM,I2,IH))				MAIN	414		
		DO 545 K=1,NSPC				MAIN	415		
		WRITE(3,548)K,K,K,K				MAIN	416		
420	545	CONTINUE				MAIN	417		
	548	FORMAT(6X,2HDT,I2,12H=-DRH*(1.0-U,I2,7H)+KH*DU,I2)				MAIN	418		
		DO 550 K=1,NSPC				MAIN	419		
		WRITE(3,552)(K,L=1,7)				MAIN	420		
	550	CONTINUE				MAIN	421		
425	552	FORMAT(6X,4HDFAC,I2,1H=,2HDT,I2,2H/B,I2,2H-T,I2,3H*DB,I2,				MAIN	422		
		* 3H/(8,I2,2H*B,I2,IH))				MAIN	423		
		DO 590 K=1,NSPC				MAIN	424		
		WRITE(3,592)K,K,K,K,K				MAIN	425		
430	590	CONTINUE				MAIN	426		
	592	FORMAT(6X,3HDX,I2,5H=DFAC,I2,3H*DX,I2,4H*FAC,I2,4H*DDX,I2)				MAIN	427		
		DO 595 K=1,NSPC				MAIN	428		
	595	WRITE(3,598)K,K,K,K,K				MAIN	429		
	598	FORMAT(6X,4HDX,I2,3H=DU,I2,3H*VX,I2,2H*U,I2,4H*DVX,I2)				MAIN	430		
435	C	*****				MAIN	431		
	C	USE A BINARY APPROXIMATION FOR THERMAL DIFFUSION FOR THE				MAIN	432		
	C	INDICATED SPECIES.				MAIN	433		
	C	*****				MAIN	434		
	C	WRITE THE NECESSARY ALPHA I J, WHERE I IS A SPECIES WE WANT TO				MAIN	435		
	C	COMPUTE THE THERMAL DIFFUSION FOR.				MAIN	436		
440	C	*****				MAIN	437		
	901	WRITE(3,901)				MAIN	438		
		FORMAT(1HC,2X,40HCOMPUTE ALPHA FOR THE APPROPRIATE PAIRS.)				MAIN	439		
		LHDF=5HTHDF				MAIN	440		
445		DO 900 I=1,NM				MAIN	441		
		IPL=I+1				MAIN	442		
		DO 900 J=1PL,NSPC				MAIN	443		
		IF(LRTHD(I).NE.LHDF.AND.LRTHD(J).NE.LHDF)GO TO 900				MAIN	444		
		IF(LRTHD(I).EQ.LHDF)IP=1				MAIN	445		
		IF(LRTHD(I).EQ.LHDF)JP=J				MAIN	446		
450		IF(LRTHD(I).NE.LHDF)IP=J				MAIN	447		
		IF(LRTHD(I).NE.LHDF)JP=I				MAIN	448		
		I=SQRT(ESK(IP)*ESK(JP))				MAIN	449		
		IF(UM(IP).EQ.0.0.AND.UM(JP).EQ.0.0)GO TO 1302				MAIN	450		
455	C	COMPUTING RULF. P. 528, REID AND SHERWOOD.				MAIN	451		
	C	WE ARE ASSUMING AT MOST ONE POLAR SPECIES.				MAIN	452		
		IF(UM(IP).NE.0.0)LP=IP				MAIN	453		


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460      IF (UM(JP),NE,0.0)LP=JP
      IF (LP,EQ,1P)LNP=JP
      IF (LP,EQ,JP)LNP=1P
      UMP=UM(LP)*1.0E-18
      SGC=SGA(LP)*1.0E-8
      TPSTAR=UMP*UMP/(ESK(LP)*RK*SGC*SGC*SGC*SGRT(8.0))
      FC=1.0*(1.0/SQRT(2.0))*(ALP(LNP)*TPSTAR/(SGA(LNP)**3))*SQRT(ESK(
      * LP)/ESK(LNP))
      WRITE(6,1305)IP,JP,LNP,FC
1305      FORMAT(15X,4I6,1PE12.4)
      E=E*FC*FC
      CONTINUE
      WRITE(3,903)E
      FORMAT(6X,5HTS=T/,1PE14.6)
470      LBRTP=3HRT
      WRITE(3,906)LBRTP,ARTP,CRTP
      FORMAT(6X,A3,1H=,1PE14.6,5H*EXP(,1PE14.6,4H/TS) )
906      LBC=3HCST
      WRITE(3,906)LBC,ACST,CCST
      WRITE(3,909)
      FORMAT(6X,16HCSTP=6.0*CSI-5.0 )
      WM=(W(IP)-W(JP))/W(IP)*W(JP)
      WRITE(3,912)IP,JP,WM
480      FORMAT(6X,2HAL,2I2,1H=,1PE14.6,9H*RT*PCSTP )
      WRITE(3,915)E
      FORMAT(6X,7HOTS=DT/,1PE14.6)
915      A=-ARTP*CRTP
      LBDRTP=4HDRTP
      WRITE(3,918)LBDRTP,A,CRTP
485      FORMAT(6X,A4,1H=,1PE14.6,5H*EXP(,1PE14.6,16H/TS)*DTS/(TS*TS) )
      LBDC=4HDCST
      A=-ACST*CCST
      WRITE(3,918)LBDC,A,CCST
490      WRITE(3,921)
      FORMAT(6X,14HDCSTP=6.0*DCST )
      WRITE(3,924)IP,JP,WM
921      FORMAT(6X,3HDAL,2I2,1H=,1PE14.6,22H*(ORTP*PCSTP+RTP*DCSTP) )
924      IF (LBTHD(JP),NE,LBDRTP)GO TO 900
      WRITE(3,927)JP,IP,JP
495      FORMAT(6X,2HAL,2I2,2H=-,2HAL,2I2)
      WRITE(3,930)JP,IP,JP
930      FORMAT(6X,3HDAL,2I2,2H=-,3HDAL,2I2)
900      CONTINUE
      WRITE(3,951)
      FORMAT(1HC,2X,48HCOMPUTE THERMAL DIFFUSION FOR THE GIVEN SPECIES.)
500      LBX=1HX
      LBALP=3H*AL
      LBHX=2HDX
      LBHALP=4H*DAL
      DO 950 I=1,NSPC
      IF (LBTHD(I),NE,LBDRTP)GO TO 950
      IF (1.EQ,1)WRITE(3,933)((LBPL,LBX,J,LHALP,I,J),J=2,NSPC)
933      FORMAT(6X,4HSUM=,4(2A1,I2,A3,2I2),A1,4(15X,1H*,1X,
      * 5(A1,I2,A3,2I2,A1)) )
      IF (1.EQ,NSPC)WRITE(3,933)((LBPL,LBX,J,LHALP,I,J),J=1,NM)
      IF (1.EQ,1.OR,1.EQ,NSPC)GO TO 935
      IN=I-I
510

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515      IP=I+1
      WRITE(3,933)((LBPL,LBX,J,LRALP,I,J),J=1,IM),((LBPL,LBX,J,LRALP,
* I,J),J=IP,NSPC)
      CONTINUE
935      WRITE(3,936)I
      FORMAT(6X,SHRKT=X,I2,4H*SUM )
936      WRITE(3,939)I
      FORMAT(6X,I2HVTOP=PKT*UVX,I2,3H*UT )
939      WRITE(3,942)I
      FORMAT(6X,7HVBOT=DX,I2,2H*U )
942      WRITE(3,945)I
      FORMAT(6X,3HUVT,I2,10H=VTOP/VBOT )
945      IF(I.EQ.I)WRITE(3,948)((LBPL,LBX,J,LRALP,I,J,LRPL,LBX,J,LRALP,I,
* J),J=2,NSPC)
      FORMAT(6X,SHDSUM=2(AI,A2,I2,A3,2I2,2AI,I2,A4,2I2),AI,
948      * 8(/5X,IH*,IX,2(A2,I2,A3,2I2,2AI,I2,A4,2I2,AI)) )
      IF(I.EQ.NSPC)WRITE(3,948)((LBPL,LBX,J,LRALP,I,J,LRPL,LBX,
* J,LRDALP,I,J),J=I,NM)
      IF(I.EQ.I.OR.I.EQ.NSPC)GO TO 952
      IM=I-1
      IP=I-1
      WRITE(3,948)((LBPL,LBX,J,LRALP,I,J,LRPL,LBX,J,LRDALP,I,J),
* J=I,IM),((LBPL,LBX,J,LRALP,I,J,LRPL,LBX,J,LRDALP,I,J),J=IP,NSPC)
      CONTINUE
952      WRITE(3,955)I,I
      FORMAT(6X,7HDKT=DX,I2,6H*SUM+X,I2,5H*DSUM )
955      WRITE(3,958)I,I,I
      FORMAT(6X,I4HVTOP=URKT*UVX,I2,12H*UT+RKT*DUVX,I2,
958      * 11H*DT+RKT*UVX,I2,4H*DDT )
      WRITE(3,961)I,I
      FORMAT(6X,9HVBOT=DDX,I2,5H*U+DX,I2,3H*UT )
961      WRITE(3,964)I
      FORMAT(6X,4HUVT,I2,34H=DVTOP/VBOT-VTOP*VBOT/(VBOT*VBOT) )
964      CONTINUE
950      WRITE(3,1129)
      FORMAT(1HC,2X,36HFIND THE FINAL VALUES OF UV AND DUV. )
1129      DO 1130 K=I,NSPC
      IF(LBTHD(K).EQ.LBDOFF)WRITE(3,1132)K,K,K
      IF(LBTHD(K).NE.LBDOFF)WRITE(3,1131)K,K
      CONTINUE
1130      FORMAT(6X,2HUV,I2,4H=UVX,I2)
1131      FORMAT(6X,2HUV,I2,4H=UVX,I2,4H+UVT,I2)
1132      DO 1135 K=I,NSPC
      IF(LBTHD(K).EQ.LBDOFF)WRITE(3,1134)K,K,K
      IF(LBTHD(K).NE.LBDOFF)WRITE(3,1137)K,K
      CONTINUE
1135      FORMAT(6X,3HUV,I2,5H=DUVX,I2)
1137      FORMAT(6X,3HUV,I2,5H=DUVX,I2,5H+DUVT,I2)
1138      CONTINUE
995      LUV=2HUV
      WRITE(3,1212)((LHM,LUV,K),K=1,NSPC)
1212      FORMAT(6X,3HUV=8(AI,A2,I2),AI,2(/5X,IH*,IA,8(A2,I2,AI)) )
      DO 1215 K=1,NSPC
1215      WRITE(3,1218)K,K,K
1218      FORMAT(6X,2HUV,I2,3H=UV,I2,5H+DUV*U,I2)
      LDUV=3HUV
      WRITE(3,1222)((LHM,LUDUV,K),K=1,NSPC)
570

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515      1P=1+I
      WRITE(3,933)((LBPL,LBX,J,LBALP,I,J),J=1,IM),((LBPL,LBX,J,LBALP,
      * I,J),J=IP,NSPC)
      CONTINUE
      WRITE(3,936)I
      FORMAT(6X,5HDKT=X,I2,4H*SUM )
      WRITE(3,939)I
      FORMAT(6X,12HVTOP=DKT*UVX,I2,3H*UT )
      WRITE(3,942)I
      FORMAT(6X,7HVBOT=DX,I2,2H* )
      WRITE(3,945)I
      FORMAT(6X,3HUVT,I2,10H=VTOP/VBOT )
      IF(1.EQ.1)WRITE(3,948)((LBPL,LBX,J,LBALP,I,J,LBPL,LBX,J,LBALP,I,
      * J),J=2,NSPC)
      FORMAT(6X,5HDSUM=2(A1,A2,I2,A3,2I2,2A1,I2,A4,2I2),A1,
      * 8(5X,IH*,1X,2(A2,I2,A3,2I2,2A1,I2,A4,2I2,A1)) )
      IF(1.EQ.NSPC)WRITE(3,948)((LBPL,LBX,J,LBALP,I,J,LBPL,LBX,
      * J,LBDALP,I,J),J=1,NM)
      IF(1.EQ.1.OR.1.EQ.NSPC)GO TO 952
      IM=I-1
      1P=1+I
      WRITE(3,948)((LBPL,LBX,J,LBALP,I,J,LBPL,LBX,J,LBDALP,I,J),
      * J=1,IM),((LBPL,LBX,J,LBALP,I,J,LBPL,LBX,J,LBDALP,I,J),J=IP,NSPC)
      CONTINUE
      WRITE(3,955)I,I
      FORMAT(6X,7HDKT=DX,I2,6H*SUM*X,I2,5H*DSUM )
      WRITE(3,958)I,I,I
      FORMAT(6X,14HVTOP=DKT*UVX,I2,12H*DT+DKT*DUVX,I2,
      * 11H*DT+DKT*UVX,I2,4H*DDT )
      WRITE(3,961)I,I
      FORMAT(6X,9HVBOT=DDX,I2,5H*DT+DX,I2,3H*DT )
      WRITE(3,964)I
      FORMAT(6X,4HUVT,I2,34H=DVTOP/VBOT-VTOP*(VBOT*VBOT) )
      CONTINUE
      WRITE(3,1129)
      FORMAT(1HC,2X,36HFIND THE FINAL VALUES OF UV AND DUV. )
      DO 1130 K=1,NSPC
      IF(LBTHD(K).EQ.LBDOFF)WRITE(3,1132)K,K,K
      IF(LBTHD(K).NE.LBDOFF)WRITE(3,1131)K,K,K
      CONTINUE
      1130      FORMAT(6X,2HUV,I2,4H=UVX,I2)
      1131      FORMAT(6X,2HUV,I2,4H=UVX,I2,4H*UVT,I2)
      1132      DO 1135 K=1,NSPC
      IF(LBTHD(K).EQ.LBDOFF)WRITE(3,1134)K,K,K
      IF(LBTHD(K).NE.LBDOFF)WRITE(3,1137)K,K,K
      CONTINUE
      1135      FORMAT(6X,3HUV,I2,5H=DUVX,I2)
      1137      FORMAT(6X,3HUV,I2,5H=DUVX,I2,5H*DUVT,I2)
      1138      CONTINUE
      995      LUV=2HUV
      WRITE(3,1212)((LHM,LHUV,K),K=1,NSPC)
      1212      FORMAT(6X,3HUV=8(A1,A2,I2),A1,2(/5X,IH*,1X,8(A2,I2,A1)) )
      DO 1215 K=1,NSPC
      1215      WRITE(3,1218)K,K,K
      1218      FORMAT(6X,2HUV,I2,3H=UV,I2,5H*DUV*U,I2)
      LHUV=3HUV
      WRITE(3,1222)((LHM,LHUV,K),K=1,NSPC)
      570

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```

1222 FORMAT(6X,4HDDV=,8(A1,A3,I2),A1,2(/5X,1H*,1X,8(A3,I2,A1)) )
1225 DO 1225 K=1,NSPC
1225 WRITE(3,1228)K,K,K
1228 FORMAT(6X,3HDDV,12,4H=DDV,12,6H+DDV*DU,12,6H+DDV*U,12)
575 DO 485 K=1,NSPC
485 WRITE(3,488)K,K
488 FORMAT(6X,9HDDV(1ST+,12,7H)=RH*UV,12)
DO 810 K=1,NSPC
810 WRITE(3,812)K,K,K
812 FORMAT(6X,10HDDV(1ST+,12,8H)=URH*UV,12,7H+RH*DDV,12)
580 C *****
C FIND THE TIME DERIVATIVES.
C *****
612 WRITE(3,612)
612 FORMAT(1HC,2X,26HFIND THE TIME DERIVATIVES.)
622 WRITE(3,622)
622 FORMAT(6X,15HSP=ASP*HSP*TIME)
TMSPH2=TMN/(PHN*PHN)
628 WRITE(3,628)
628 FORMAT(1X,3H100,2X,8HCONTINUE)
632 WRITE(3,632)
632 FORMAT(6X,25HIF (KPU.EQ.NPDE)GO TO 150)
636 WRITE(3,636)TMN
636 FORMAT(6X,3HRY=,1PE20,10,8H*R (KPU.E) )
TMSPH=TMN/PHN
595 WRITE(3,638)TMSPH
638 FORMAT(6X,4HDI=,1PE20,10,16H*DDHUV(1ST+KPU.E) )
WRITE(3,642)
642 FORMAT(6X,23HFVAL=SP*UPH (KPU.E)+UY+RY)
WRITE(3,646)
646 FORMAT(6X,6HRETURN)
648 WRITE(3,648)
648 FORMAT(1X,3H150,2X,8HCONTINUE)
DO 650 K=1,NM
605 WRITE(3,652)K,K
650 CONTINUE
652 FORMAT(6X,2HDDU,12,5H=UPH(,12,1H) )
K=NSPC
LBDU=2HDDU
610 WRITE(3,656)K,((LBM,LBDU,J),J=1,NM)
610 FORMAT(6X,2HDDU,12,1H=,8(A1,A2,I2),A1,2(/5X,1H*,1X,8(A2,I2,A1)) )
WRITE(3,662)TMSPH2
662 FORMAT(6X,3HDL=,1PE20,10,1H*)
664 WRITE(3,664)
664 FORMAT(5X,1H*,1X,4H(DRHLM(1C)*UPH(NPDE)+RHLM(1C)*UPH2(NPDE)) )
LHBL=1H
LHC=6HC(1ST+
LHDDV=10H)*RHUV(1ST
WRITE(3,668)TMSPH,((LHBL,LHPL,LHC,K,LHDDV,LHPL,K,LAP),K=1,
* NSPC),LHP
668 FORMAT(6X,4HDI=,1PE20,10,12H*UPH(NPDE)*(,2A1,A6,12,A10,A1,12,
* 3A1,10(/5X,1H*,1X,2(A6,12,A10,A1,12,3A1)) )
TMSTP=TMN/TPN
LHR=2HPL
620 LHR=RH)*H(1ST+
WRITE(3,672)TMSTP,((LHHL,LHPL,LHC,K,LHHR,K,LHP),K=1,NSPC),LHP
672 FORMAT(6X,4HDI=,1PE20,10,2PH*(,2(A1,A2,12,AH,12,A1),2A1,

```

PROGRAM	LOADF	76/76	OPT=1	ROUND=+-*/	THACE	FIN	4.8+49H	04/15/80	13.55.29	PAGE	12
630		* 9(/5X,IH*1X,2(A2,I2,A8,I2,3A1)))						MAIN	625		
		WRITE(3,676)						MAIN	626		
	676	FORMAT(6X,35HFVAL=SP*UPH(NPDE)*(IL+TR+TD)/CM(IC))						MAIN	627		
		STOP						MAIN	628		
		END						MAIN	629		

HLOCK ADDRESS LENGTH FILE

LOADF 110 12230 LG0
 /STP.END/ 12340 1 SL-FTNL18
 /FCL.C./ 12341 30 SL-FTNL18
 /QB.IO./ 12371 144 SL-FTNL18
 Q2NTRY= 12535 4 SL-FTNL18
 COMIO= 12541 10 SL-FTNL18
 FECSK= 12551 41 SL-FTNL18
 FEIFST= 12612 3 SL-FTNL18
 FLIN= 12615 156 SL-FTNL18
 FLIOUT= 12773 315 SL-FTNL18
 FMTAP= 13310 377 SL-FTNL18
 FORSYS= 13707 300 SL-FTNL18
 FORUTL= 14207 45 SL-FTNL18
 GETFIT= 14254 54 SL-FTNL18
 INCOM= 14330 144 SL-FTNL18
 INPC= 14474 173 SL-FTNL18
 KODER= 14667 476 SL-FTNL18
 KRAKER= 15365 454 SL-FTNL18
 OUTC= 16041 155 SL-FTNL18
 OUTCOM= 16216 204 SL-FTNL18
 ERRCAP= 16422 317 SL-FTNL18
 FERCAP= 16741 171 SL-FTNL18
 EXP.MSG 17132 16 SL-FTNL18
 SOUT 17150 6 SL-FTNL18
 SORT. 17156 32 SL-FTNL18
 SYSAID= 17210 1 SL-FTNL18
 SYS=1ST 17211 65 SL-FTNL18

1 H2 THDFF 2.0000E+00 2.9200E+00 3.8000E+01 0. 7.9000E-01

.31001901E+01 .51119464E-03 .52644210E-07 -.34909973E-10 .36945345E-14 H2
 -.87738042E+03 -.19629421E+01 .30574451E+01 .26765200E-02 -.58099162E-05 H2
 .55210391E-08 -.18122739E-11 -.98890474E+03 -.22997056E+01 H2

2 N2 2.8000E+01 3.6200E+00 9.7500E+01 0. 0.

.28963194E+01 .15154866E-02 -.57235277E-06 .99807393E-10 -.65223555E-14 N2
 -.90586184E+03 .61615144E+01 .36748261E+01 -.12081500E-02 .23240102E-05 N2
 -.63217559E-09 -.22577253E-12 -.10611588E+04 .23580424E+01 N2

VISCOSITY FROM WARNATZ ST PAR.
 LEAST SQUARES FIT, I=300,2000.
 THERMAL CONDUCTIVITIES FROM WARNATZ ST PAR.
 LEAST SQUARES FIT, I=300,2000.

1 H2 2.188700E-06 6.502900E-01 H2 VISCOSITY.

1 H2 6.357900E-06 7.393300E-01 H2 THERMAL CONDUCTIVITY.

2 H2 4.266700E-06 6.613600E-01 N2 VISCOSITY.

2 H2 6.407700E-07 7.999600E-01 N2 THERMAL CONDUCTIVITY.

BINARY DIFFUSION COEFFICIENTS FROM WARNATZ ST PAR.
 LEAST SQUARES FIT, I=100,300

1	1	H2	H2	1.119300E-04	1.661400E+00	H2	H2	BINARY DIFFUSION.
1	2	H2	N2	5.951700E-05	1.663800E+00	H2	N2	BINARY DIFFUSION.
2	2	N2	N2	1.537400E-05	1.672900E+00	N2	N2	BINARY DIFFUSION.

8.112200E-01 4.866900E-02 RTP=RT/(6C*-5) FIT A*EXP(C/T)

9.542600E-01 -1.435700E-01 C* HCB FIT A*EXP(C/T)

TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03


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1  SUBROUTINE F(TIME,PH,U,UPH,UPH2,FVAL,NPDE,IC,KSKT,KSKP)
   DIMENSION U(NPDE),UPH(NPDE),UPH2(NPDE)
   COMMON/TARAB/ASP,BSP,TPN,PHN,IMN,TMSPH,TMSTP,TPENT
   COMMON/TARP/PRESS,PSR,NPDEM
   COMMON/TARSM/SMALL
5  DIMENSION K(20)
   DIMENSION C(1000),H(1000),RHL(100),DRHLM(100),CM(100)
   COMMON/TABCT/RL,CPMX,H0(20),R2D(20),R2DM(20)
   COMMON/TABMF/RHUV(1000),DRHUV(1000)
10  COMMON/TABRY/T,RH,Y1,Y2,Y3,Y4,Y5,Y6,Y7,Y8,Y9,Y10
   C AT EACH CALL THE TIME RATE OF CHANGE FOR ONE PDE IS RETURNED IN FVAL.
   C FOR THE COMPLETE TRANSPORT CASE, WE DO NOT WANT THE U VALUES OR
   C THEIR FIRST DERIVATIVES TO BE ZERO. THIS CAN LEAD TO DIVISION
   C BY ZERO.
15  DO 5 K=1,NPDEM
   IF(ARS(U(K)),LT,SMALL)U(K)=SMALL
5  IF(ARS(UPH(K)),LT,SMALL)UPH(K)=SMALL
   C TEST CASE. BINARY MIX OF H2 AND N2. WARNAT2 TRANSPORT VALUES.
   YN=1.0-U( 1)
   CALL RT(U,YN,R,NPDE,KPDE,IC,KSKP)
20  IST= 2*(IC-1)
   IF(KSKT.GT.1)GO TO 100
   IF(KSKR.GT.1)GO TO 125
   C NT1S ENTHALPIES AND HEAT CAPACITIES.
25  IF(T.GT.1000.)GO TO 2000
   C 1=1.9872*( 3.05744510E+00+T*( 2.67652000E-03
   *+T*( -5.80991620E-06+T*( 5.52103910E-09+T*( -1.81227390E-12))))
   H 1=1.9872*( -9.88904740E+02+T*( 3.05744510E+00
   *+T*( 2.67652000E-03/2.0+T*( -5.80991620E-06/3.0
   *+T*( 5.52103910E-09/4.0+T*( -1.81227390E-12/5.0))))))
30  C 2=1.9872*( 3.67482610E+00+T*( -1.20815000E-03
   *+T*( 2.32401020E-06+T*( -6.32175590E-10+T*( -2.25772530E-13))))
   H 2=1.9872*( -1.06115880E+03+T*( 3.67482610E+00
   *+T*( -1.20815000E-03/2.0+T*( 2.32401020E-06/3.0
   *+T*( -6.32175590E-10/4.0+T*( -2.25772530E-13/5.0))))))
   GO TO 3000
2000 CONTINUE
   C 1=1.9872*( 3.10019010E+00+T*( 5.11194640E-04
   *+T*( 5.26442100E-08+T*( -3.49099730E-11+T*( 3.69453450E-15))))
40  H 1=1.9872*( -8.77380420E+02+T*( 3.10019010E+00
   *+T*( 5.11194640E-04/2.0+T*( 5.26442100E-08/3.0
   *+T*( -3.49099730E-11/4.0+T*( 3.69453450E-15/5.0))))))
   C 2=1.9872*( 2.89631940E+00+T*( 1.51548660E-03
   *+T*( -5.72352770E-07+T*( 9.98073930E-11+T*( -6.52235550E-15))))
45  H 2=1.9872*( -9.05861840E+02+T*( 2.89631940E+00
   *+T*( 1.51548660E-03/2.0+T*( -5.72352770E-07/3.0
   *+T*( 9.98073930E-11/4.0+T*( -6.52235550E-15/5.0))))))
3000 CONTINUE
   C SPECIFIC HEATS AND SPECIFIC ENTHALPIES.
50  C(IST+ 1)=C 1/ 2.00
   H(IST+ 1)=H 1/ 2.00
   C(IST+ 2)=C 2/ 28.00
   H(IST+ 2)=H 2/ 28.00
   IP5 CONTINUE
55  C VISCOSITY FROM WARNAT2 ST PAR.
   C LEAST SQUARES FIT, I=300,2000.
   C THERMAL CONDUCTIVITIES FROM WARNAT/ ST PAR.

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C LEAST SQUARES FIT, T=300.2000.
C V 1= 2.188700E-06*(T** 6.502900E-01)
C V 2= 4.266700E-06*(T** 6.613600E-01)
C RL 1= 6.357900E-06*(T** 7.383300E-01)
C RL 2= 6.407700E-07*(T** 7.999600E-01)
C HINARY DIFFUSION COEFFICIENTS FROM WARNATZ ST PAR.
C LEAST SQUARES FIT, T=100.300
C PRESS = 1.00
C O 1 2= 5.951700E-05*(T** 1.663800E+00)
C SPACE DERIVATIVES.
YS=Y 3
X 1=Y 1/YS
X 2=Y 2/YS
U 1=U( 1 )
DU 1=UPH( 1 )
DDU 1=UPH2( 1 )
U 2=1.0-U 1
DU 2=-DU 1
DDU 2=-DDU 1
DY 1=DU 1/ 2.00
DY 2=DU 2/ 28.00
DYS=+DY 1+DY 2
C TPN = 1.0000E+03 PHN = 5.0000E-05 TMN = 1.0000E-03
DT=UPH(NPDE)* 1.0000E+03
DRH=- 1.2187690433E-02*(DT/(T+DYS/YS)/(T*YS)
VL 1= 1.57284638E+05*(T**(-7.36330000E-01))
VL 2= 1.56062238E+06*(T**(-7.99960000E-01))
DRL 1= 4.694228E-06*(T**(-2.616700E-01))*DT
DRL 2= 5.125904E-07*(T**(-2.000400E-01))*DT
DVL 1= -1.161280E+05*(T**(-1.738330E+00))*DT
DVL 2= -1.248435E+06*(T**(-1.799960E+00))*DT
DYS=DYS/(YS*YS)
DX 1=DY 1/YS-Y 1*DYSY
DX 2=DY 2/YS-Y 2*DYSY
DDY 1=DDU 1/ 2.00
DDY 2=DDU 2/ 28.00
DDYS=+DDY 1+DDY 2
DYSYSQ=(DYS/YS)**2
DDX 1=(DDY 1-2.0*DY 1*DYS/YS+2.0*Y 1*DYSYSQ-Y 1*DDYS/YS)/YS
DDX 2=(DDY 2-2.0*DY 2*DYS/YS+2.0*Y 2*DYSYSQ-Y 2*DDYS/YS)/YS
VD 1 2= 1.68019221E+04*(T**(-1.66380000E+00))
VD 1 2= -2.79550381E+04*(T**(-2.66380000E+00))*DT
C SPECIFIC HEAT OF THE MIXTURE. N15 FORMULA.
CM(IC)=+C(1ST+ 1)*U 1+C(1ST+ 2)*U 2
C THERMAL CONDUCTIVITY OF THE MIXTURE.
C AVERAGE OF LINEAR AND RECIPROCAL MIXING RULES.
RLSUM=+X 1*RL 1+X 2*RL 2
RLSIV=+X 1*VL 1+X 2*VL 2
RLSIV=1.0/RLSIV
RLM=0.5*(PLSUM+RLSIV)
RMLM(IC)=RH*RLM
C SPACE DER OF DENSITY TIMES THERMAL (OND.
DLSUM=+X 1*DRL 1+DX 1*RL 1+X 2*DRL 2+DX 2*RL 2
DLSIV=+DX 1*VL 1+X 1*DVL 1+DX 2*VL 2+X 2*DVL 2
DLSIV=-RLSIV*RLSIV*DLSIV
DRLM=0.5*(DLSUM+DLSIV)

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115      DRHLM(1C)=DRH*RLM+RH*DRLM
      C SOLVE FOR UV.
      SUM 1=X 2*VD 1 2
      SUM 2=X 1*VD 1 2
      H 1=X 1*SUM 1* 5.0000E-05
      B 2=X 2*SUM 2* 5.0000E-05
      T 1=-RH*(1.0-U 1)
      T 2=-RH*(1.0-U 2)
      FAC 1=T 1/R 1
      FAC 2=T 2/R 2
      VX 1=FAC 1*DX 1
      VX 2=FAC 2*DX 2
      UVX 1=U 1*VX 1
      UVX 2=U 2*VX 2
      C SPACE DER OF DENSITY TIMES UV.
      USUM 1=DX 2*VD 1 2+X 2*DVD 1 2
      USUM 2=DX 1*VD 1 2+X 1*DVD 1 2
      DR 1= 5.0000E-05*(UX 1*SUM 1+X 1*DSUM 1)
      DR 2= 5.0000E-05*(UX 2*SUM 2+X 2*DSUM 2)
      DT 1=-DRH*(1.0-U 1)+RH*DU 1
      DT 2=-DRH*(1.0-U 2)+RH*DU 2
      UFAC 1=DT 1/B 1-T 1*UB 1/(B 1*B 1)
      DFAC 2=DT 2/B 2-T 2*UB 2/(B 2*B 2)
      DVX 1=DFAC 1*DX 1+FAC 1*DDX 1
      DVX 2=DFAC 2*DX 2+FAC 2*DDX 2
      DUVX 1=DU 1*VX 1+U 1*DVX 1
      DUVX 2=DU 2*VX 2+U 2*DVX 2
      C COMPUTE ALPHA FOR THE APPROPRIATE PAIRS.
      TS=T/ 6.086871E+01
      RTP= 8.112200E-01*EXP( 4.866900E-02/TS)
      CST= 9.542600E-01*EXP( -1.435700E-01/TS)
      CSTP=6.0*CST-5.0
      AL 1 2= -8.666667E-01*RTP*CSTP
      DTS=DT/ 6.086871E+01
      DRTP= -3.948127E-02*EXP( 4.866900E-02/TS)*DTS/(TS*TS)
      DCST= 1.370031E-01*EXP( -1.435700E-01/TS)*DTS/(TS*TS)
      DCSTP=6.0*DCST
      DUAL 1 2= -8.666667E-01*(DRTP*CSTP+RTP*DCSTP)
      C COMPUTE THERMAL DIFFUSION FOR THE GIVEN SPECIES.
      SUM=X 2*AL 1 2
      RKT=X 1*SUM
      VTOP=RKT*UVX 1*DT
      VBOT=DX 1*T
      UVT 1=VTOP/VBOT
      USUM=X 2*AL 1 2+X 2*DAL 1 2
      DRKT=DX 1*SUM+X 1*USUM
      DVTOP=DRKT*UVX 1*DT+RKT*DUVX 1*DT+RKT*UVX 1*DOT
      DVBOT=DX 1*T+DX 1*DT
      DUVT 1=DVTOP/VBOT-VTOP*DVBOT/(V*DT*V*DT)
      C FIND THE FINAL VALUES OF UV AND DUV.
      UV 1=UVX 1+UVT 1
      UV 2=UVX 2
      DUV 1=DUVX 1+DUVT 1
      DUV 2=DUVX 2
      DV=-UV 1-UV 2
      UV 1=UV 1+DV*U 1
      UV 2=UV 2+DV*U 2

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175      DDV=-DUV 1-DUV 2
          DUV 1=DUV 1+DV*DU 1+DDV*U 1
          DUV 2=DUV 2+DV*DU 2+DDV*U 2
          RHUV(IST+ 1)=RH*UV 1
          RHUV(IST+ 2)=RH*UV 2
          DRHUV(IST+ 1)=DRH*UV 1+RH*DUV 1
          DRHUV(IST+ 2)=DRH*UV 2+RH*DUV 2
      C FIND THE TIME DERIVATIVES.
          SP=ASP+BSP*TIME
180      100 CONTINUE
          IF(KPDE.EQ.NPDE)GO TO 150
          HY= 1.000000000E-03*R(KPDE)
          DY=- 2.000000000E+01*DRHUV(IST+KPDE)
          FVAL=SP*UPH(KPDE)+DY*RY
          RETURN
185      150 CONTINUE
          DU 1=UPH( 1)
          DU 2=-DU 1
          TL= 4.000000000E+05*
          * (DRHLM(IC)*UPH(NPDE)+RHLM(IC)*UPH2(NPDE))
          TD=- 2.000000000E+01*UPH(NPDE)*( +C(IST+ 1)*RHUV(IST+ 1) +
          * C(IST+ 2)*RHUV(IST+ 2))
          TR=- 1.000000000E-06*( +R( 1)*H(IST+ 1) +R( 2)*H(IST+ 2))
          FVAL=SP*UPH(NPDE)+(TL+TR+TD)/CM(IC)
          RETURN
190      198 END
195      F 173
          F 174
          F 175
          F 176
          F 177
          F 178
          F 179
          F 180
          F 181
          F 182
          F 183
          F 184
          F 185
          F 186
          F 187
          F 188
          F 189
          F 190
          F 191
          F 192
          F 193
          F 194
          F 195
          F 196
          F 197
          F 198

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LIST OF SYMBOLS

- $A_{ij}^* = \Omega_{ij}^{(2,2)*} / \Omega_{ij}^{(1,1)*}$, quotient of collision integrals.
 $B_{ij}^* = [5\Omega_{ij}^{(1,2)*} - 4\Omega_{ij}^{(1,3)*}] / \Omega_{ij}^{(1,1)*}$, quotient of collision integrals.
 $C_{ij}^* = \Omega_{ij}^{(1,2)*} / \Omega_{ij}^{(1,1)*}$, quotient of collision integrals.
 $C_{i,int}$ = internal heat capacity, cal-mole⁻¹-K⁻¹.
 $C_{i,rot}$ = rotational heat capacity, cal-mole⁻¹-K⁻¹.
 $C_{i,tr}$ = translational heat capacity, cal-mole⁻¹-K⁻¹.
 $C_{i,v}$ = heat capacity at constant volume, cal-mole⁻¹-K⁻¹.
 c_{pi} = specific heat, cal-gm⁻¹-K⁻¹.
 $c_p = \sum_{i=1}^N c_{pi} Y_i$, specific heat of the mixture, cal-gm⁻¹-K⁻¹.
 D_{ij} = binary diffusion coefficient, cm²-s⁻¹.
 D_{im} = diffusion coefficient of species i into a mixture, cm²-s⁻¹.
 D_{ij} = multicomponent diffusion coefficient, cm²-s⁻¹.
 D_i^T = multicomponent thermal diffusion coefficient, gm-s⁻¹-cm⁻¹.
 $D_{i,int,j}$ = binary diffusion coefficient for internal energy, cm²-s⁻¹.
 h_i = specific enthalpy, cal-gm⁻¹.
 k = Boltzmann constant = 1.38054X10⁻¹⁶ erg-K⁻¹-molecule⁻¹.
 k_{ij} = thermal diffusion ratio.
 k_{im} = thermal diffusion ratio between species i and the rest of the mixture.
 M_i = molecular weight, gm-mole⁻¹.
 p = pressure, atm.
 q = total energy flux relative to the fluid velocity, cal-cm⁻²-s⁻¹.
 R_i = rate of production of ith species by chemical reaction, mole-cm⁻³-s⁻¹.
 R = gas constant = 1.9872 cal-mole⁻¹-K⁻¹.
 R_a = gas constant = 82.05 cm³-atm-mole⁻¹-K⁻¹.

LIST OF SYMBOLS (Cont'd)

t = time, s.

T = temperature, K.

T_u = temperature of unburned mixture, K.

T_B = temperature of burned mixture, K.

$T_i^* = T/(\epsilon_i/k)$.

$T_{ij}^* = T/(\epsilon_{ij}/k)$.

u = fluid velocity, cm-s^{-1} .

V_i = diffusion velocity, cm-s^{-1} .

\mathcal{V}_i = diffusion velocity due to species gradients, cm-s^{-1} .

\mathcal{W}_i = diffusion velocity due to the temperature gradient, cm-s^{-1} .

x = spatial coordinate, cm.

X_i = mole fraction.

Y_i = mass fraction.

Y_{iu} = mass fraction of species i in the unburned mixture.

Y_{iB} = mass fraction of species i in the burned mixture.

α_i = polarizability, \AA^3 .

ϵ_i/k = Lennard-Jones or Stockmayer parameter, K.

η_i = viscosity, poise = $\text{gm-cm}^{-1}\text{-s}^{-1}$.

μ_i = dipole moment, debye = $10^{-18} \text{ gm}^{1/2}\text{-cm}^{5/2}\text{-s}^{-1}$.

σ_i = Lennard-Jones or Stockmayer parameter, \AA .

λ_o = thermal conductivity of the mixtures, neglecting diffusion effects, $\text{cal-cm}^{-1}\text{-s}^{-1}\text{-K}^{-1}$.

$\lambda_{o,tr}$ = thermal conductivity due to translational energy, $\text{cal-cm}^{-1}\text{-s}^{-1}\text{-K}^{-1}$.

$\lambda_{o,int}$ = thermal conductivity due to internal energy, $\text{cal-cm}^{-1}\text{-s}^{-1}\text{-K}^{-1}$.

LIST OF SYMBOLS (Cont'd)

$\lambda_{\text{mix}}^{\text{mon}}$ = thermal conductivity of a mixture of monatomic gases, $\text{cal-cm}^{-1}\text{-s}^{-1}\text{-K}^{-1}$.

$\lambda_{\text{mix}}^{\text{poly}}$ = thermal conductivity of a mixture, $\text{cal-cm}^{-1}\text{-s}^{-1}\text{-K}^{-1}$.

ρ = fluid density, gm-cm^{-3} .

ξ_{ij} = rotational collision numbers.

$\Omega_{ij}^{(1,1)*}; \Omega_{ij}^{(2,2)*}; \Omega_{ij}^{(1,2)*}; \Omega_{ij}^{(1,3)*}$ = collision integral.

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